

A Novel Flash Ironmaking Process

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American Iron and Steel Institute/University of Utah

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Lawrence Kavanagh, American Iron and Steel Institute

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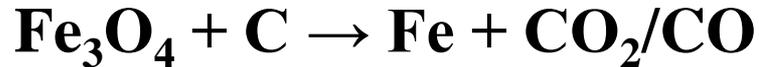
Project Objective

- Develop a new ironmaking process w/ significant reduction in energy consumption and CO₂ generation
- Blast furnace requires pelletization and/or sintering of iron ore concentrate
- Consumes large amounts of energy and carbon → CO₂ emissions
- Alternative ironmaking processes must have:
 - Large production capacities (e.g., ~1,000,000 tpy of iron)
 - Use the main raw material (i.e., iron ore) with minimal pretreatment

Technical Approach

Current practice

Blast Furnace



- Produces >90% iron
- Large capital investments
- Special coal for cokemaking
- Needs pelletization/sintering
- Significant Energy Consumption and CO₂ emissions

New Approach

Flash Ironmaking Process



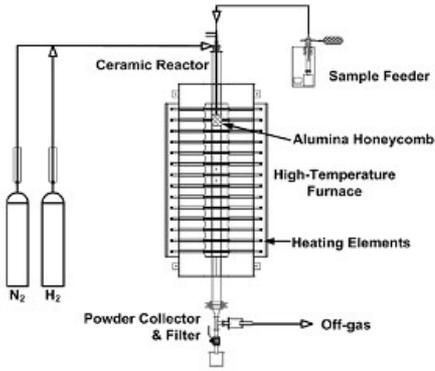
- Gas-Solid Suspension Reduction
Natural Gas, Hydrogen, Coal Gas
- Iron concentrate WITHOUT
 - Cokemaking
 - Pelletization
 - Sintering
- ✓ Significant Reduction in CO₂ & Energy Consumption
- ✓ Rapid reaction rate and favorable Net Present Value (NPV)

Technical Approach

- Install, commission & conduct test on a new large scale bench reactor at the University of Utah
- Multidisciplinary team:
 - American Iron and Steel Institute
 - ArcelorMittal USA
 - TimkenSteel
 - United States Steel Corporation
 - Berry Metal Company
 - Bench reactor fabrication
 - University of Utah
 - Lead Research Organization



Transition and Deployment

Project Objectives	Kinetic Feasibility Technology Road Map (2005-2007)	Proof of Concept at Lab Scale AISI CO ₂ Breakthrough (2008-2011)	Process Validation/ Scale-up Innovative Manufacturing Initiative (2012-2017)	Industrial Pilot TBD (2017+)
Experimental Apparatuses				<p>Approaches</p> <ol style="list-style-type: none"> 1. Large scale <u>75-100k tpy</u> 2. Modest-scale: <u>10-25k tpy</u> 3. Expand U of Utah work: <u>Similar to bench reactor but larger</u>
Funding	<p>Federal, \$350k Industry, \$150k Total, \$500k</p>	<p>Federal, \$ 0 Industry, \$ 4.8million Total, \$4.8million</p>	<p>Federal, \$ 8.2 million Industry, \$ 2.7 million Total, \$10.9 million</p>	<p>\$10 – 75million Funding TBD</p>

Transition and Deployment

- Benefits steel users and steel-related industry
- North American steel industry is end user
- To be used to produce iron as a raw material for steelmaking resulting in:
 - Direct use of iron ore concentrate
 - Lower capital cost
 - Scalable to large capacities
 - Avoidance of cokemaking
- Commercialization through licensing & royalty
- Sustainable as a more energy efficient and lower-emitting ironmaking process

Measure of Success

- If successful, iron will be produced at a lower cost, using less energy, and emitting less CO₂
- Potential energy savings: ~3.5 GJ/ton Fe vs. avg. BF
- CO₂ emission: Less than 36% vs. avg. BF process
- If 40% of US iron production is replaced by this process, only 3% of US natural gas production would be consumed.

Metric	H ₂ -based process	Reformerless natural gas process	Blast Furnace process
Energy Requirement (GJ/ton of hot metal)	11.3	14.5	18.0
CO ₂ emission (tons/ton of hot metal)	0.04	1.02	1.60

- NPV for standard case (15 year period): \$401M (2010)/(1 M tpy) Natural gas cost: \$5/M (2010) BTU HHV

Project Management & Budget

Task	Description	Milestones		
		Key Inputs	Criteria	Date
1	Bench Scale Reactor -Installation -Commissioning	Go/No Go Decision # 1: Operating Temperature Solid feed rate Operation time	1400°C >1 kg/hr >6 hr	11/30/2015
2	Testing Program -Existing lab flash reactor -Drop-tube reactor -Bench reactor -CFD model	Go/No Go Decision # 2: Metallization Min. amt. reducing gas Go/No Go Decision # 3: Metallization Min. amt. reducing gas Milestone # 4: Metallization Solid feed rate	95% 3.0x 95% 1.5x 95% >5 kg/hr	6/30/16 11/30/16 6/30/17
3	Industrial pilot reactor -Design -Cost estimate			
4	Program Administration			8/31/17

Total Project Budget	
DOE Investment	\$ 8,200,000
Cost Share	\$ 2,700,000
Project Total	\$10,900,000

Results and Accomplishments

- Commissioning complete; process milestones met Q4 2015
 - Achieved and held 1400°C for eight hours
 - Achieved prescribed gas and material flow rates



Next Steps

- Begin experimental program aimed at operational flexibility, scale-up costs, process control and optimization.
- Continued process modeling
- Additional milestones later in 2016