



# Novel Materials for High Efficiency Direct Methanol Fuel Cells

## 2009 Fuel Cell Projects Kickoff Meeting

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Application Number:  
Arkema Inc. (1281)

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# Project Objectives

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- Develop ultra-thin membranes having extremely low methanol crossover, high conductivity, durability, and low cost.
- Develop cathode catalysts that can operate with considerably reduced platinum loading and improved methanol tolerance.
- Produce an MEA combining these two innovations and having a performance of at least 150 mW/cm<sup>2</sup> at 0.4 V and a cost of less than \$0.80/W for the membrane and cathode catalyst.

# Organization

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PEM Development and testing  
MEA diagnostics and durability



Catalyst development  
MEA production and testing



Cutting-edge characterization of  
MEAs and development of composite  
membranes



# Technical Barriers and Targets

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- Barriers Addressed in DOE Fuel Cell Technical Plan:
  - Durability
  - Cost
  - Performance
- Targets

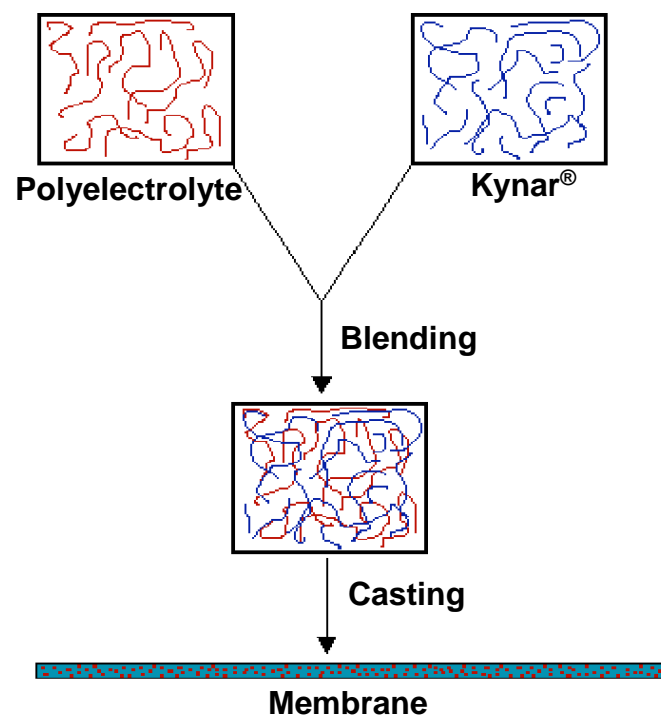
Characteristic	Industry Benchmark	Project Target
Methanol Permeability	$1-3 \cdot 10^{-6} \text{ cm}^2/\text{s}$	$5 \cdot 10^{-8} \text{ cm}^2/\text{s}$
Areal resistance ( $\Omega\text{cm}^2$ ), 70 °C	0.120 (Nafion <sup>®</sup> 117)	0.080 (2 mil thick film)
Catalyst Mass Activity (RDE) †	22.5 mW/mg Pt	> 100 mW/mg Pt
MEA Cathode Catalyst Loading	4 mg/cm <sup>2</sup>	1.5 mg/cm <sup>2</sup>
MEA I-V Cell Characteristic	90 mW/cm <sup>2</sup> @ 0.4 V	150 mW/cm <sup>2</sup> @ 0.4 V
MEA Lifetime	> 3,000 h	5,000 h

† conditions at 0.45 V & 70 °C



# Technical Approach: Membrane Development

- Polymer blend
  - Decouples conductivity from other requirements
  - Kynar<sup>®</sup> PVDF
    - Chemical and electrochemical stability
    - Mechanical strength
    - Excellent barrier against methanol
  - Polyelectrolyte
    - H<sup>+</sup> conduction and water uptake
- Robust blending process
  - PVDF can be compatibilized with a large range of polyelectrolytes
  - Morphology and physical property control
  - Phase separation on a scale of 10-100s of nm
- Lower cost approach compared to PFSA
  - Kynar<sup>®</sup> PVDF - commercial product
  - Polyelectrolyte – hydrocarbon based

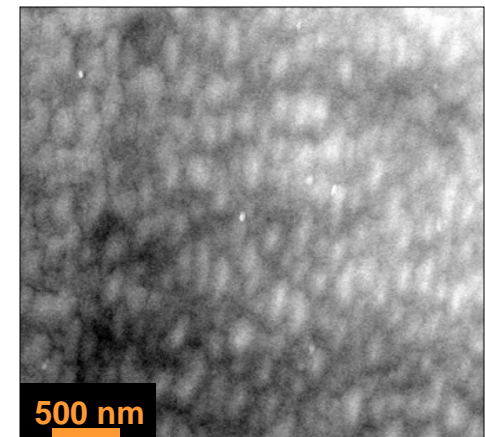


# Technical Approach: Membrane Development

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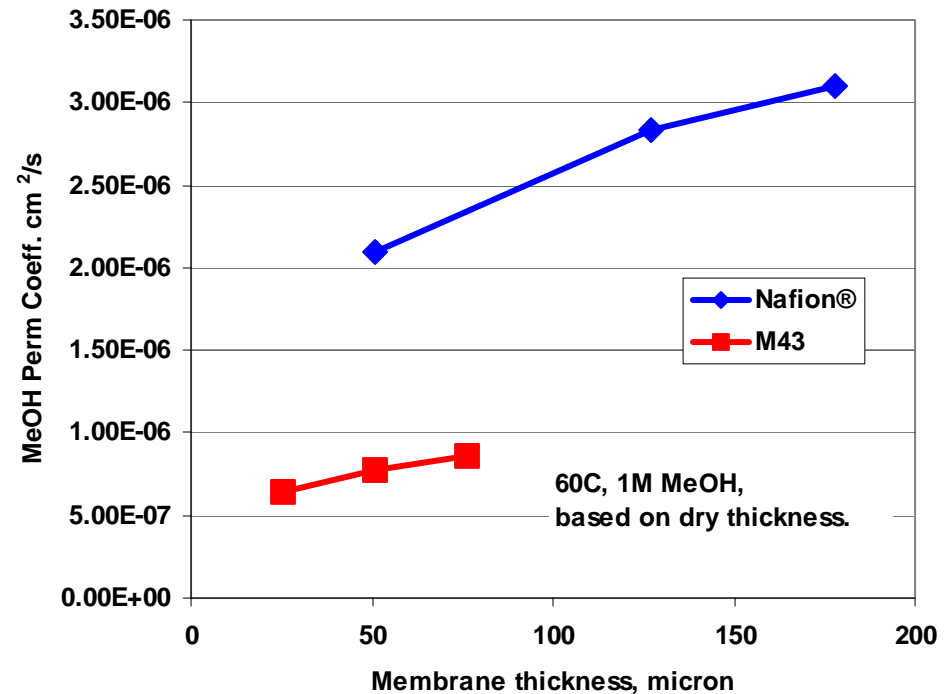
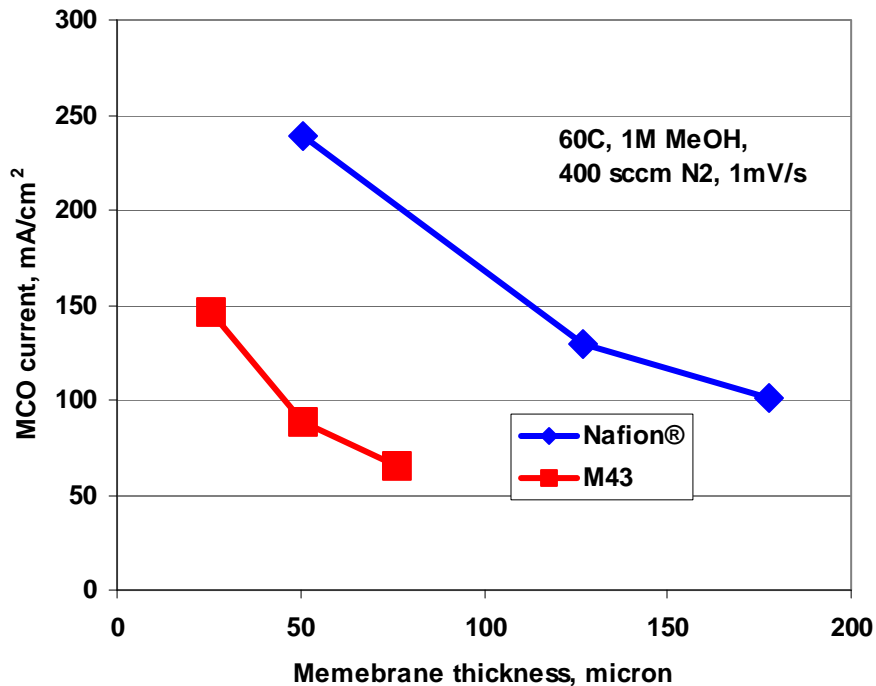
The key to the desired properties resides in careful control of composition, architecture, and morphology of the membrane components.

- Phase separation on the order of 10s of nm
  - Polymer architecture, composition, and type of compatibilizer
- PVDF matrix optimization
  - Degree of crystallinity
- Tailor the polyelectrolyte composition to minimize methanol permeation in this phase
  - Different acid and ion-containing groups
- Acidic inorganic additives
  - Reduce swelling in the membrane while maintaining conductivity



# Preliminary Data: M43 Methanol Crossover

Conductivity: 140 mS/cm (1 mil) @ 70 °C (in DI Water)

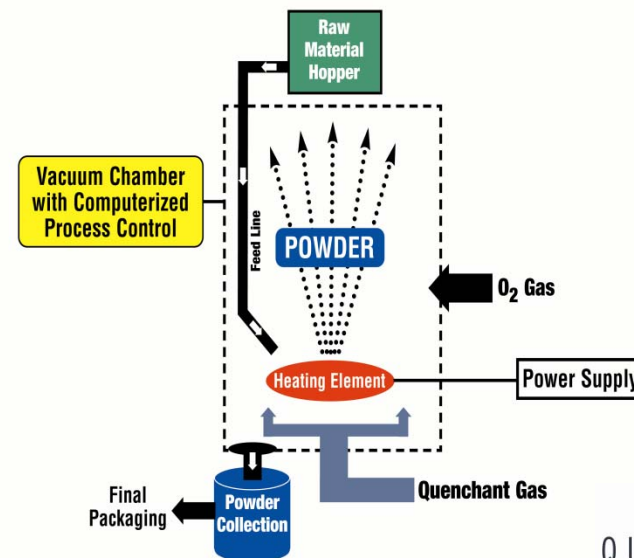
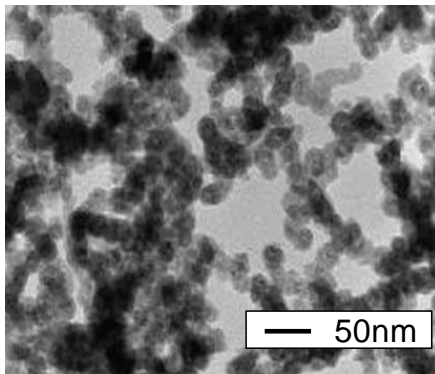


- M43 was developed for hydrogen applications
- Without any optimization, M43 is already a good methanol barrier



# Technical Approach: Methanol Tolerant Cathode Catalyst

- Pd based alloy nanocatalyst mixed with Pt/C
  - Improved mass activity by suppressing methanol oxidation
  - Significant cost reduction by lower Pt content
  - Particle size = 3-10nm
- Pd-based nanocatalysts prepared using gas phase condensation
  - Control of particle size, alloy ratio, and core-shell structure
- Catalysts screening by rotating disk voltammetry, in presence and absence of methanol





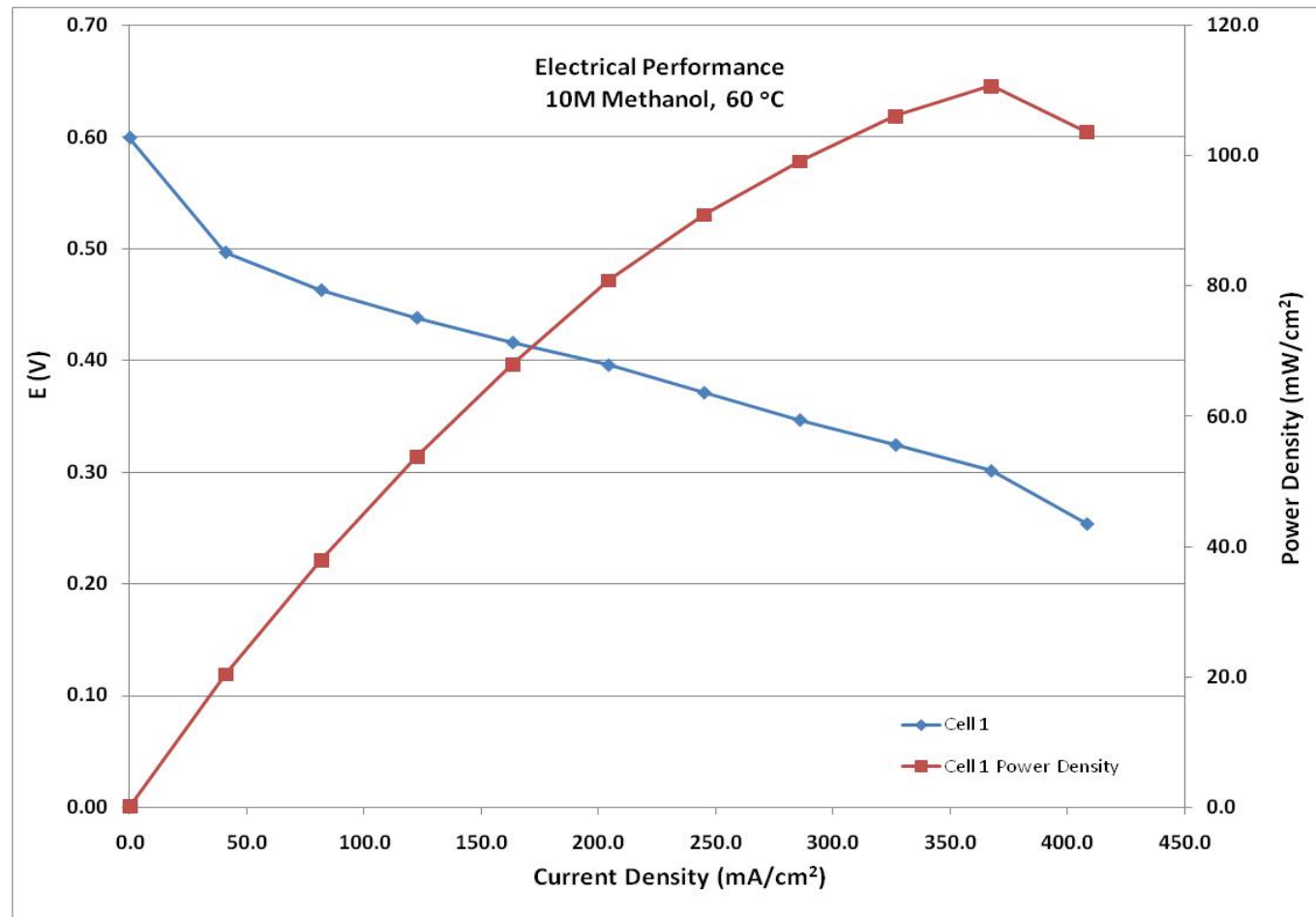
# Technical Approach: MEA Testing

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- MEA development and characterization (QSI)
  - Optimize catalyst layer composition/construction
    - Ionomer content
    - GDE vs CCM
- MEA diagnostics (IIT, Arkema, QSI)
  - Single cell polarization with 1-10M methanol/air
  - Anode and cathode half-cell polarization measurement using reference electrode
  - Linear sweep voltammetry and CO<sub>2</sub> sensor to monitor methanol crossover
  - Cyclic voltammetry for catalyst active area
  - In-situ AC impedance for MEA resistance and transport resistances.
- MEA durability testing (Arkema, IIT, QSI)
  - Constant current mode, monitoring voltage loss over time.

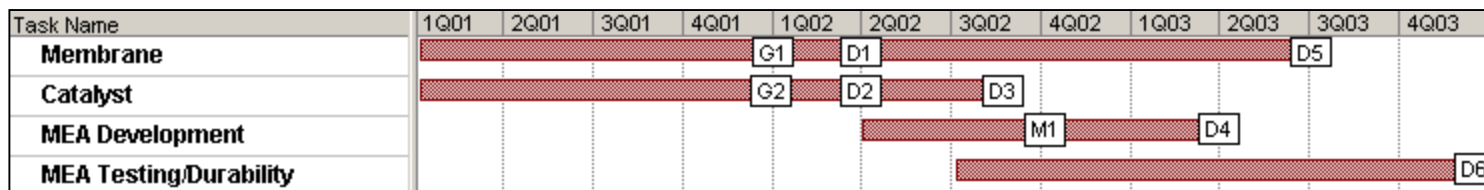
# Preliminary Results: MEA Performance

## Arkema M43 Low Crossover Membrane, QSI-Nano<sup>®</sup> Methanol Tolerant Cathode Catalyst (10M Methanol, 60 °C)



# Proposed Project Timeline

Project start: January, 2010



- G1: Membrane w/ areal resistance  $\leq 0.080 \Omega\text{cm}^2$  and a diffusion coefficient  $\leq 1 \cdot 10^{-7} \text{ cm}^2/\text{s}$
- G2: Catalyst w/mass activity  $> 70 \text{ mW/mg}$
- D1: Membrane scale-up for MEA development
- D2: Catalyst scale-up for MEA development
- D3: MEA w/ 50% Pt reduction and mass activity  $> 100 \text{ mW/mg}$
- M1: MEA w/ ohmic resistance  $< 0.12 \Omega\text{cm}^2$  (determined from impedance)
- D4: MEA performance of  $150 \text{ mW/cm}^2$  @  $0.4 \text{ V}$  ( $60 \text{ }^\circ\text{C}$ ,  $1 \text{ M}$  methanol)
- D5: Membrane w/ areal resistance  $\leq 0.080 \Omega\text{cm}^2$  and a diffusion coefficient  $\leq 5 \cdot 10^{-8} \text{ cm}^2/\text{s}$
- D6: MEA passes 5,000 h durability testing



# Proposed Project Budget

- Assuming start-up date Jan. 2010
- Total Project Cost: \$3,501,264
  - Non-federal: \$867,530
  - Federal: \$2,633,734



	FY2010	FY2011	FY2012	FY2013
Non-federal	\$232,667	\$281,129	\$282,523	\$71,211
Federal	\$706,355	\$853,478	\$857,713	\$216,188
<b>Total project</b>	<b>\$939,022</b>	<b>\$1,134,607</b>	<b>\$1,140,236</b>	<b>\$287,399</b>

