

# Lean Gasoline Emissions Control: NH<sub>3</sub> generation over commercial Three-Way Catalysts and Lean-NOx Traps

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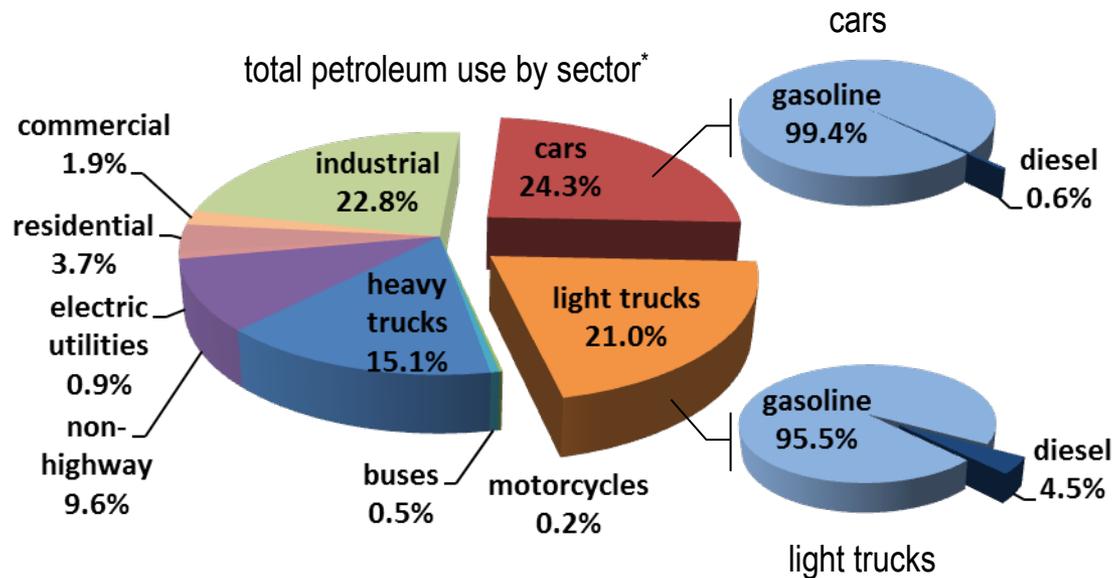
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University of South Carolina

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# Small improvements in gasoline fuel economy significantly decreases fuel consumption



***Lean gasoline vehicles can decrease US gasoline consumption by ~30 million gal/day***

- 132,000 million gallons of fuel used by cars and light trucks annually\*\*
- **New car and light-truck sales dominated by gasoline engines**
- 10% fuel economy benefit † from base case of 22.6/18.1 mpg\*\* has big impact
  - Saves >200,000,000 barrels gasoline annually
  - 5% of overall petroleum used
- **HOWEVER...emissions control challenges exist**

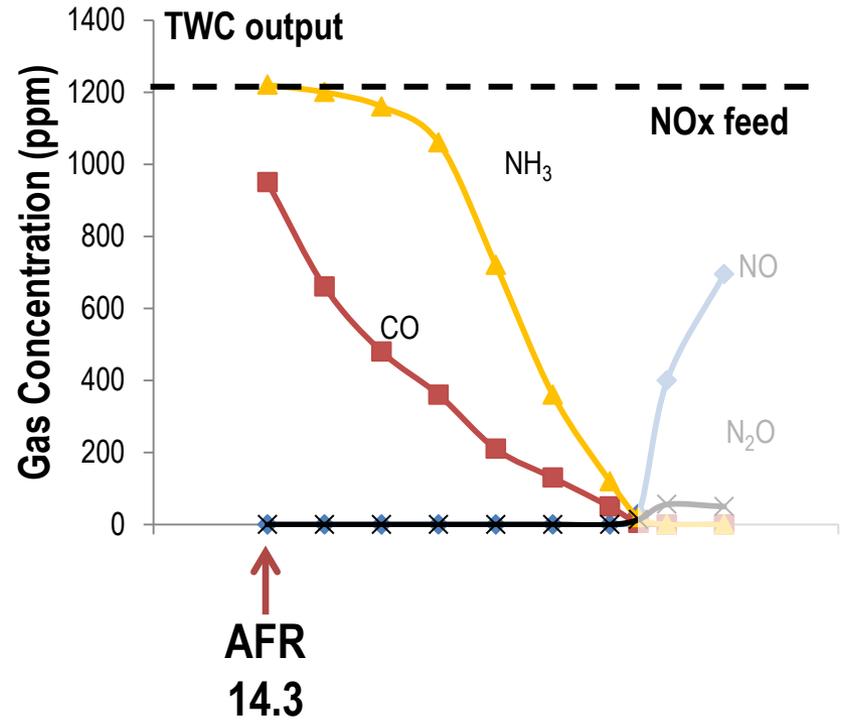
# Why NH<sub>3</sub>-generation on TWCs?

- Zeolite-based NH<sub>3</sub>-SCR has been shown to have very high NO<sub>x</sub> conversions over wide temperature window
- Urea injection systems are unlikely solution in lean gasoline systems
  - Significant additional cost would deter consumers
  - Higher engine out NO<sub>x</sub> will require more urea
    - introducing urea filling infrastructure issues on this scale
  - Other NH<sub>3</sub> introduction methods being studied
- Utilizing existing TWCs on gasoline vehicles is intriguing since they are already on the vehicle and will be needed on lean gasoline vehicles
  - NH<sub>3</sub> generation recently explored in “Passive SCR” approach\*
- Goal is to investigate potential of using similar levels of PGM on TWC
  - while maximizing lean timing and minimizing fuel penalty

\* - GM: SAE 2011-01-0306, SAE 2010-01-0366

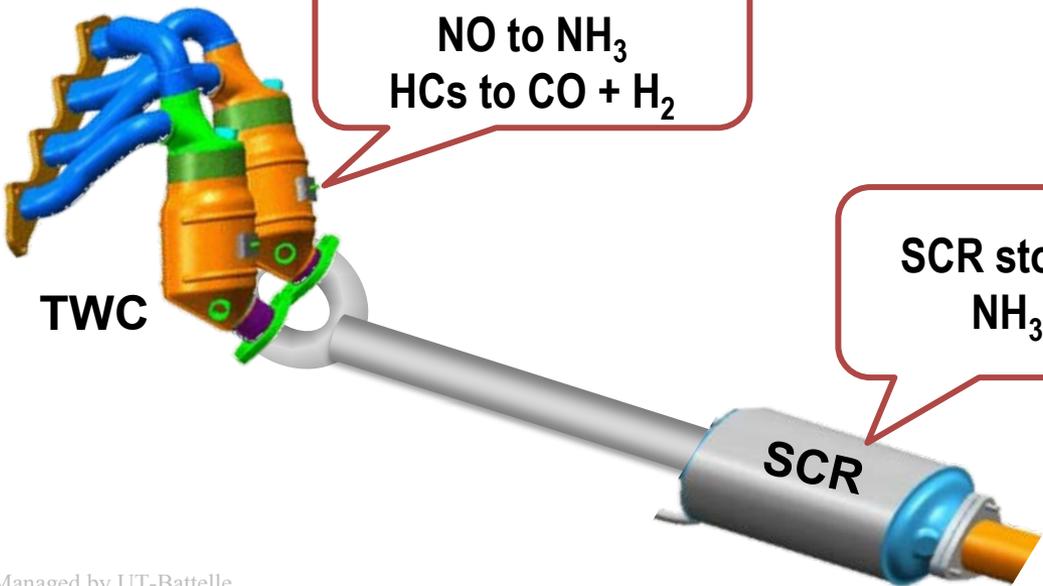
# “Passive” SCR for lean gasoline emissions control

slightly rich operation  
AFR  $\approx$  14



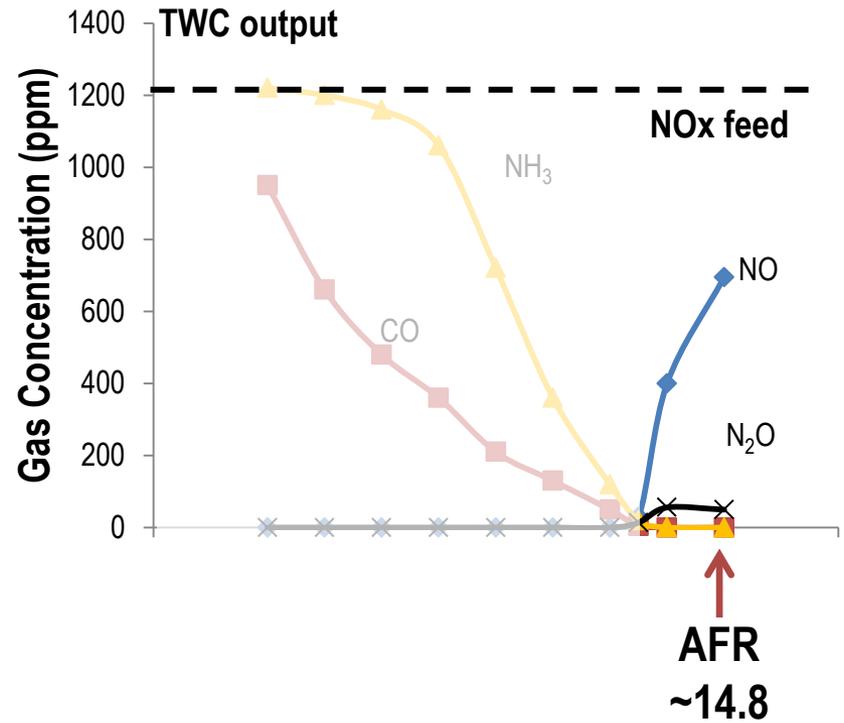
TWC converts:  
NO to NH<sub>3</sub>  
HCs to CO + H<sub>2</sub>

SCR stores  
NH<sub>3</sub>



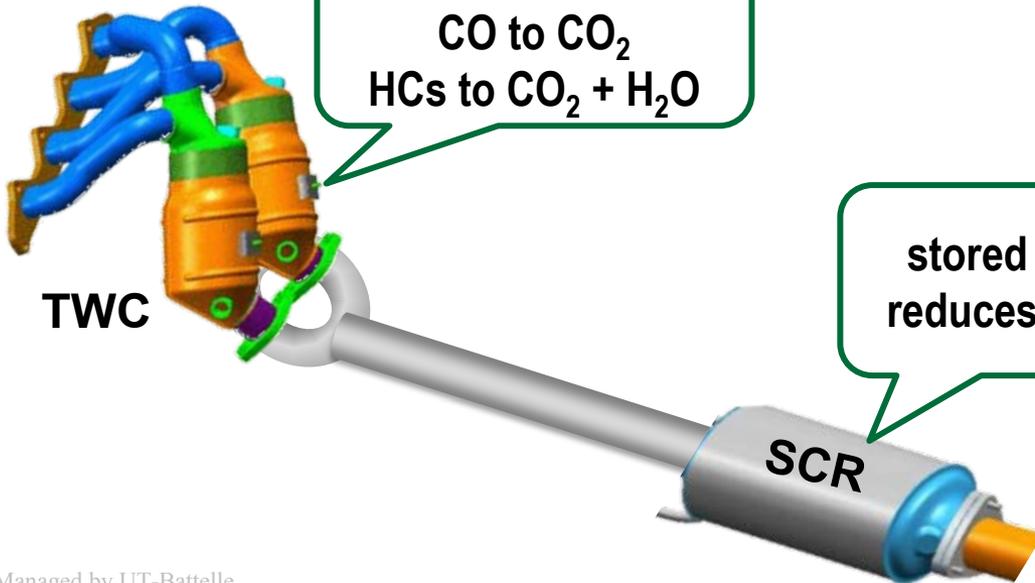
# “Passive” SCR for lean gasoline emissions control

lean operation  
AFR  $\approx 24$



TWC converts:  
CO to CO<sub>2</sub>  
HCs to CO<sub>2</sub> + H<sub>2</sub>O

stored NH<sub>3</sub>  
reduces NOx

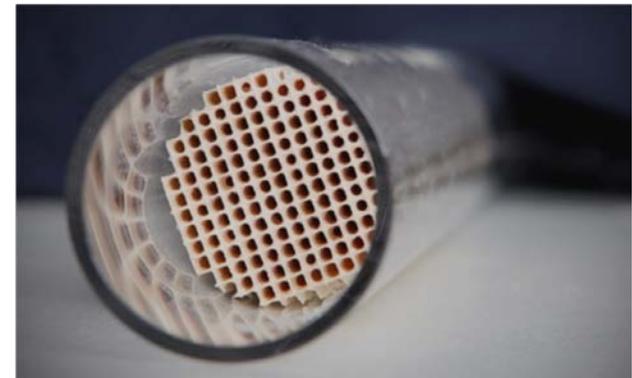
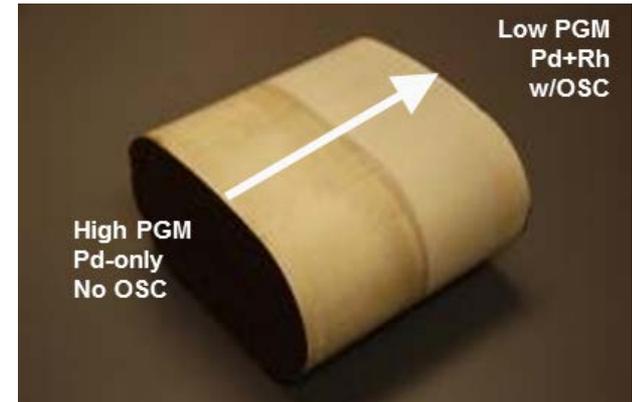


# **NH<sub>3</sub> GENERATION IN BENCH REACTORS**

# TWC and LNT studied in bench-core reactor with varying PGM content

- For bench reactor, focusing on modern TWC technology

- 1.3L TWC is a 2 formulation combination (combo)
  - Total PGM: 0/4.0/0.16 g/L Pt/Pd/Rh (118 g/ft<sup>3</sup> total PGM)
- Front 0.6L of TWC is Pd-only no Ce
  - High PGM: 0/6.7/0 g/L Pt/Pd/Rh (190 g/ft<sup>3</sup> total PGM)
  - No ceria-based OSC, but oxygen storage measured
    - Expected to proceed via Pd-O formation
- Rear 0.7L of TWC is Pd/Rh+Ce w/ Ceria
  - Low PGM: 0/1.1/0.3 g/L Pt/Pd/Rh (40 g/ft<sup>3</sup> total PGM)
- Investigating each portion individually and in combined form
  - Degreened at 16h at 700C in humidified air (2.7% H<sub>2</sub>O)



- LNT is commercial formulation from lean gasoline BMW

- 2.6L Pt/Pd/Rh = 7/3/1, 3.3 g/L-cat (94 g/ft<sup>3</sup>); Ba loading: 20 g/L (560 g/ft<sup>3</sup>); Ce: 56 g/L (1600 g/ft<sup>3</sup>)
- Degreened at 16h at 700°C in humidified air (2.7% H<sub>2</sub>O)

# TWC is effective and tunable NH<sub>3</sub> generator

- **Example feed conditions:**

~AFR	O <sub>2</sub>	NO	CO	H <sub>2</sub>	C <sub>3</sub> H <sub>6</sub>
14.6	1.59%	0.12%	1.80%	0.60%	0.10%
14.4	1.34%	0.12%	1.80%	0.60%	0.10%
14.2	1.06%	0.12%	1.80%	0.60%	0.10%

- **NH<sub>3</sub> readily generated; varies with PGM**

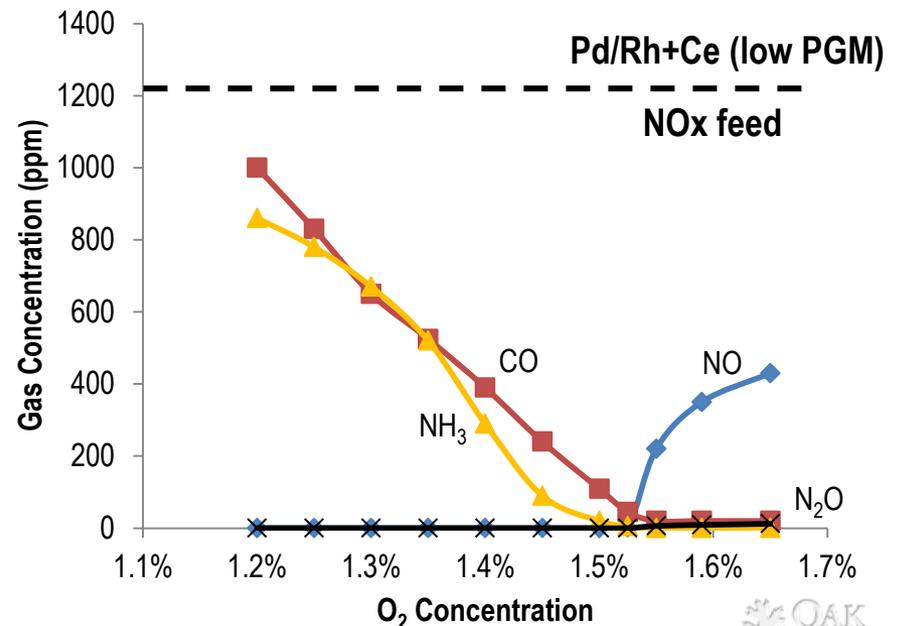
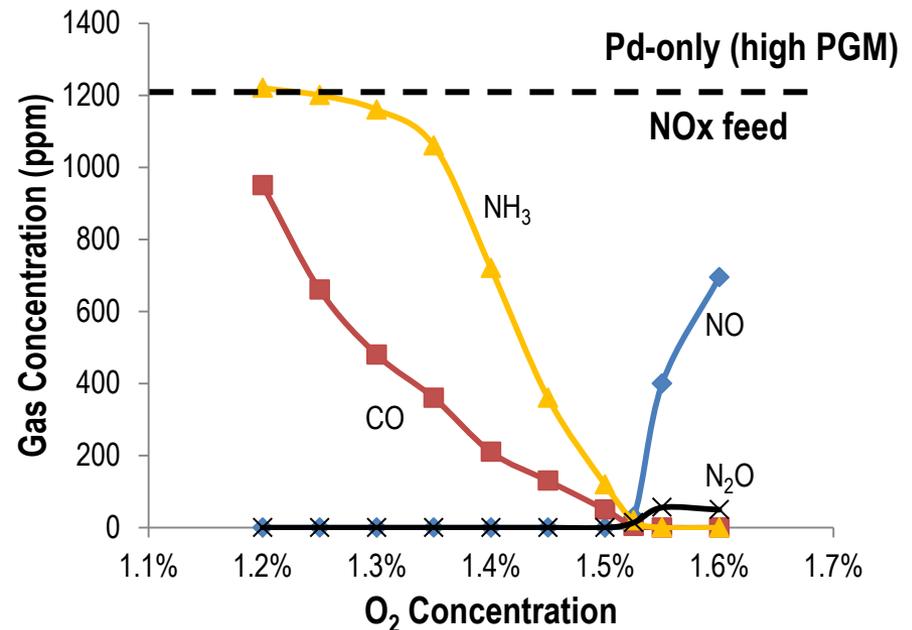
- For Pd-only TWC with high PGM:
  - All NO fed converted to NH<sub>3</sub> when very rich
- For Pd/Rh+Ce (low PGM) TWC:
  - NH<sub>3</sub> production is still significant but reduced

- **At all conditions, >95% CO conversion**

- C<sub>3</sub>H<sub>6</sub> not observed in effluent

- **N<sub>2</sub>O formation observed under lean conditions and varies with PGM content**

- Up to 56 ppm with high PGM (Pd-only) TWC
- Less than 10 ppm with low PGM (Pd+Rh) TWC

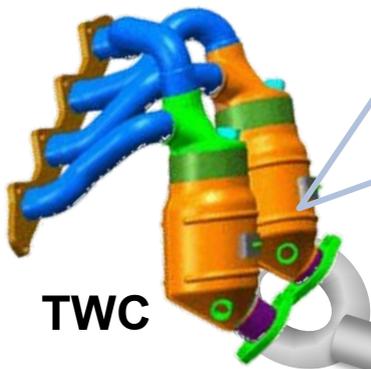
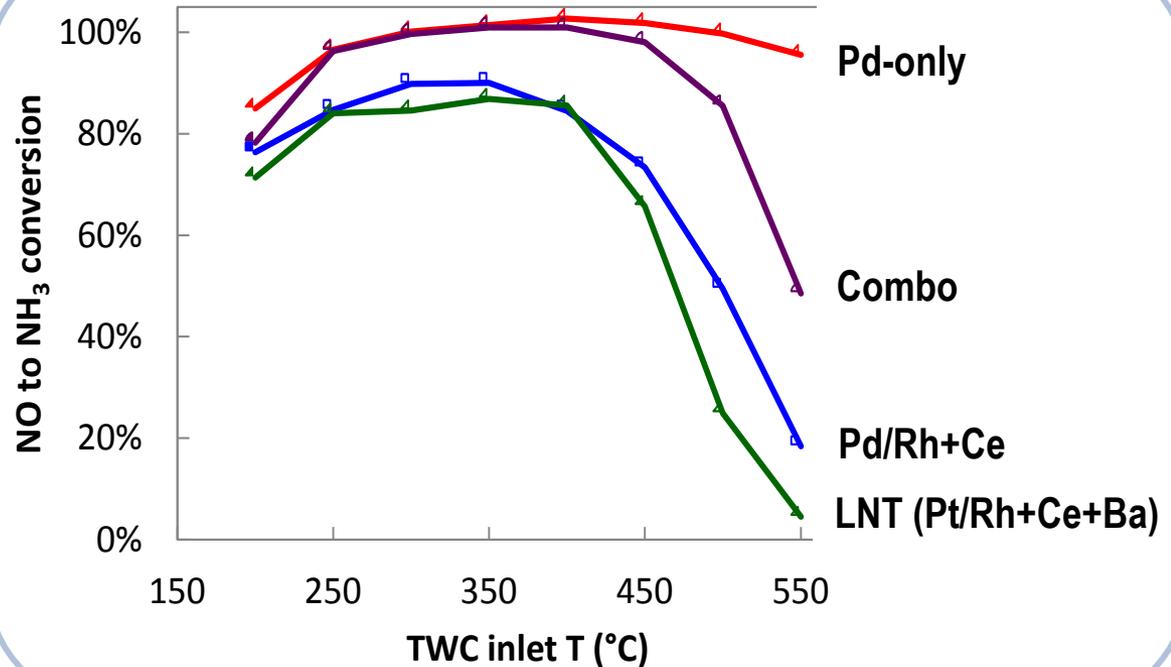


Midbed Temperatures: 460-500°C



# PGM content and Pt/Pd/Rh ratios impact NH<sub>3</sub> production

Evaluated multiple upstream catalyst formulations for NH<sub>3</sub> generation



TWC

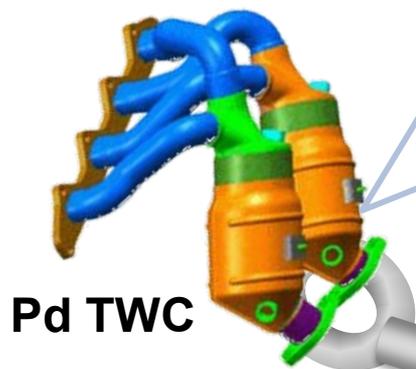
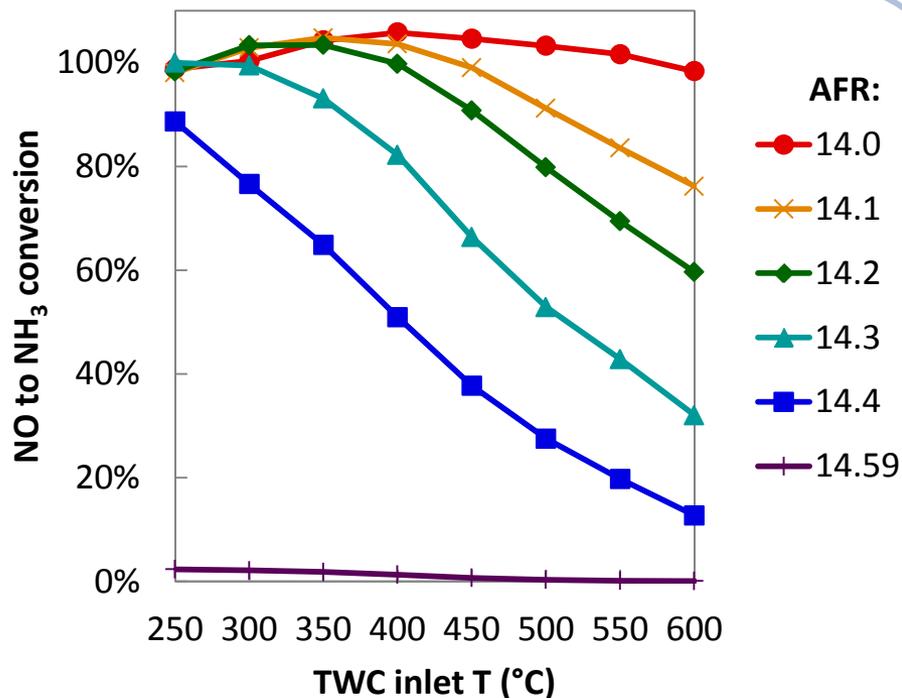
High PGM (Pd-only) best for NH<sub>3</sub> generation



SCR

# AFR and temperature dictate $\text{NH}_3$ production

Quantified  $\text{NH}_3$  generation  
over Pd only TWC

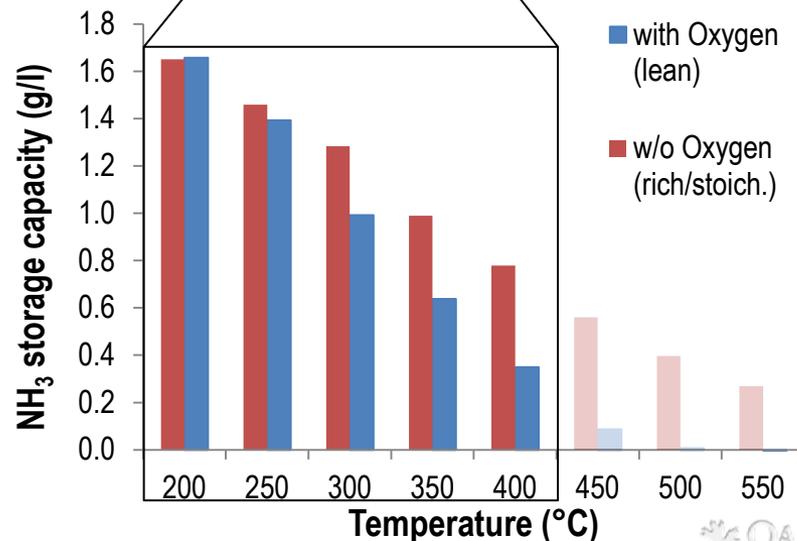
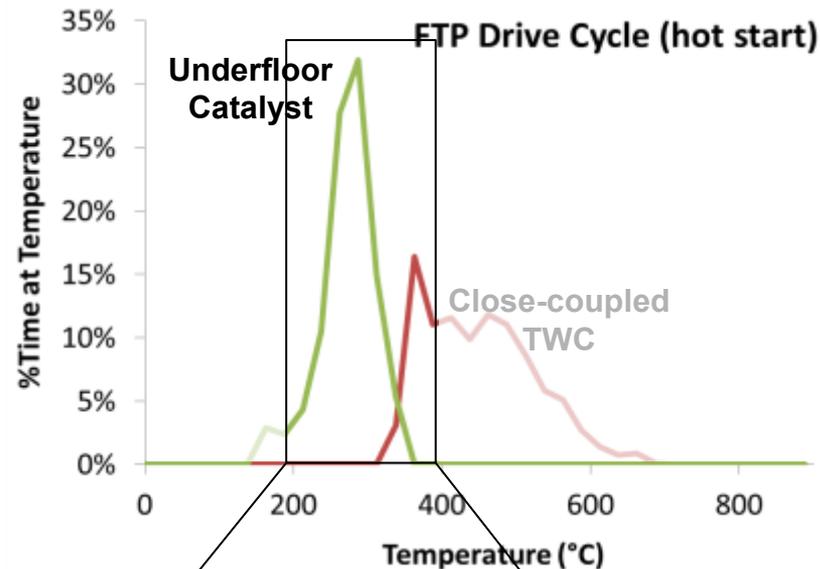


$\text{NH}_3$  generated over wide T window  
Need richer conditions at higher T



# NH<sub>3</sub> production over LNT and TWC occurs at temperatures relevant to vehicle operation and NH<sub>3</sub> storage on SCR

- Histogram of catalyst temperatures during drive cycle with BMW 120i
  - FTP (hot start)
  - 200-350°C for underfloor catalyst
  - 350-600°C for close-coupled (cc) TWC
- TWC: tunable NH<sub>3</sub> production 250-600°C
- NH<sub>3</sub> production temperatures over cc-TWC mesh well with NH<sub>3</sub> storage temperatures on underfloor SCR
  - More NH<sub>3</sub> storage occurs under rich/stoichiometric conditions
  - However switching from rich to lean will result in NH<sub>3</sub> release if over-saturated



# PASSIVE SCR APPROACH IN BENCH REACTOR

# Fully-automated two furnace bench reactor employed with TWC and SCR

## Lean

600 ppm NO<sub>x</sub>

8% O<sub>2</sub>

5% H<sub>2</sub>O, 5% CO<sub>2</sub>, Bal. N<sub>2</sub>

- Switches from lean to rich when FTIR reads 20 ppm NO<sub>x</sub>

## Rich

1200 ppm NO<sub>x</sub>

1.8% CO

0.6% H<sub>2</sub>

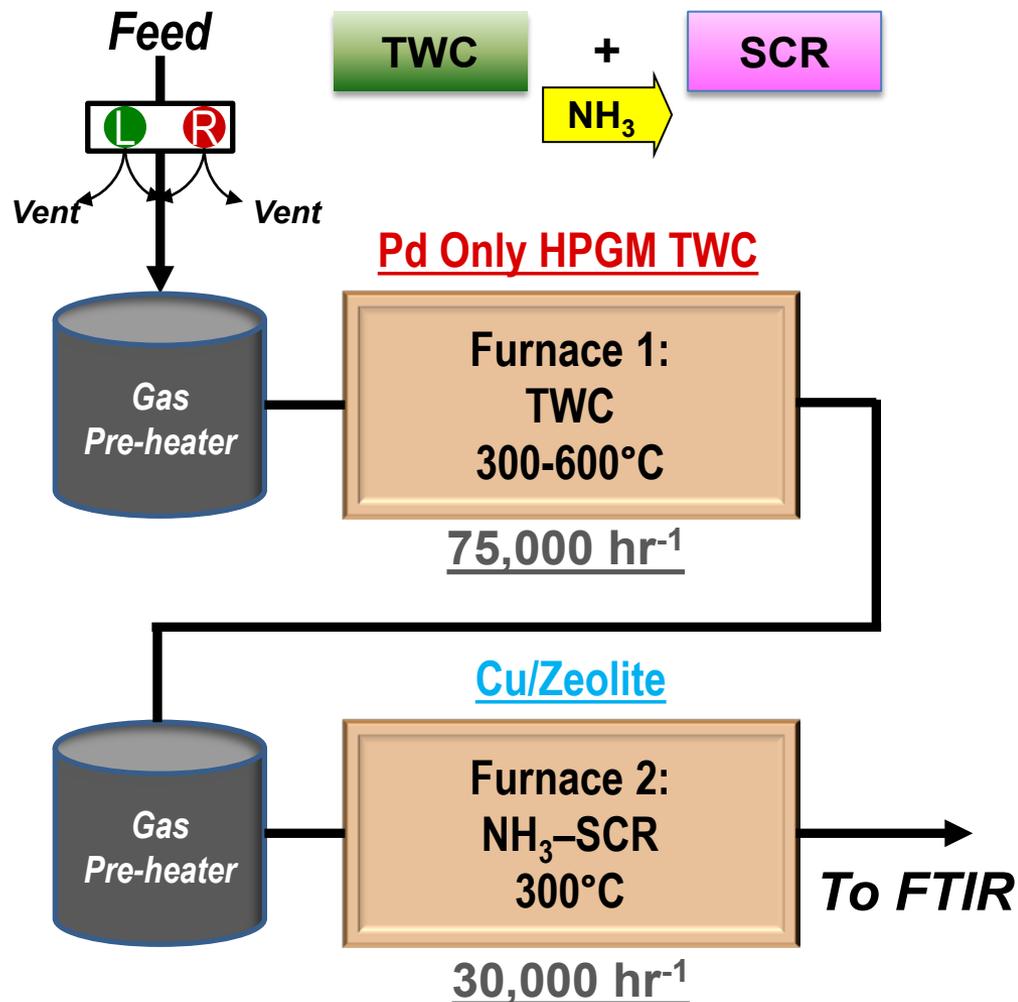
0.1% C<sub>3</sub>H<sub>6</sub>

0.79%, 0.98%, 1.06%, 1.20% :O<sub>2</sub>

14.0 14.1 14.2 14.3 :AFR

5% H<sub>2</sub>O, 5% CO<sub>2</sub>, Bal. N<sub>2</sub>

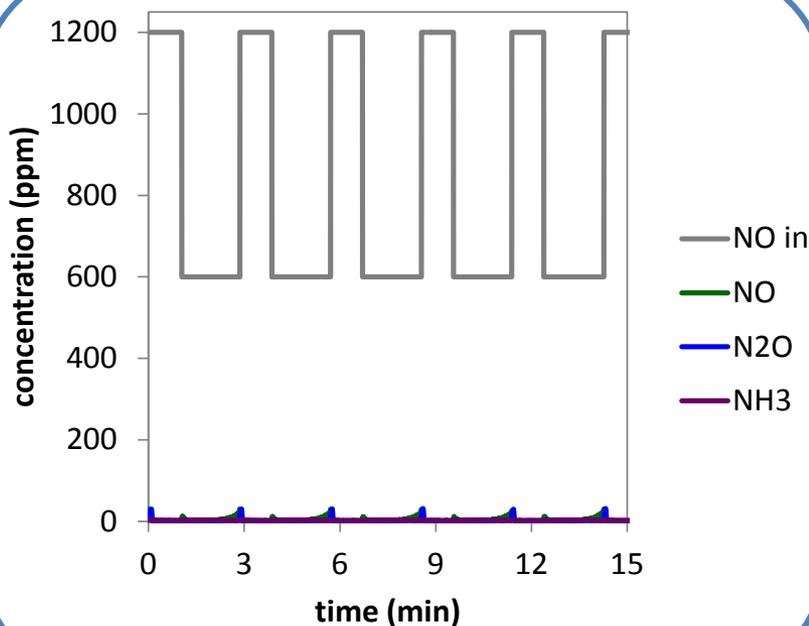
- Rich to lean when predicted NH<sub>3</sub> storage is half filled



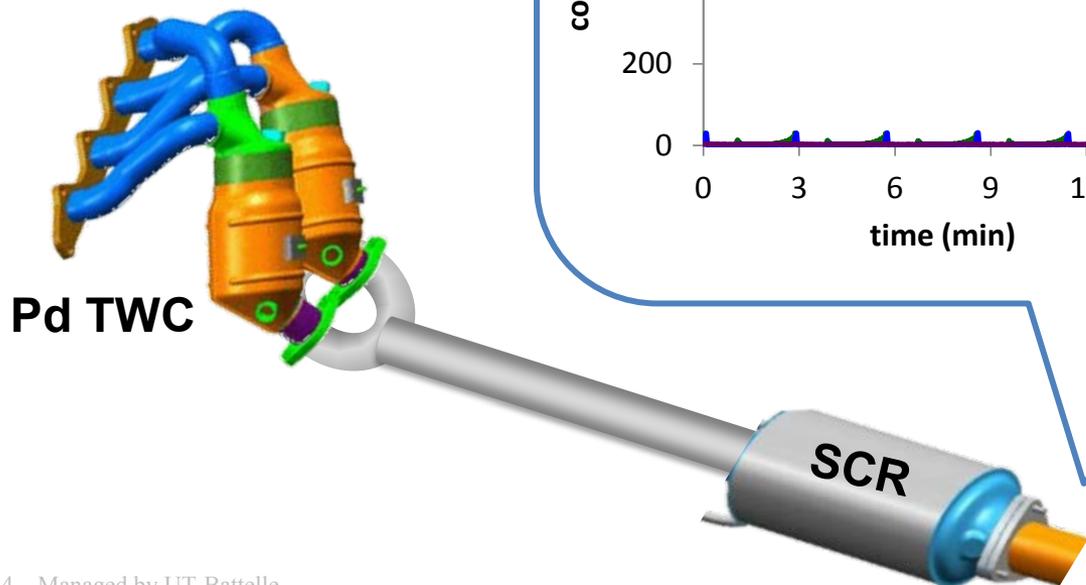
# Manual optimization of cycling illustrates the potential of this approach

## Flow reactor proof of concept: TWC+SCR under cyclic operation

**TWC inlet** 450 °C  
**SCR inlet** 300 °C  
**rich time** 60 s (AFR $\approx$ 14)  
**lean time** 110 s (AFR $\approx$ 24)  
**NOx conv.** 99.5%  
**CO conv.** 93.9%

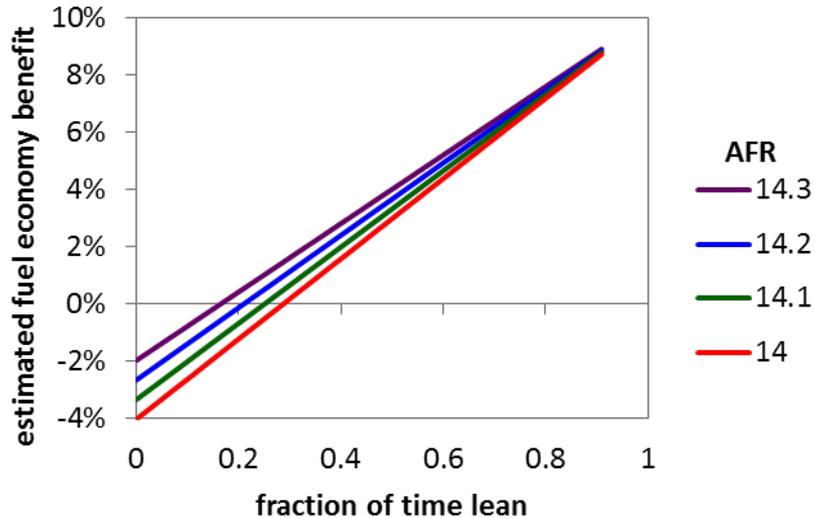


	avg (ppm)	max (ppm)
NO	4	31
N <sub>2</sub> O	2	32
NH <sub>3</sub>	3	4
CO	1200	3900



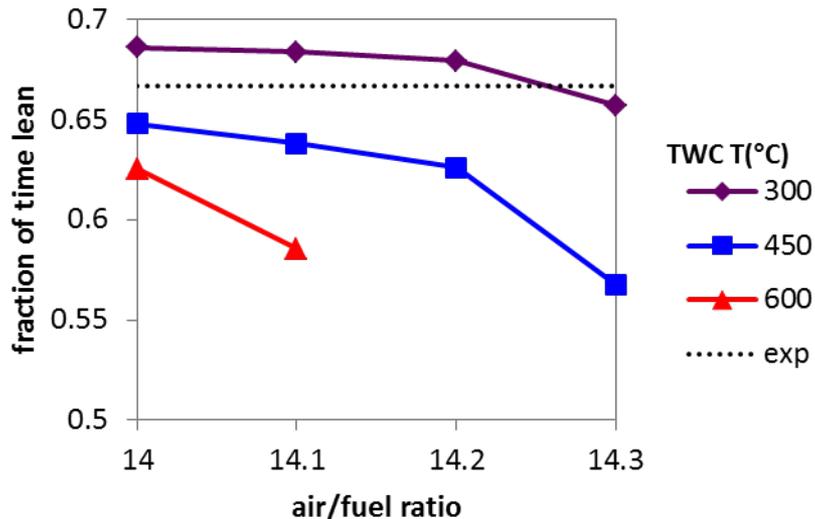
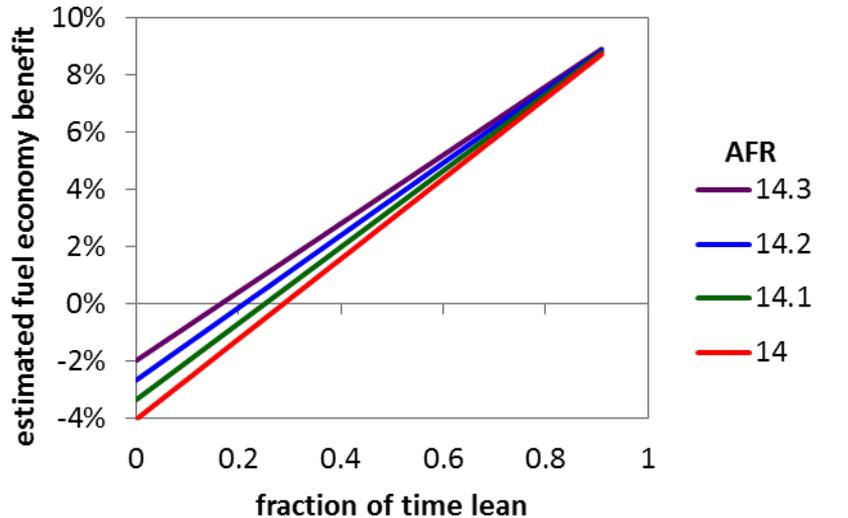
**Estimated fuel economy gain: 5-6%**

# Fuel economy impacts of NOx emissions compliance with passive SCR



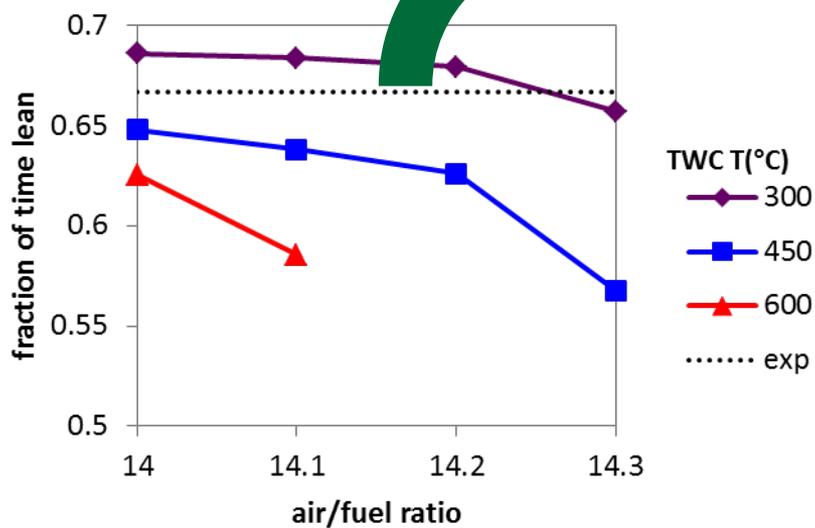
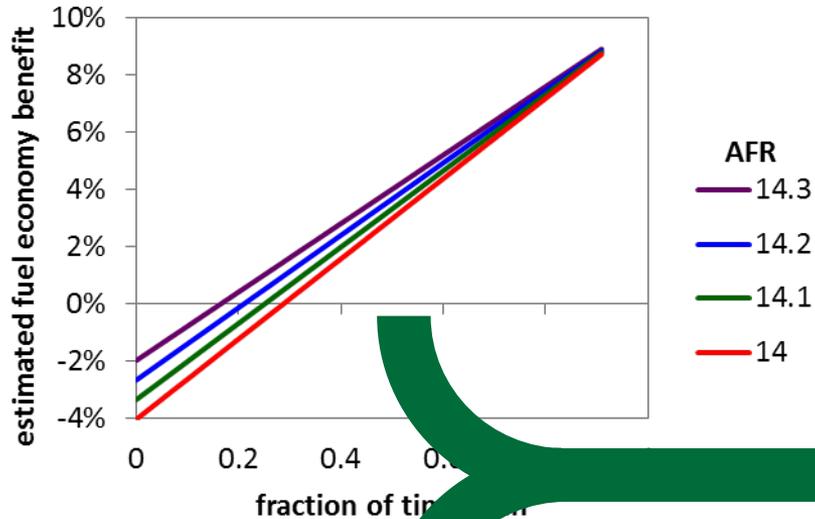
- Rich excursions to generate  $\text{NH}_3$  increase fuel consumption due to:
  - temporary loss of lean operation  
fuel economy boost (assumed 10%)
  - injection of excess fuel
- Overall impact on fuel economy depends on:
  - how long the engine can run lean
  - how rich it must go to generate  $\text{NH}_3$

# Fuel economy impacts of NOx emissions compliance with passive SCR

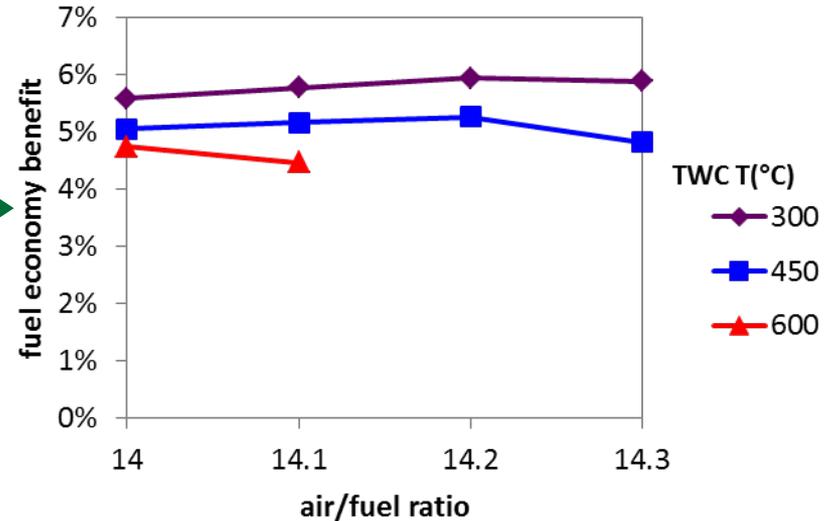


- Fraction of time lean depends on:
  - NH<sub>3</sub> yield during rich operation
    - decreases with TWC T and AFR
  - relative NOx flux (concentration and flow rate) during rich vs. lean
    - rich NOx = 2 x lean NOx here
- Exploiting flow changes during transient driving could increase lean operation time
- Higher than expected lean time at 300°C due to NOx storage over TWC during lean operation
  - possible formulation strategy
- For all conditions shown NOx conversion is > 99%

# Fuel economy impacts of NOx emissions compliance with passive SCR



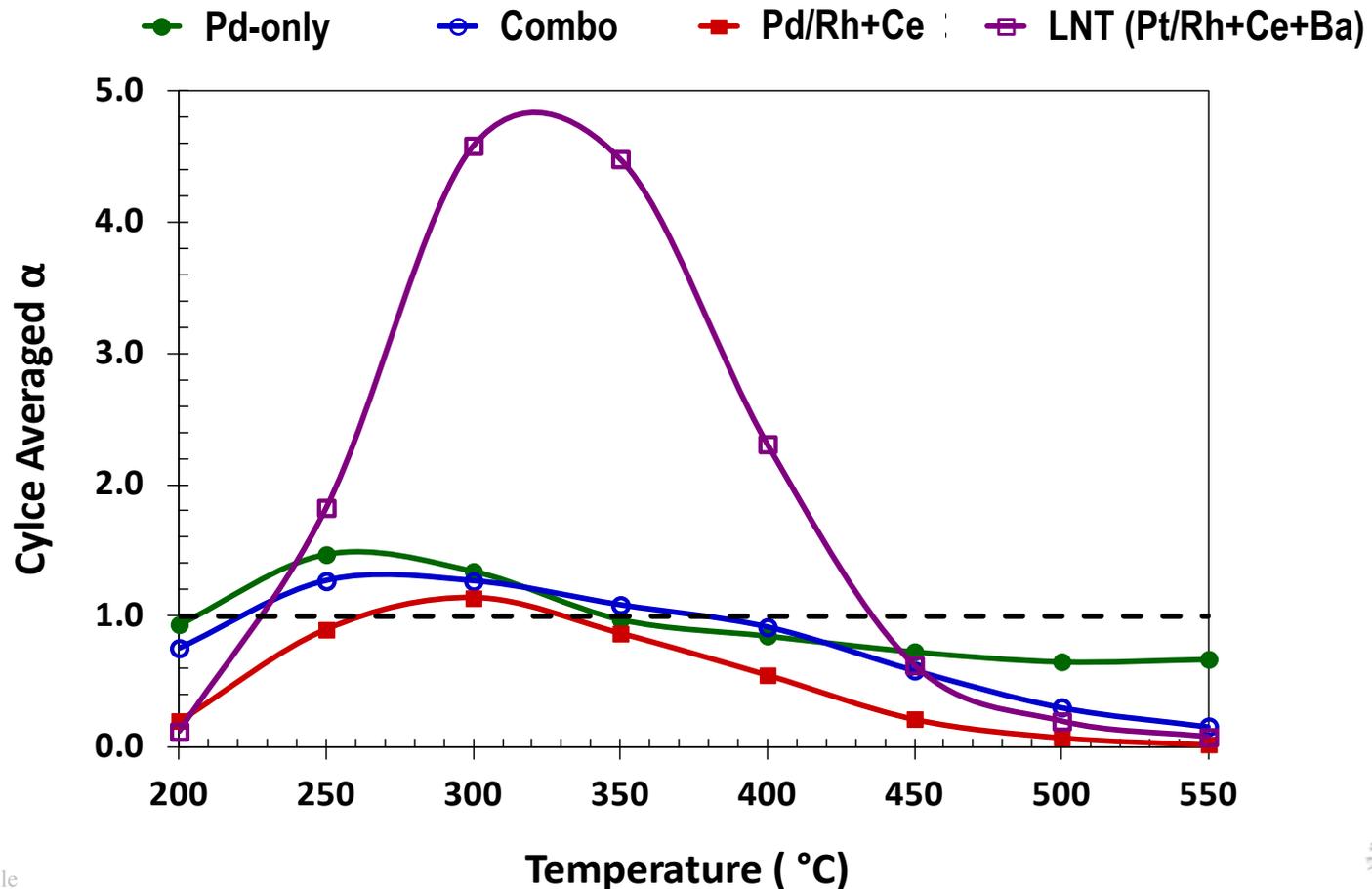
- Current implementation of passive SCR generates a net fuel economy benefit of 5-6% over a comparable stoich. engine
- Optimal AFR depends on TWC T



- Possibilities for reducing fuel penalty:
  - higher NOx flux ratios during transient operation on vehicle
  - addition of a NOx storage material

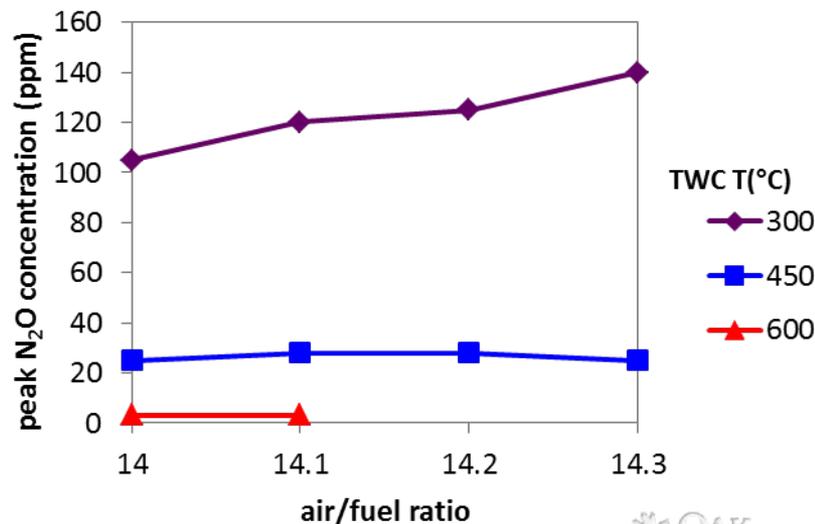
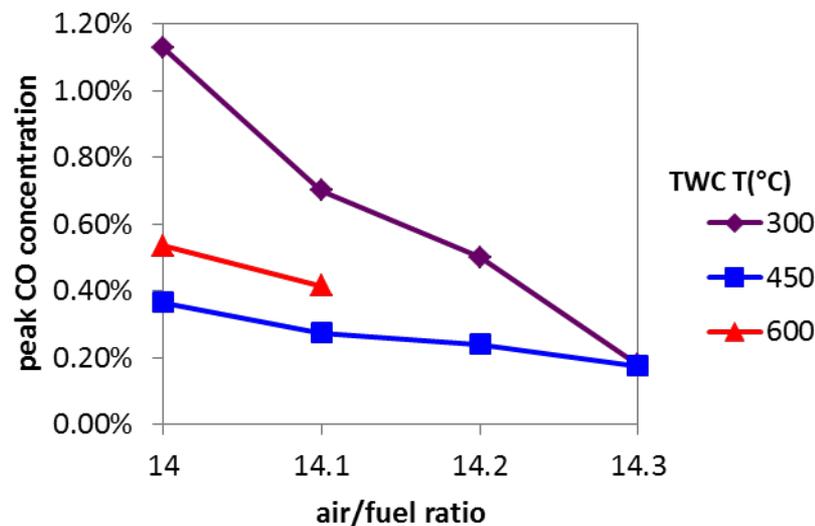
# For a fixed cycle, addition of NO<sub>x</sub> storage significantly increases NH<sub>3</sub> formation

- Cycle Averaged Alpha is 3+ times higher than best TWC formulation
  - Alpha: NH<sub>3</sub> produced / NO<sub>x</sub> in effluent



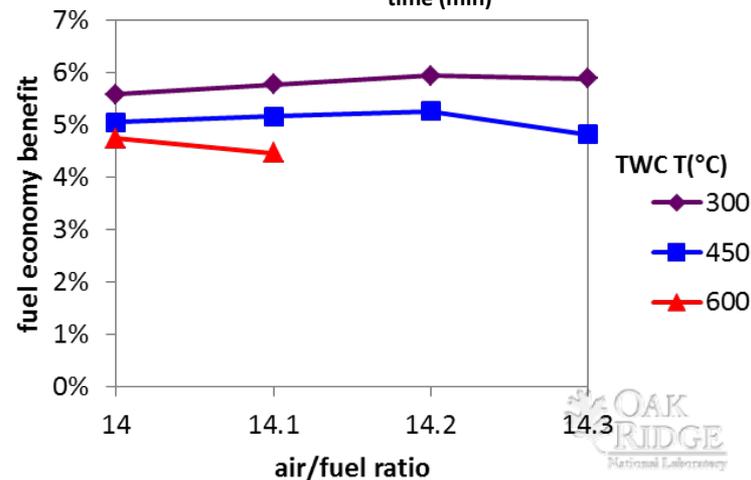
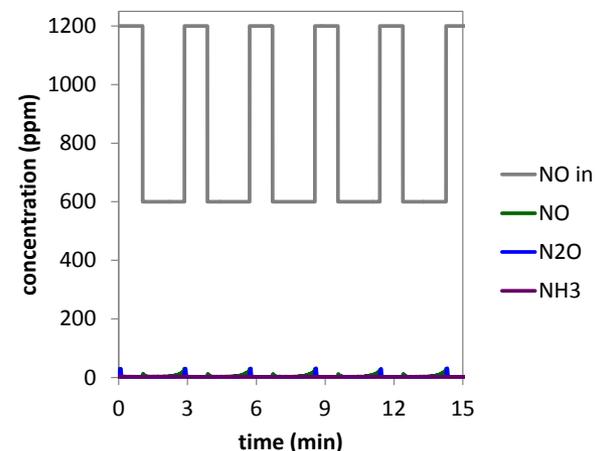
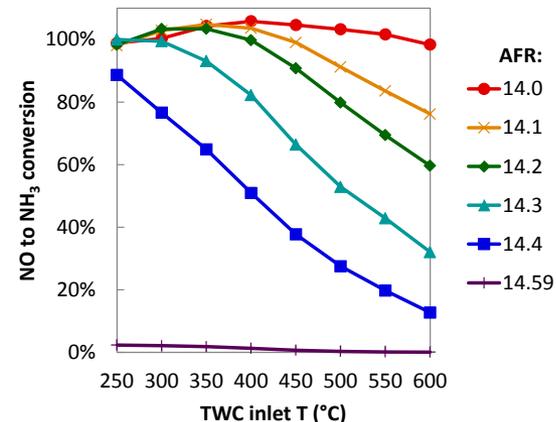
# Emissions other than NOx still present potential challenges

- Current operating strategies optimized for NOx reduction
- Minimal HCs observed with 0.1% C<sub>3</sub>H<sub>6</sub> in feed
  - Consumed by reactions with NOx, O<sub>2</sub>, or steam reforming
- Significant CO slips during rich operation
  - higher AFRs reduce but do not eliminate
  - CO slip a complicated function of TWC temperature due to water-gas shift kinetics and thermodynamics
  - downstream cleanup catalyst and secondary air may be required
- N<sub>2</sub>O may be problematic at low TWC temperatures
  - potential for mitigation by changes in formulation or operating strategy



# Summary

- TWCs shown to be able to produce  $\text{NH}_3$  over a broad temperature window
  - Key variables are PGM content, temperature and AFR
- Greater than 99%  $\text{NO}_x$  conversion observed in passive approach
  - Lean-only conversion is >98%
  - CO slip is a concern and will need to be accounted for
- Significant fuel economy gain realized which could be improved with  $\text{NO}_x$  storage on TWC
  - Future efforts exploring addition of  $\text{NO}_x$  storage component on Pt-free TWC



# Acknowledgements

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  - Gurpreet Singh and Ken Howden
- **University of South Carolina**
  - Graduate Student support of Chris DiGiulio
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  - Wei Li, Chang Kim, Kushal Narayanaswamy, Paul Nagt
- **Umicore**
  - Catalysts and Monthly teleconferences
  - Chris Owens, Ken Price, Doug Ball, Tom Pauly, Corey Negohosian
- **University of Wisconsin**
  - Modeling (not discussed here) and Monthly teleconferences
  - Chris Rutland and Jian Gong

# ADDITIONAL SLIDES

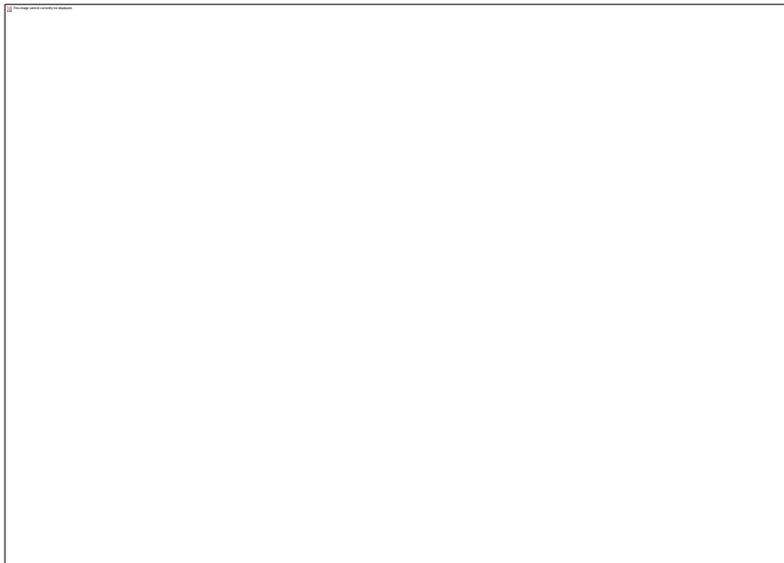
# Reaction Conditions

Lambda	AFR	O <sub>2</sub>	NO	CO	H <sub>2</sub>	C <sub>3</sub> H <sub>6</sub>
1.000	14.59	1.59%	0.12%	1.80%	0.60%	0.10%
0.996	14.54	1.525%	0.12%	1.80%	0.60%	0.10%
0.995	14.52	1.51%	0.12%	1.80%	0.60%	0.10%
0.987	14.40	1.34%	0.12%	1.80%	0.60%	0.10%
0.973	14.20	1.06%	0.12%	1.80%	0.60%	0.10%
0.960	14.00	0.79%	0.12%	1.80%	0.60%	0.10%

# BMW lean GDI LNT benchmarking against CLEERS reference

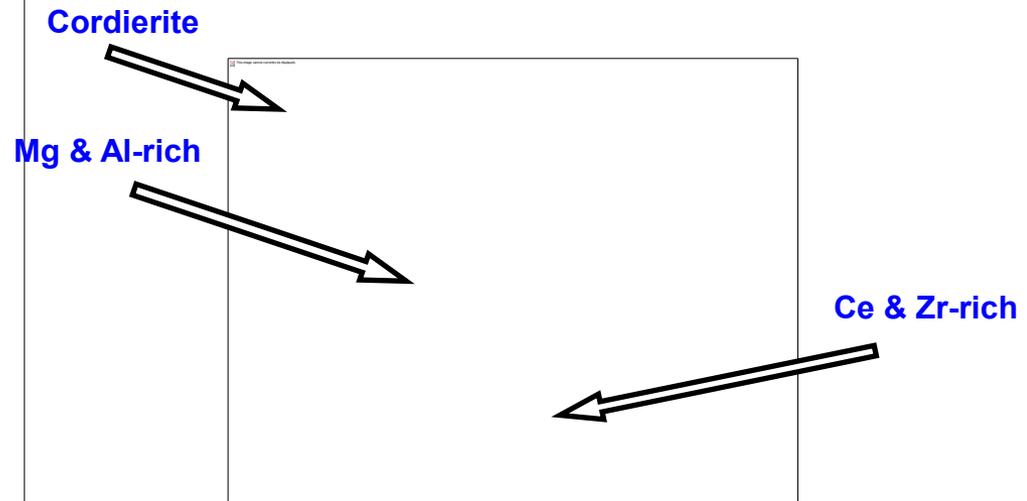
## CLEERS reference

Lean GDI, 2004, provided by Umicore



## New LNT

Lean GDI, 2009, from BMW 120i vehicle



	CLEERS reference	New LNT
Cell density (cps)	625	413
Ba loading (g/ft <sup>3</sup> )	442	565
PGM loading (g/ft <sup>3</sup> )	103	94
Pt/Pd/Rh ratio	8/3/1	7/3/1

- Responsive to FY10 review comments
- Initial characterization indicates similar basic components in both LNTs
  - Reactor evaluation planned
  - Catalyst used in an ORNL lean gasoline engine-based project (see ACE033 talk)

# Detailed elemental analysis of different LNT technologies on hand

## New LNT

### Lean GDI, 2009, from BMW 120i vehicle

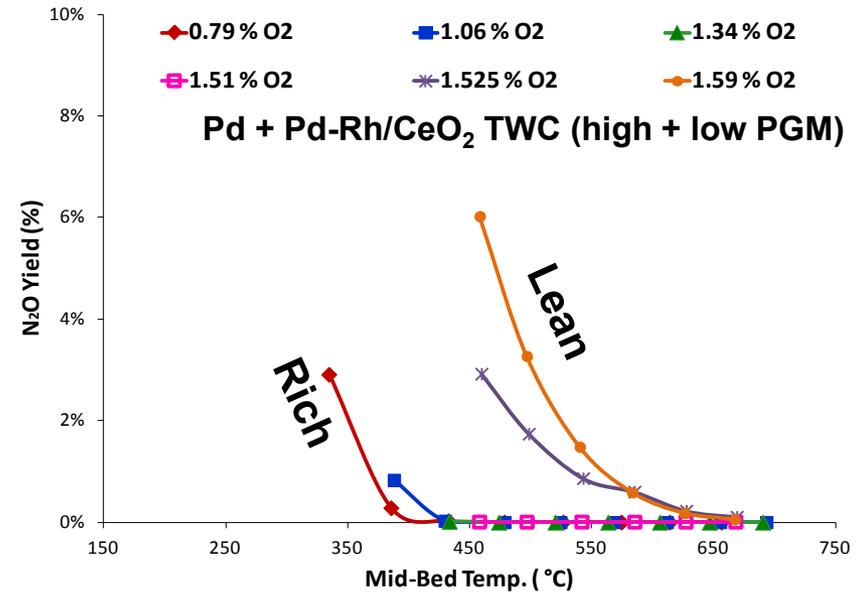
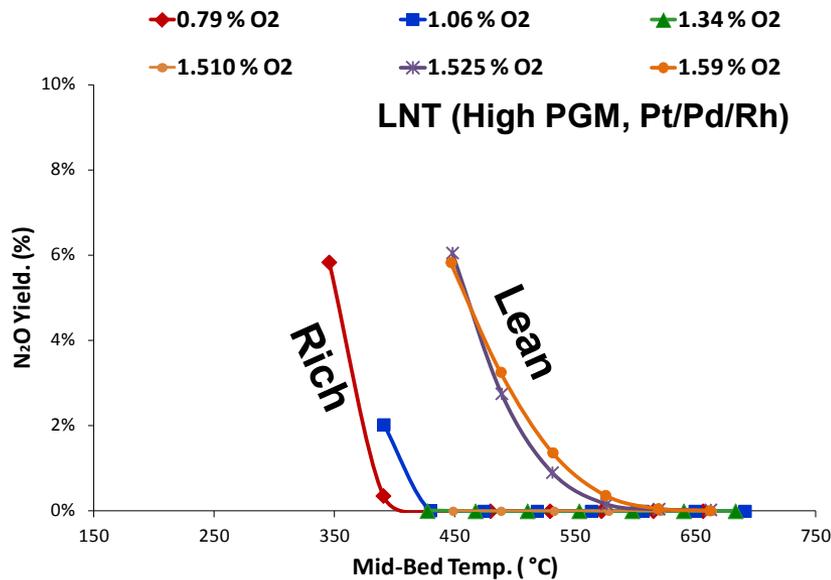
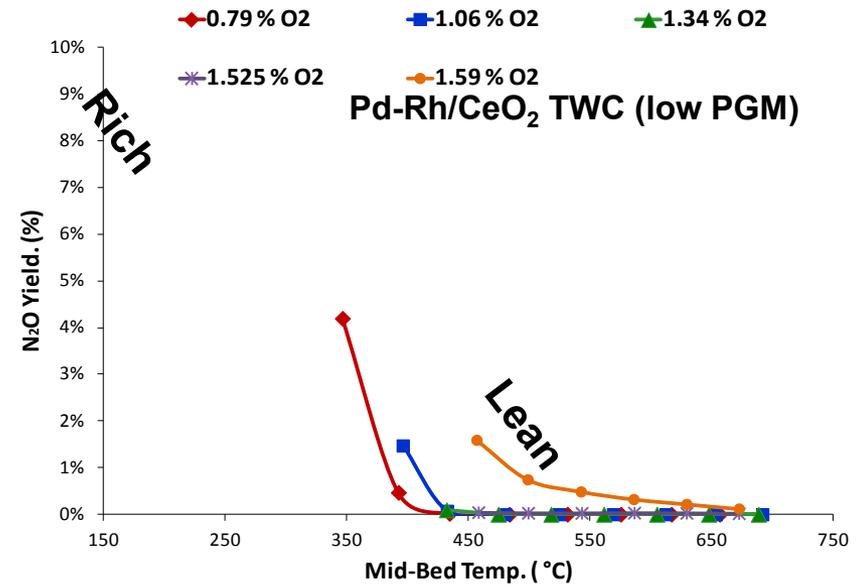
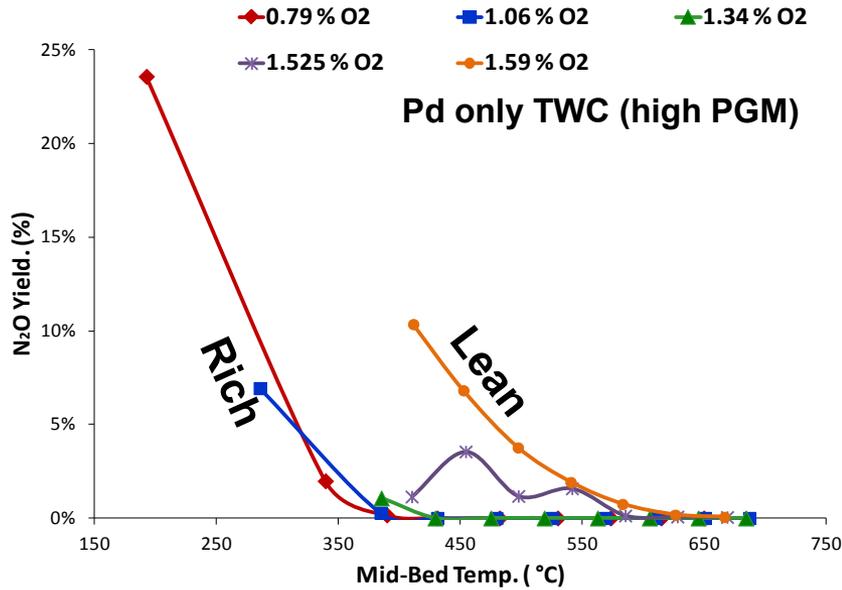
BMW LNT				
Element	Loading (g/ft3)	Loading (g/in3)	Loading (g/L)	
Ba	565	0.33	19.9	
Ce	1572	0.91	55.5	
Zr	122	0.07	4.3	
La	69	0.04	2.5	PGM ratio
Pt	62	0.04	2.2	7
Pd	24	0.01	0.8	3
Rh	8	0.00	0.3	1
PGM loading	94	0.05	3.3	

## CLEERS reference

### Lean GDI, 2004, provided by Umicore

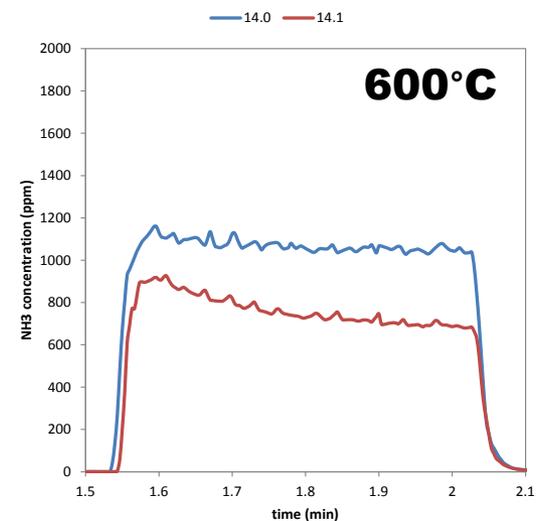
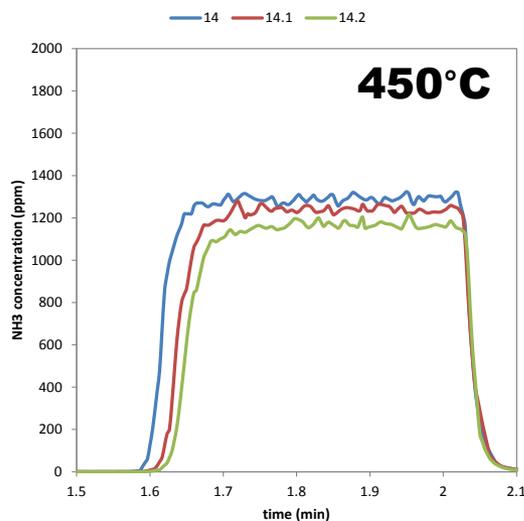
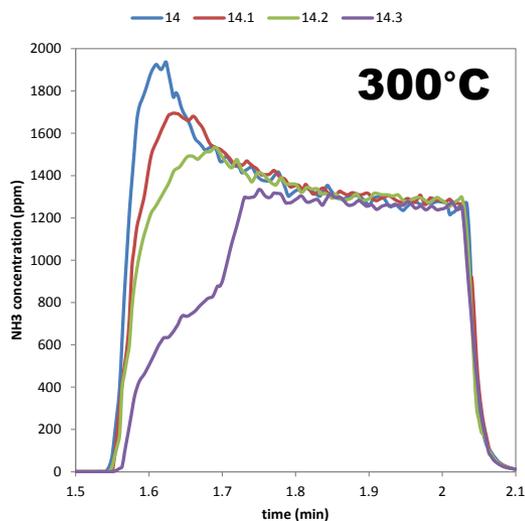
cf. CLEERS Umicore LNT				
Element	Loading (g/ft3)	Loading (g/in3)	Loading (g/L)	
Ba	442	0.256	15.6	
Ce	1978	1.145	69.9	
				PGM ratio
Pt	72	0.042	2.5	8
Pd	23	0.013	0.8	3
Rh	9	0.005	0.3	1
PGM loading	103	0.06	3.6	

# N<sub>2</sub>O formation can be significant on all catalysts and under lean or rich operation

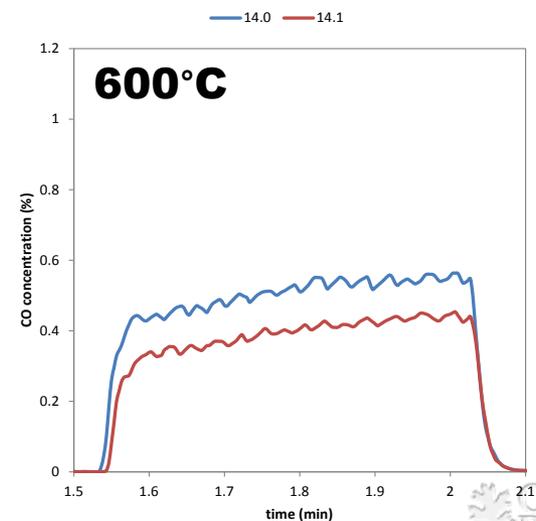
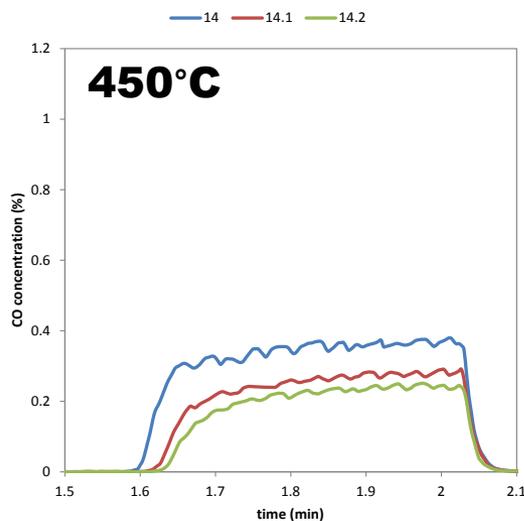
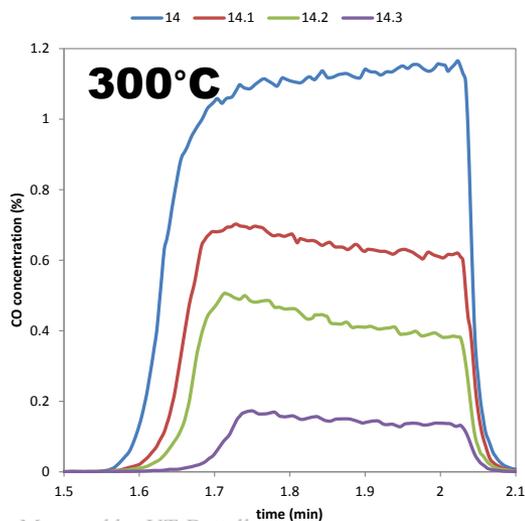


# TWC (high PGM Pd-only) transients

- $\text{NH}_3$  profiles during lean to rich transitions:

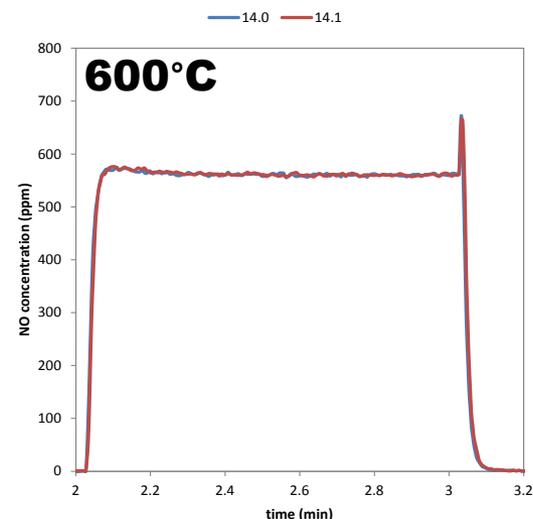
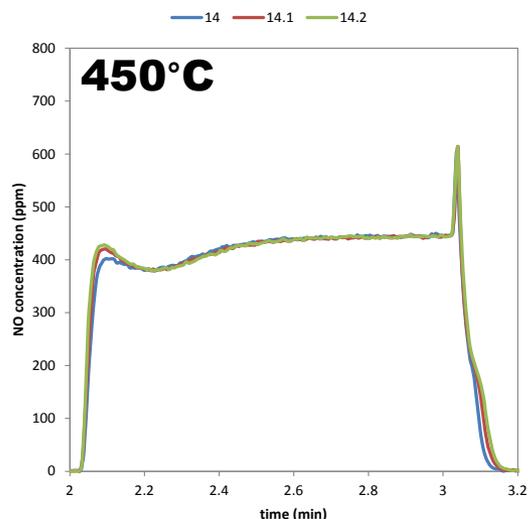
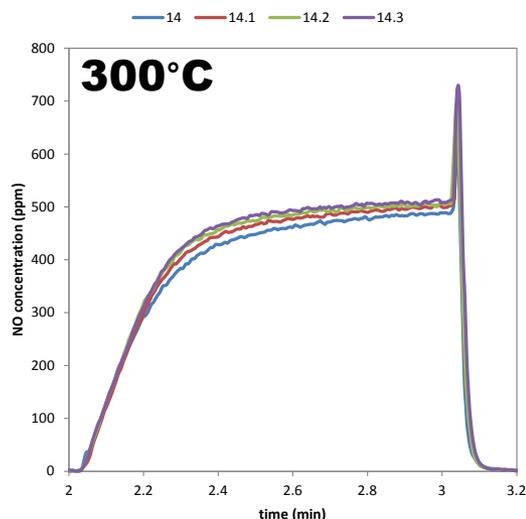


- CO profiles during lean to rich transitions:

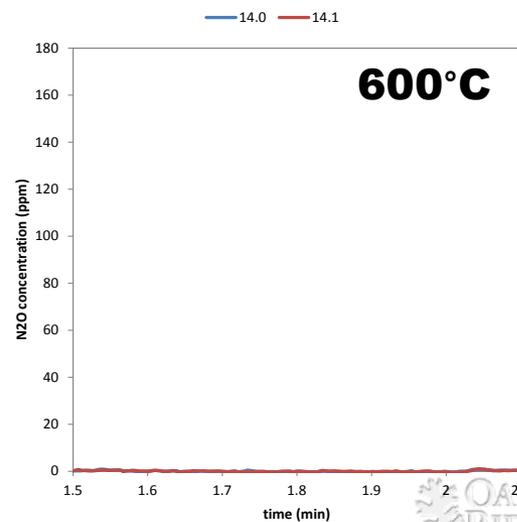
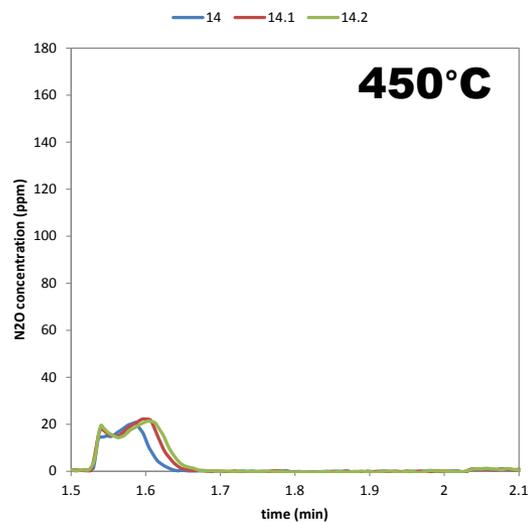
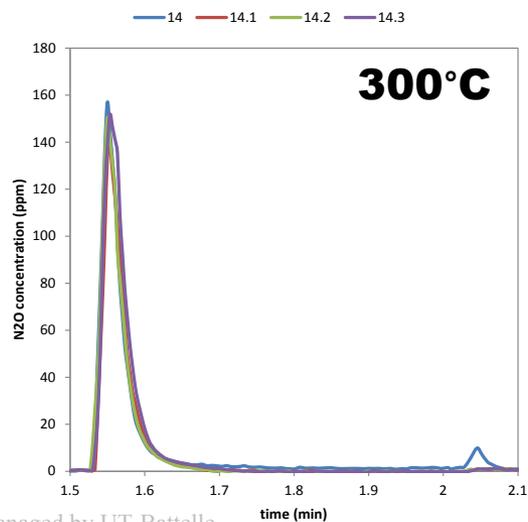


# TWC (high PGM Pd-only) transients

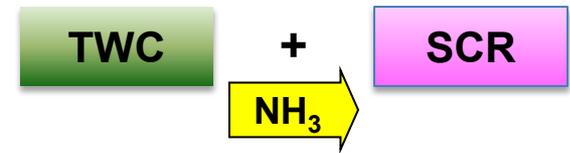
- NO profiles during lean to rich transition illustrate some storage at low temperature:



- N<sub>2</sub>O profiles during lean to rich transitions:



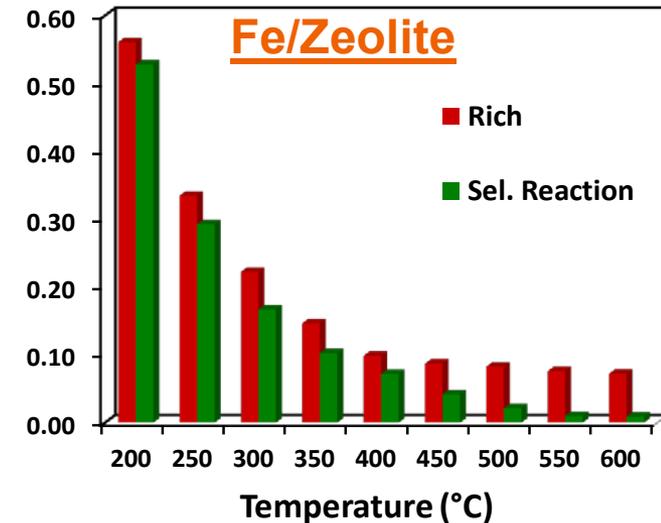
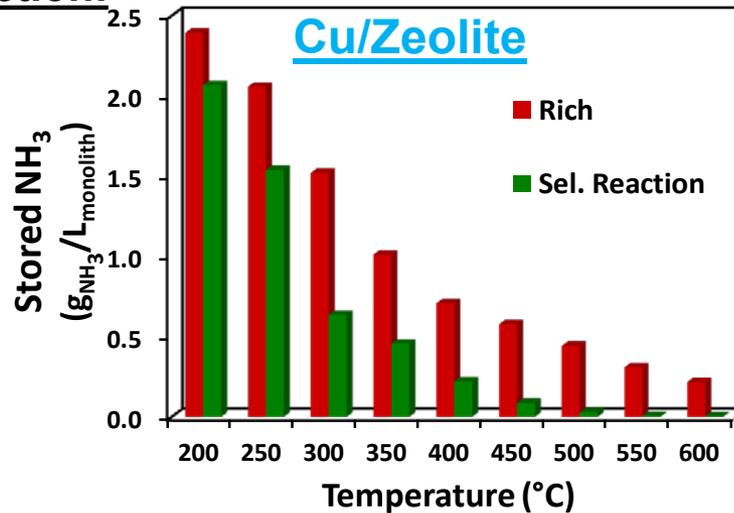
# SCR Screening:



## NH<sub>3</sub>-SCR Storage/Reaction: SV = 30,000 hr<sup>-1</sup>

**Storage:**  
500 ppm NH<sub>3</sub>  
5% H<sub>2</sub>O, bal. N<sub>2</sub>

**Reaction:**  
500 ppm NO  
10% O<sub>2</sub>  
5% H<sub>2</sub>O, bal. N<sub>2</sub>



## Steady-State NH<sub>3</sub>-SCR: SV = 30,000 hr<sup>-1</sup>

500 ppm NO  
500 ppm NH<sub>3</sub>  
10% O<sub>2</sub>  
5% H<sub>2</sub>O

