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# Hydrogen Home Refueling

Status, Key Issues, and Challenges



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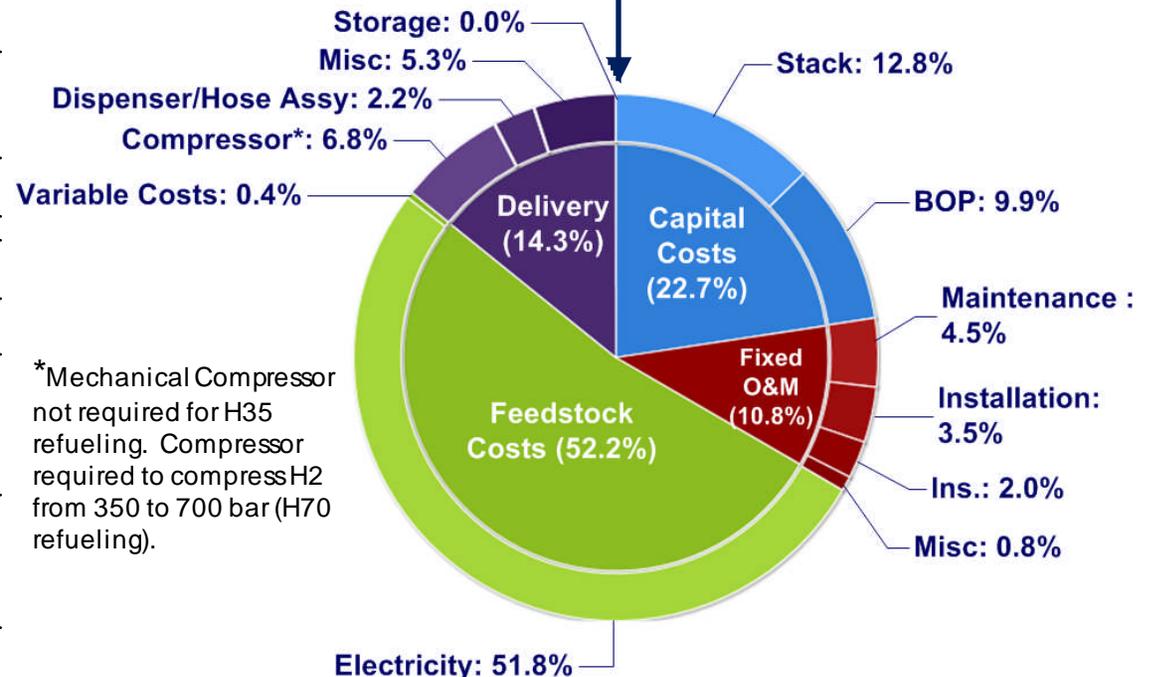
**Giner, Inc.**

89 Rumford Ave,  
Newton, Ma. 02466

# Home Refueling Costs

Based on Forecourt H2A Model (Ver. 3.0)

H <sub>2</sub> Production Cost Contribution	DOE Target	Home Refueler
	(2020)	(2013)
Capital Costs	\$0.50	\$1.05
Fixed O&M	\$0.20	\$0.50
Feedstock Costs System Efficiency: 65 kWh <sub>e</sub> /kg -H <sub>2</sub>	\$1.60 (\$0.037/kW)	\$2.40 (\$0.037/kW)
Other Variable Costs (including utilities)	<\$0.10	\$0.02
<b>Total Hydrogen Production Cost (\$/kg)</b>	<b>2.30</b>	<b>3.98</b>
Delivery (CSD)	\$1.70	\$0.66 (5,000 psig output, no Storage or Forecourt Station Requirements)
<b>Total Hydrogen Production Cost (\$/kg)</b>	<b>&lt;4.00</b>	<b>4.64</b>

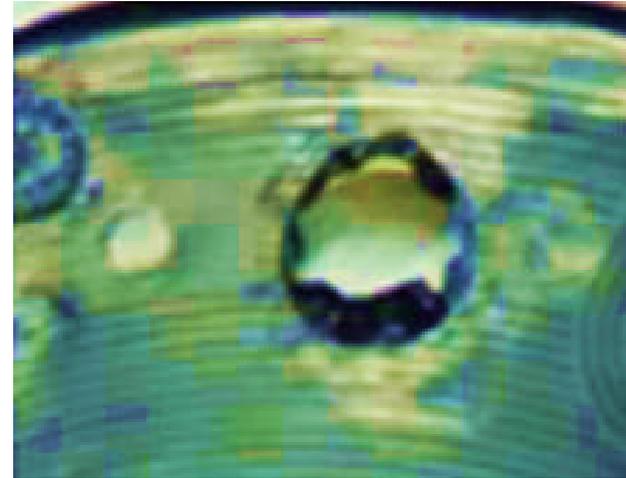


\*Mechanical Compressor not required for H35 refueling. Compressor required to compress H<sub>2</sub> from 350 to 700 bar (H70 refueling).

- H2A Ver. 3 includes higher installation costs and higher pressure requirement for H70 hydrogen refueling
  - Hydrogen pressure requirement 12,688 psig (previously 6,250 psig)
- **Progress inline with achieving new 2020 Target of <\$4.00/kg-H<sub>2</sub>**
  - Delivery: No Storage (or forecourt station costs)
  - Can achieve <\$4.00 kg/H<sub>2</sub> for 5,000 psig vehicle refueling
  - Improving stack output pressure to 12,000 psig is required to meet 2020 target for H70 refueling

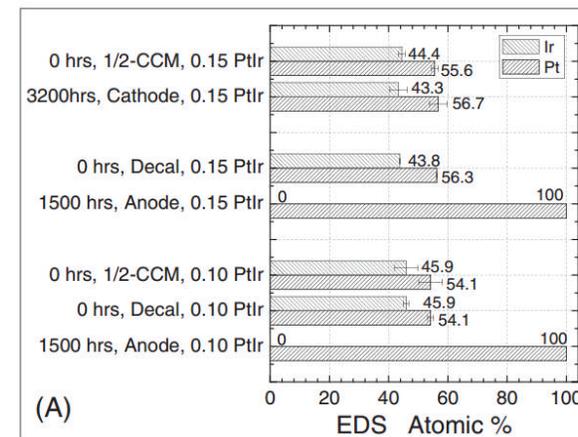
# Home Refueling Issues: Technical Challenges

- Components
  - Membrane
    - Permeability
    - Creep (Sealing)
    - Degradation
  - Catalyst
    - Anode Dissolution
  - Separators
    - H<sub>2</sub> Embrittlement
- Safety



Membrane operated under 5000 psid

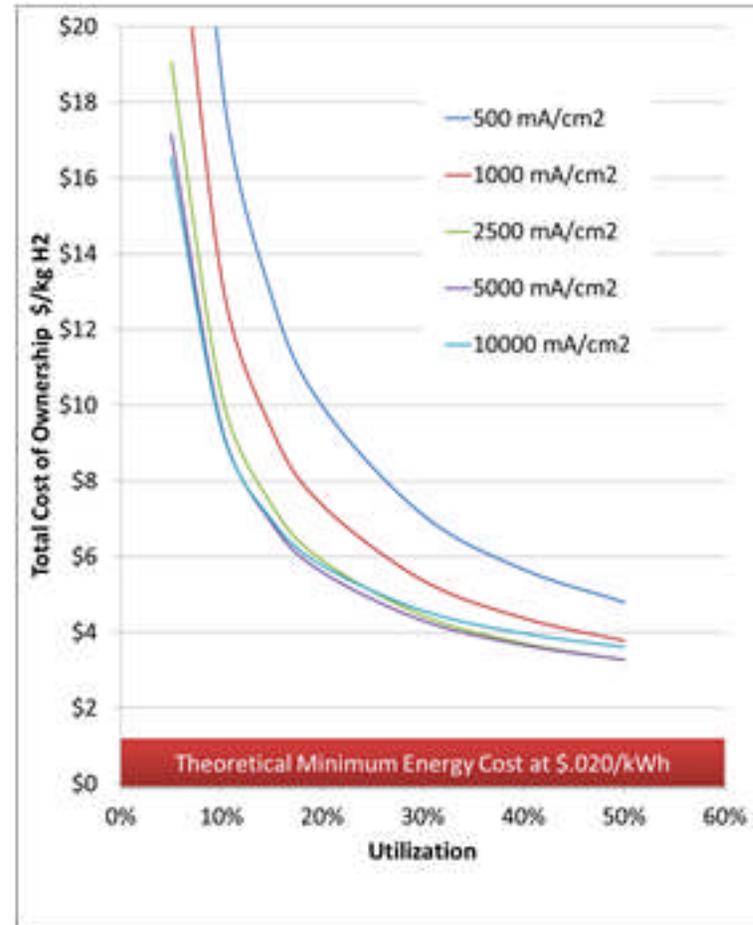
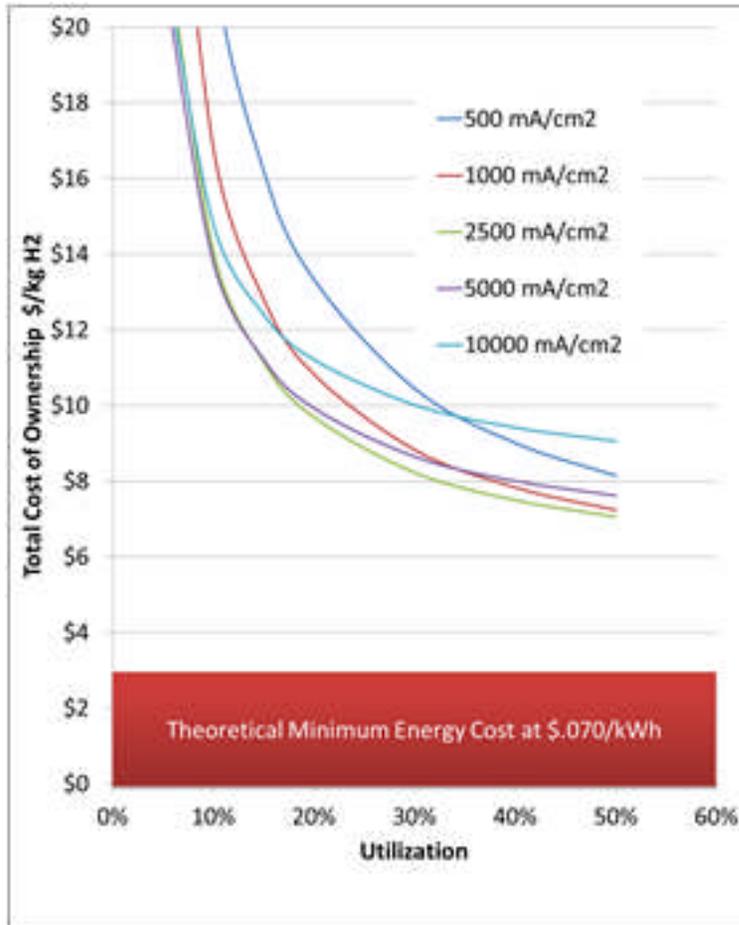
Ir shown to be unstable in NSTF catalysts



Debe et al. Journal of The Electrochemical Society, 159(6) K165-K176 (2012)

# Home Refueling Issues: Cost

0.2 kg/hr System 5000 psi with no further compression



High utilization and energy contracts securing low-cost overnight are essential

## Home Refueling: Technical Needs

- Better Membrane
  - PFSA membranes developed for automotive fuel cells are a poor match
  - Permeability is too high
  - Mechanical Properties are too weak
  - Low EW not nearly as critical
- Lower catalyst cost
  - Increased Catalyst Activity
  - Higher Temperature
  - More important than in large scale electrolyzers
- Failure Testing
  - Develop methods to reduce, quantify risks
- Accelerated Testing Methods

# Home Refueling: Fundamental Questions

In general these things are well qualified for PEM fuel cells, but just touching surface for electrolysis

- How does Temperature effect OER kinetics
  - High activation energy up to 80°C then changes
- Hydrocarbon Membranes
  - Stable in full hydration
  - Better (lower) Permeability?
  - Effect on Electrode Kinetics
- AEMs?
  - Potential of negligible catalyst costs
  - Permeability/conductivity ratio?
- Catalyst Stability Factors
  - Temperature
  - Pressure
  - Voltage Cycling

