

700 bar Type IV H₂ Pressure Vessel Cost Projections

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Department of Energy Physical-Based Hydrogen Storage Workshop:
Identifying Potential Pathways for Lower Cost 700 Bar Storage Vessels

24 August 2016

USCAR, Southfield, MI

Objective

- Overview assumptions & results of latest cost analyses
- Categorize potential pathways for cost reduction
- Provide framework and reference base for workshop discussions

Outline

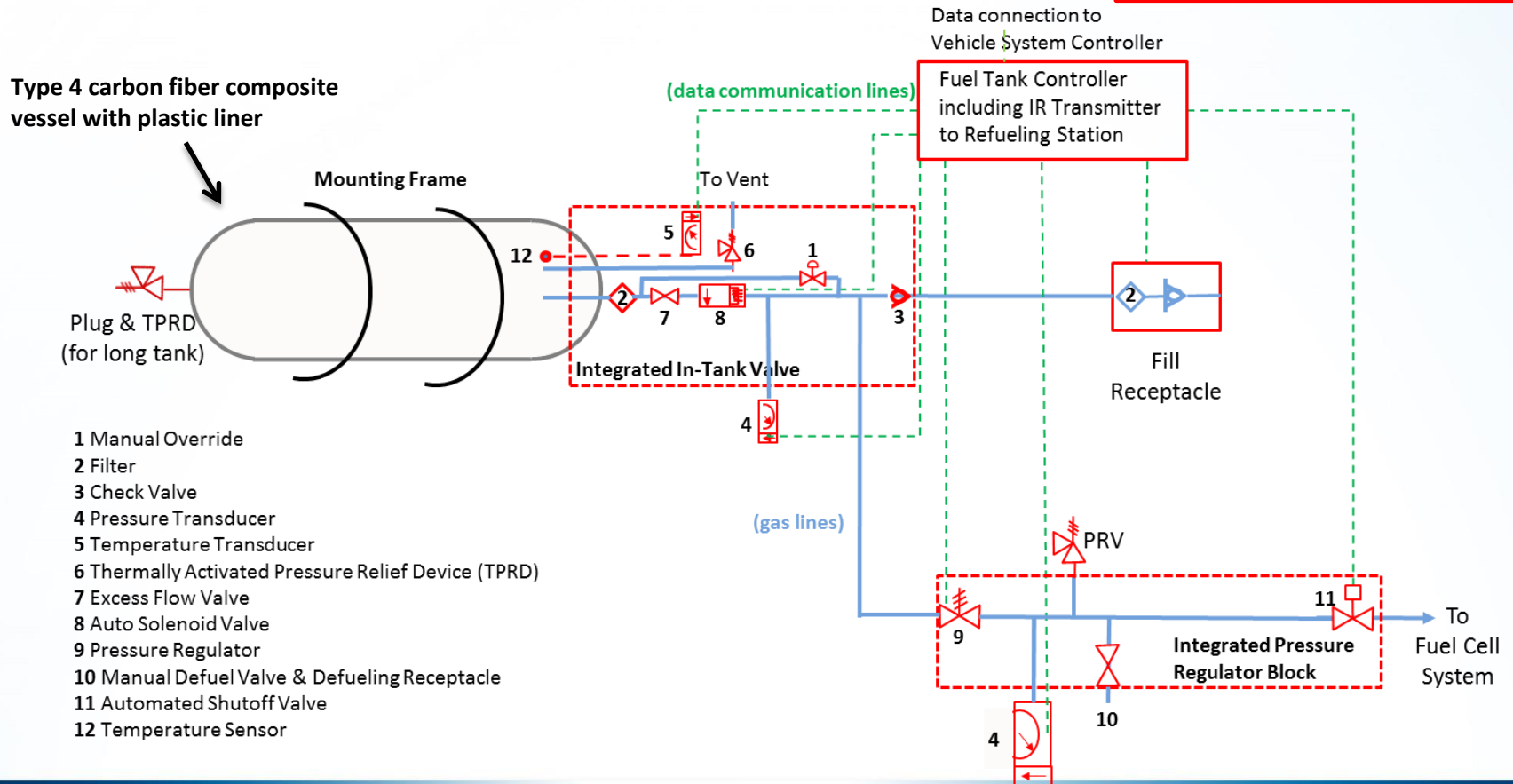
- System design
- Cost analysis methodology
- Cost projections
- Key opportunities for cost reduction
- Recent focus areas
 - Composites
 - BOP
 - Winding time

System Diagram

- System cost based on a single tank configuration
- Balance of tank includes:
 - Integrated in-tank valve
 - Integrated pressure regulator block

Cost Reduction Strategies:

- System simplification
- Multi-functionality
- Part standardization



Approach:

SA's DFMA[®] - Style Costing Methodology

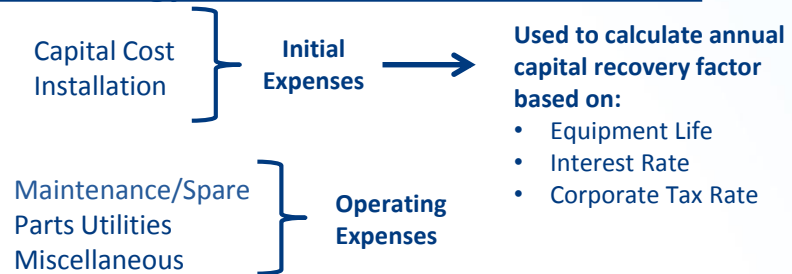
- DFMA[®] (Design for Manufacture & Assembly) is a registered trademark of Boothroyd-Dewhurst, Inc.
 - Used by hundreds of companies world-wide
 - Basis of Ford Motor Co. design/costing method for the past 20+ years
- SA practices are a blend of:
 - “Textbook” DFMA[®], industry standards and practices, DFMA[®] software, innovation, and practicality

Estimated Cost = (Material Cost + Processing Cost + Assembly Cost) x Markup Factor

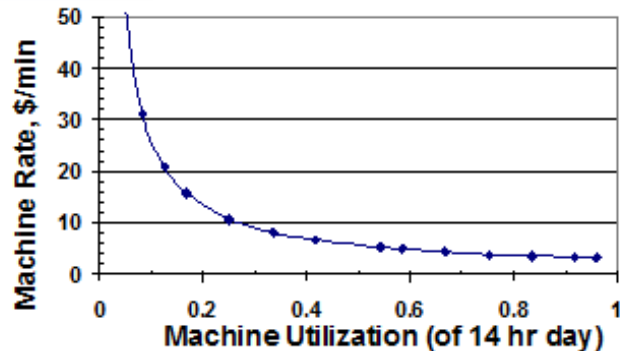
Manufacturing Cost Factors:

1. Material Costs
2. Manufacturing Method
3. Machine Rate
4. Tooling Amortization

Methodology Reflects Cost of Under-utilization:



Methodology reflects cost of under-utilization:



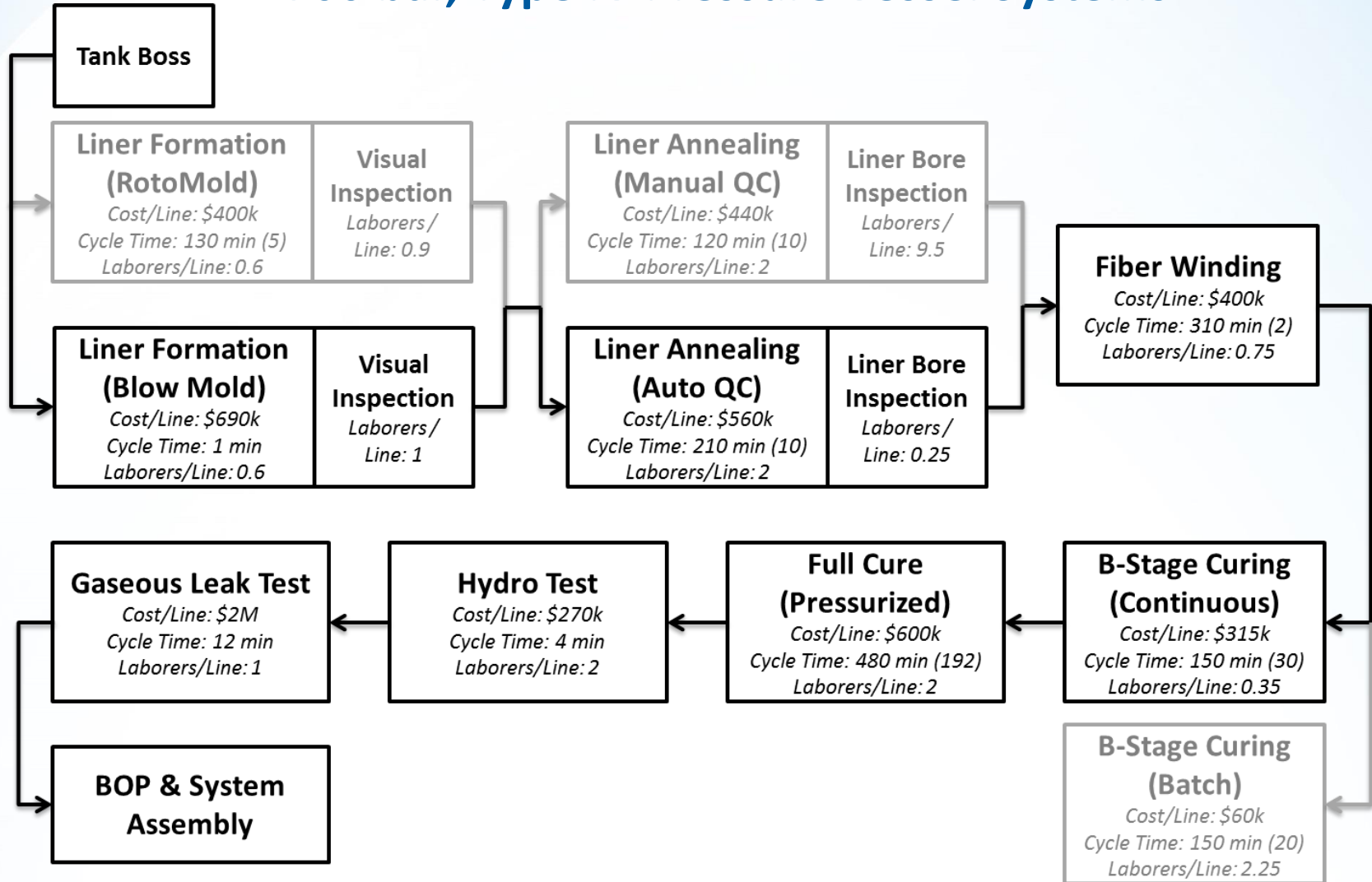
$$\frac{\left(\text{Annual Capital Repayment} + \text{Annual Operating Payments} \right)}{\left(\text{Annual Minutes of Equipment Operation} \right)} = \text{Machine Rate } (\$/\text{min})$$

Production Volume Range of Analysis:

10,000 to 500,000 H₂ storage systems per year

Manufacturing Flow Diagram

700 bar, Type IV Pressure Vessel Systems



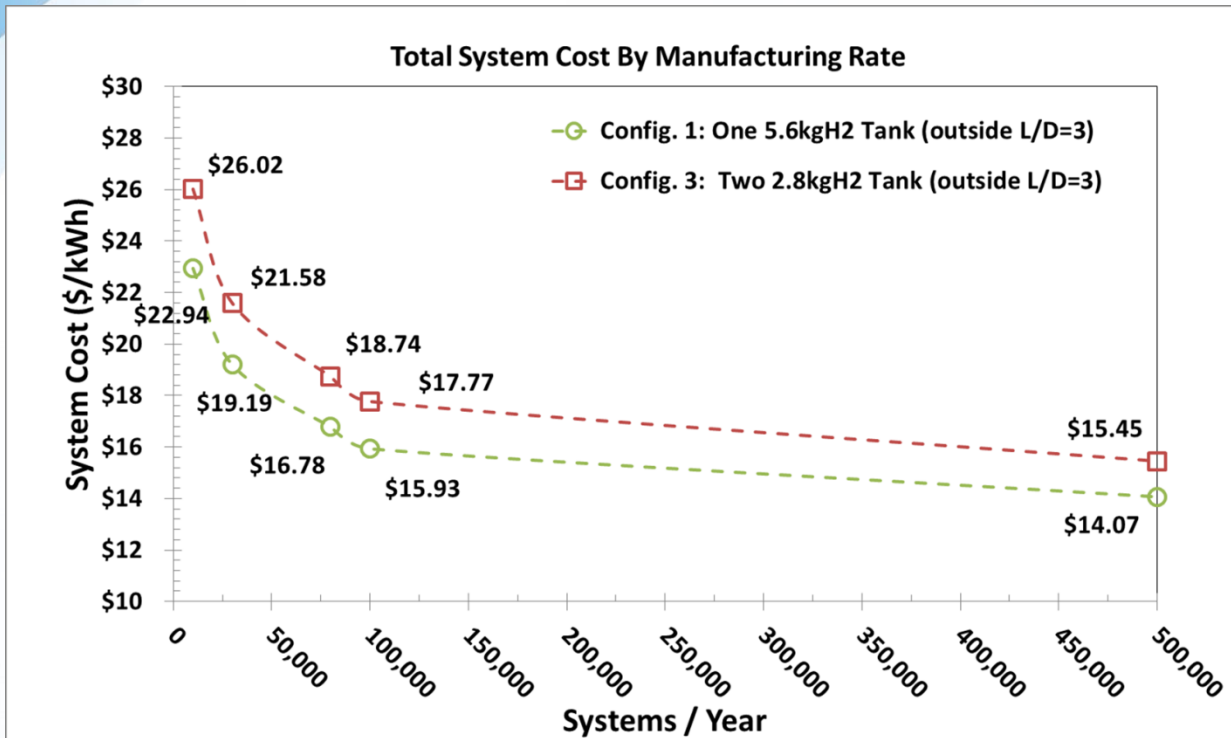
*Black indicates processes assumed for production at 500k systems/year

System Bill of Materials

(700 bar, 5.6kgH₂ usable, Single Vessel)

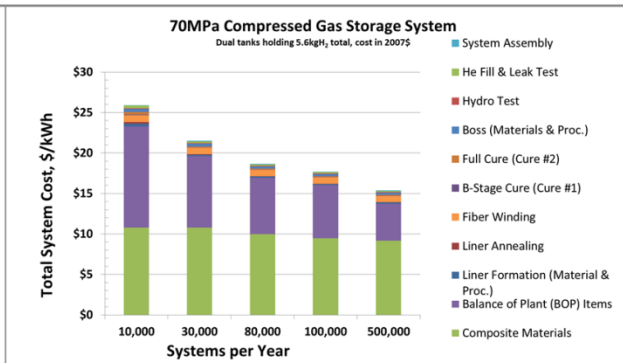
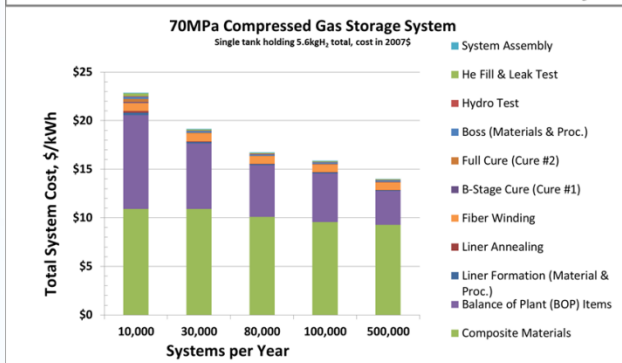
		Single-Tank Configuration					Dual-Tank Configuration				
		10,000	30,000	80,000	100,000	500,000	10,000	30,000	80,000	100,000	500,000
Liner Blow Mold	\$/kWh	\$0.27	\$0.15	\$0.11	\$0.10	\$0.10	\$0.31	\$0.18	\$0.14	\$0.14	\$0.14
Cost/tank	\$/tank	\$51.38	\$27.60	\$20.16	\$19.27	\$17.84	\$28.61	\$16.72	\$13.01	\$12.67	\$12.64
Liner Annealing	\$/kWh	\$0.17	\$0.06	\$0.03	\$0.04	\$0.03	\$0.24	\$0.07	\$0.06	\$0.05	\$0.05
Cost/tank	\$/tank	\$31.40	\$11.39	\$5.78	\$7.74	\$5.65	\$22.51	\$6.59	\$5.36	\$4.71	\$4.42
Fiber Winding (Wet Winding)	\$/kWh	\$11.72	\$11.70	\$10.86	\$10.35	\$10.04	\$11.64	\$11.62	\$10.79	\$10.28	\$9.96
Cost/tank	\$/tank	\$2,192.19	\$2,187.45	\$2,030.42	\$1,934.75	\$1,877.09	\$1,088.37	\$1,086.00	\$1,009.18	\$960.93	\$930.97
B-Stage Cure (Cure #1)	\$/kWh	\$0.09	\$0.03	\$0.02	\$0.03	\$0.02	\$0.08	\$0.05	\$0.04	\$0.04	\$0.04
Cost/tank	\$/tank	\$16.59	\$5.16	\$4.23	\$4.79	\$4.34	\$7.09	\$4.92	\$3.99	\$3.99	\$3.38
Tank Shoulder Foam	\$/kWh	\$0.09	\$0.07	\$0.06	\$0.06	\$0.06	\$0.10	\$0.08	\$0.07	\$0.07	\$0.07
Cost/tank	\$/tank	\$16.00	\$12.28	\$11.12	\$10.98	\$10.76	\$9.25	\$7.39	\$6.81	\$6.74	\$6.67
Full Cure	\$/kWh	\$0.34	\$0.06	\$0.04	\$0.05	\$0.04	\$0.31	\$0.08	\$0.07	\$0.07	\$0.06
Cost/tank	\$/tank	\$63.95	\$12.09	\$6.94	\$8.79	\$7.31	\$28.64	\$7.34	\$6.31	\$6.93	\$5.61
Boss	\$/kWh	\$0.19	\$0.15	\$0.14	\$0.13	\$0.13	\$0.38	\$0.31	\$0.28	\$0.27	\$0.27
Cost/tank	\$/tank	\$35.68	\$28.90	\$25.91	\$25.21	\$24.90	\$35.68	\$28.90	\$25.91	\$25.21	\$24.90
Hydro Test	\$/kWh	\$0.08	\$0.05	\$0.04	\$0.04	\$0.04	\$0.11	\$0.09	\$0.09	\$0.08	\$0.08
Cost/tank	\$/tank	\$14.92	\$8.76	\$7.99	\$7.52	\$7.52	\$10.30	\$8.76	\$7.99	\$7.52	\$7.49
He Fill & Leak Test	\$/kWh	\$0.28	\$0.11	\$0.09	\$0.08	\$0.08	\$0.31	\$0.23	\$0.18	\$0.16	\$0.15
Cost/tank	\$/tank	\$52.68	\$21.17	\$17.23	\$14.86	\$14.86	\$29.05	\$21.17	\$17.23	\$14.86	\$13.60
Balance of Plant (BOP) Items	\$/kWh	\$9.65	\$6.76	\$5.33	\$5.01	\$3.48	\$12.49	\$8.82	\$6.95	\$6.54	\$4.59
Cost/system	\$/system	\$1,804.23	\$1,264.37	\$997.47	\$935.88	\$650.62	\$2,334.70	\$1,648.40	\$1,300.24	\$1,223.52	\$857.41
System Assembly	\$/kWh	\$0.06	\$0.05	\$0.05	\$0.05	\$0.05	\$0.06	\$0.06	\$0.06	\$0.06	\$0.06
Cost/system	\$/system	\$10.47	\$9.61	\$9.50	\$9.44	\$9.33	\$12.00	\$12.00	\$12.00	\$12.00	\$12.00
Total System Cost	\$/kWh	\$22.94	\$19.19	\$16.78	\$15.93	\$14.07	\$26.02	\$21.58	\$18.74	\$17.77	\$15.45
Total System Cost	\$/system	\$4,289.49	\$3,588.77	\$3,136.75	\$2,979.23	\$2,630.22	\$4,865.70	\$4,035.98	\$3,503.80	\$3,322.66	\$2,888.76
Tank Cost	\$/kWh	\$13.24	\$12.38	\$11.39	\$10.88	\$10.54	\$13.47	\$12.70	\$11.72	\$11.16	\$10.80
Cost per Tank	\$/tank	\$2,474.80	\$2,314.79	\$2,129.77	\$2,033.92	\$1,970.27	\$1,259.50	\$1,187.79	\$1,095.78	\$1,043.57	\$1,009.67

System Cost vs. Manufacturing Rate



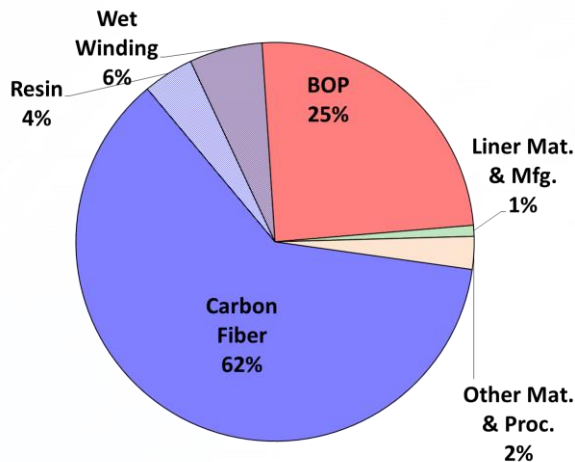
Cost Reduction Strategies:

- Increase production rate
- Single tank instead of multiple tanks



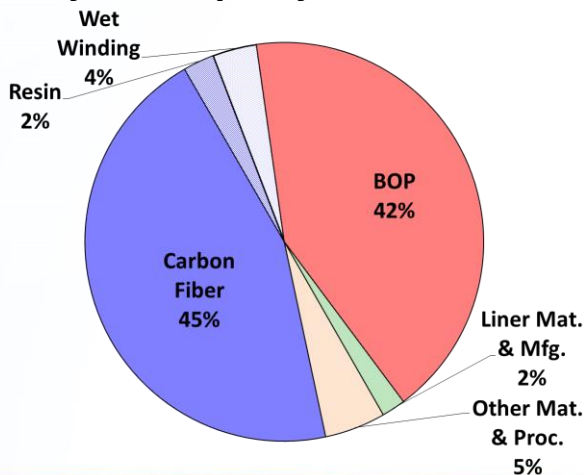
Status and Key Areas for Cost Reduction

500k Systems per year: \$14.07/kWh



- Fiber and BOP costs dominate
- Cost reductions should address:
 - **Carbon Fiber**
 - Reduced CF costs (e.g. precursor or processing cost reductions)
 - Improved material utilization (e.g. winding patterns)
 - **BOP**
 - Increased component integration
 - Parts reduction
 - Winding time not a large cost contributor

10k Systems per year: \$22.94/kWh



Carbon Fiber Production Costs

	Units	20k vehicles per year	350k vehicles per year
Precursor Production Capacity (single large plant)	tonnes/year	7,500	7,500
Precursor Required for CF Production Volume	tonnes/year	3,300	55,000
Precursor Cost (spun PAN fibers)	\$/kg	\$6.42	\$6.42
Ratio of Precursor to CF	kg/kg	2.2	2.2
CF Production Volume	tonnes/year	1,500	25,000
Cost of Precursor per kg CF	\$/kg CF	\$14.12	\$14.12
CF Processing Cost	\$/kg CF	\$15.32	\$11.49
CF Cost (no markup)	\$/kg	\$29.44	\$25.61

- Precursor production is under-sized at high CF production volume
- Precursor cost contributes ~50% of the total CF cost

Cost Reduction Strategies:

- Reduce precursor material cost (**\$/kg**)
- Increasing precursor to CF conversion efficiency (**kg_{precursor}/kg_{CF}**)
- Increase production volumes (**economies of scale**)

Composite Reduction Through Material Utilization

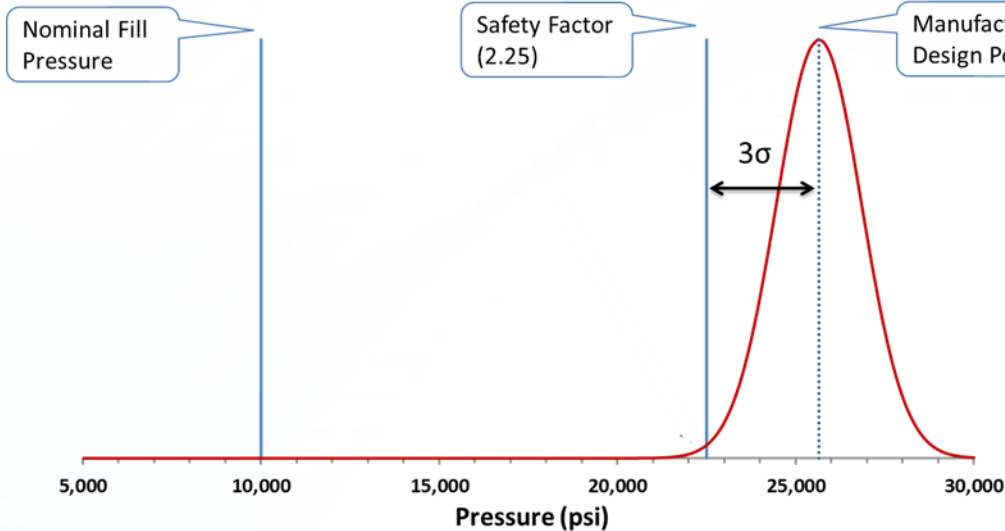
Winding Pattern	Resin	CF Volume Fraction [%]	Composite Mass [kg]	Tank Cost [\$/kWh]	BOP& Assembly [\$/kWh]	Total Cost [\$/kWh]	
PNNL/HL	Epoxy	60	106.6	12.06	3.53	15.59	} -4.7%
Toyota	Epoxy	60	99.9	11.33	3.53	14.86	
PNNL/HL	Vinyl Ester	64.7	97.0	11.04	3.53	14.57	} -3.4%
Toyota	Vinyl Ester	64.7	92.3	10.54	3.53	14.07	

Toyota cost reduction strategies:

- Eliminate high-angle helical windings using an alternate liner geometry with sharp transitions from cylinder to dome
- Alternate winding scheme with
 - One helical layer over the entire liner
 - Concentrated hoop winding over the cylinder
 - Hoop/helical winding over cylinder and dome
- Alternate boss design with a smaller diameter boss and longer flange
- Higher strength T720 vs T700 CF (cost impact not currently modeled)

Composite Reduction Through Reduced Fiber and Manufacturing Variations

$$3\sigma = 3\sqrt{COV_{Manufacturing}^2 + COV_{Fiber}^2}$$



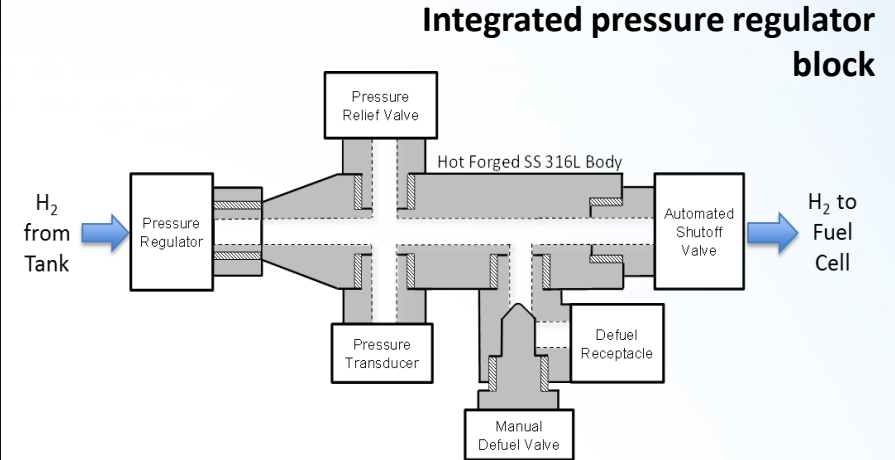
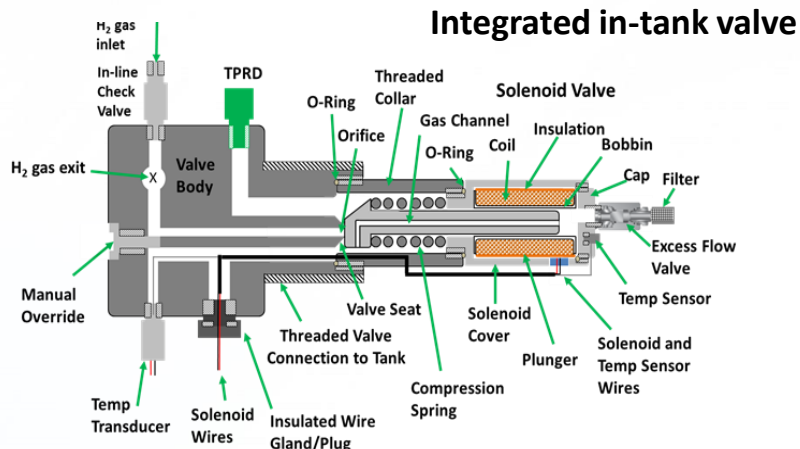
- T-700 has a COV_{fiber} of 3.3%
- Limited test samples from pilot line production have shown high fiber COVs of 7% adding almost 6 kg of CF (\$0.85/kWh)
- Fiber variations are expected to be lower at full production scale

Cost Reduction Strategies:

- R&D to lower COV during tank winding and/or during CF manufacture
- Lower Safety Factor

	Fiber	COV (mfg)	COV (fiber)	3σ	System Cost
SA Baseline	ORNL CF from PAN-MA precursor	3.3%	3.3%	14.0%	\$14.57/kWh
Observed COV_{Fiber}	ORNL CF from PAN-MA precursor	3.3%	7.0%	23.2%	\$15.42/kWh
High COV_{Fiber}	ORNL CF from PAN-MA precursor	3.3%	11.6%	36.0%	\$16.61/kWh
Tank with T-700	T-700	3.3%	3.3%	14.0%	\$16.61/kWh

Integrated BOP functionality and lower cost materials reduce system cost



	Part Count	10k sys/yr [\$/kWh]	500k sys/yr [\$/kWh]
Integrated In-Tank Valve	9 (integrated into single unit)	2.40	0.96
Integrated Regulator	9 (integrated into single unit)	3.13	1.12
Other (tubing, mount, etc.)	15	4.12	1.40
Total	33	9.65	3.48

Additional BOP Adds ~\$1.50/kWh for Two-Tank Configuration

	Single-Tank [\$/kWh]	Two-Tank [\$/kWh]
Integrated Regulator	\$0.96	\$1.75
Integrated In-Tank Valve	\$1.12	\$1.12
Other Components (Tubing, Fittings, Mounting Frame, TPRD)	\$1.40	\$1.72
Total	\$3.48	\$4.59

Cost Reduction Strategies:

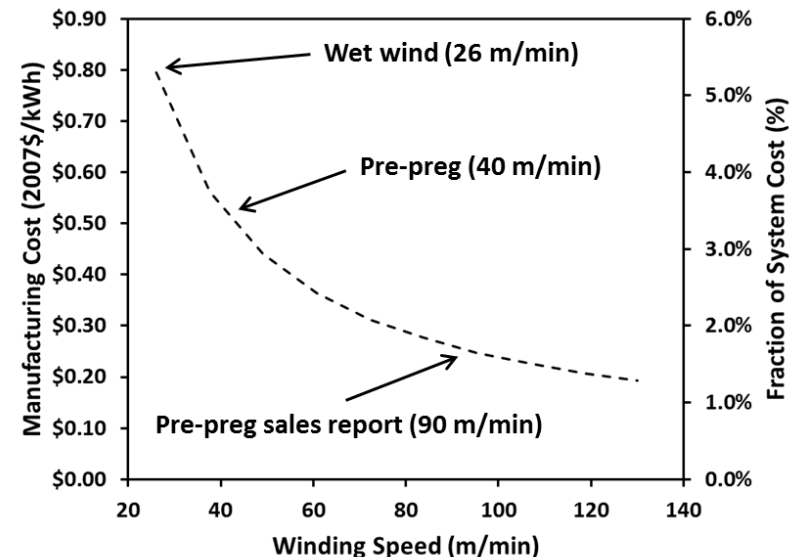
- System simplification
- Single vs. multiple tanks
- Multi-functionality
- Part standardization
- **Share valve among tanks**
- **Lower cost polymers/alloys**

Increasing Winding Speed Leads to Modest Cost Reductions

- Winding is ~5.5% of system cost for current model at 26 m/min
- System cost reductions possible (~2-4%) by increasing winding speed
- One winding line can supply around 1,500 tanks per year
 - 300 production lines required for 550k systems/year
 - Reduction in # of prod. lines is compelling reason alone to increase speed
- Manufacturing floor space and labor would be the main savings from improving winding speed

Cost Reduction Strategies:

- **Decrease winding time (limited savings)**
- **Advanced forming techniques (perhaps something radically different)**



Summary

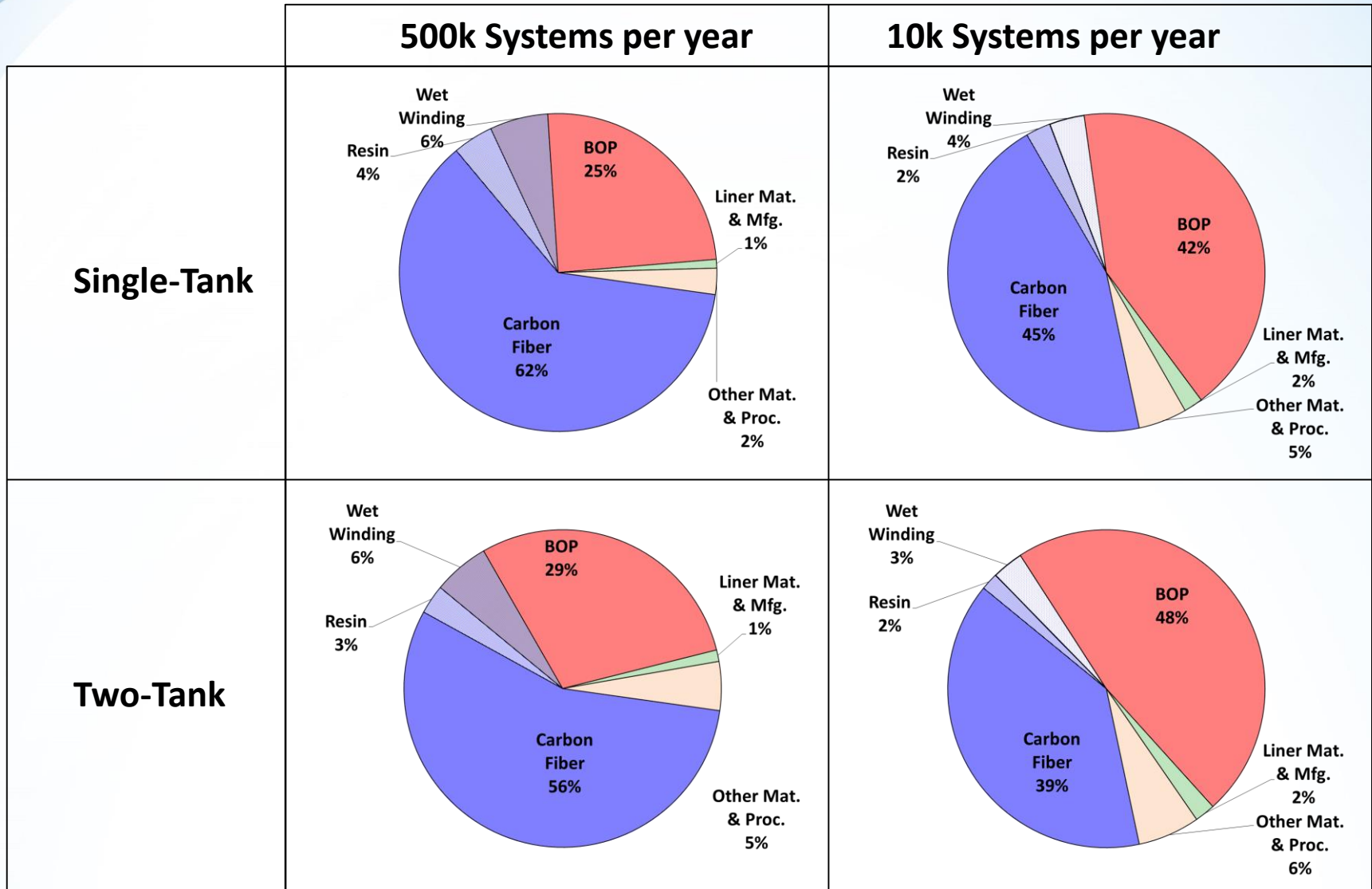
- **Carbon fiber**
 - Largest single cost item at all volumes studied (45% - 62% of system cost)
 - The cost of precursor and of converting the precursor to carbon fiber contribute approximately equally to the finished carbon fiber cost
 - Strategies to address CF cost could include reduction in
 - Precursor cost
 - Time to convert precursor fibers to CF
 - Total precursor required
 - Fiber variations must be controlled in new fiber development programs
- **Balance of Plant**
 - Further part count reduction through component integration
 - Lower cost materials
- **Manufacturing**
 - Increased winding speed will not have a significant impact on system cost, but would address the significant time to manufacturing tanks

Summary of Cost Reduction Strategies

System		<ul style="list-style-type: none"> • System simplification to reduce part counts and reduce manufacturing cost
Pressure Vessel	Carbon Fiber/Composite	<ul style="list-style-type: none"> • Reduce CF precursor cost \$/kg • New materials with lower \$/kg • Reduce CF usage • Increase strength/performance <ul style="list-style-type: none"> • Stronger fibers • Higher translation • High temperature resins to allow fast fill temperature rise
	Manufacturing	<ul style="list-style-type: none"> • Advanced forming techniques • Something radically different • Fast cure and/or low cost resins • Lower manufacturing COV • Lower Safety Factor (demonstrate safety at lower SF) • Increase production rate, market size • Decrease winding time (limited savings) • Multi-head winding, pre-preg, etc.
Balance of Plant		<ul style="list-style-type: none"> • Multi-functional components • Lower cost metals/materials-of-construction • Standardized equipment • Port sizes/diameters, connection type, material selection, etc.
Refueling Infrastructure	Functionality Placement	<ul style="list-style-type: none"> • Better utilization and lower cost if placed at station rather than placed on vehicle • Sensors, pumps, electronics, heat exchangers , etc.
	Innov. Refueling Concepts	<ul style="list-style-type: none"> • Systems that efficiently pre-cool hydrogen • Systems that can handle flow rate surge of fast filling
	PV Insulation	<ul style="list-style-type: none"> • Avoid vacuum insulation (that require gas tight welds and/or maintenance) • Develop low-k (and inexpensive) insulation • Develop automated insulation lay-up techniques • Load bearing vs. non-load bearing insulation

Backup Slides

System Cost Breakdown

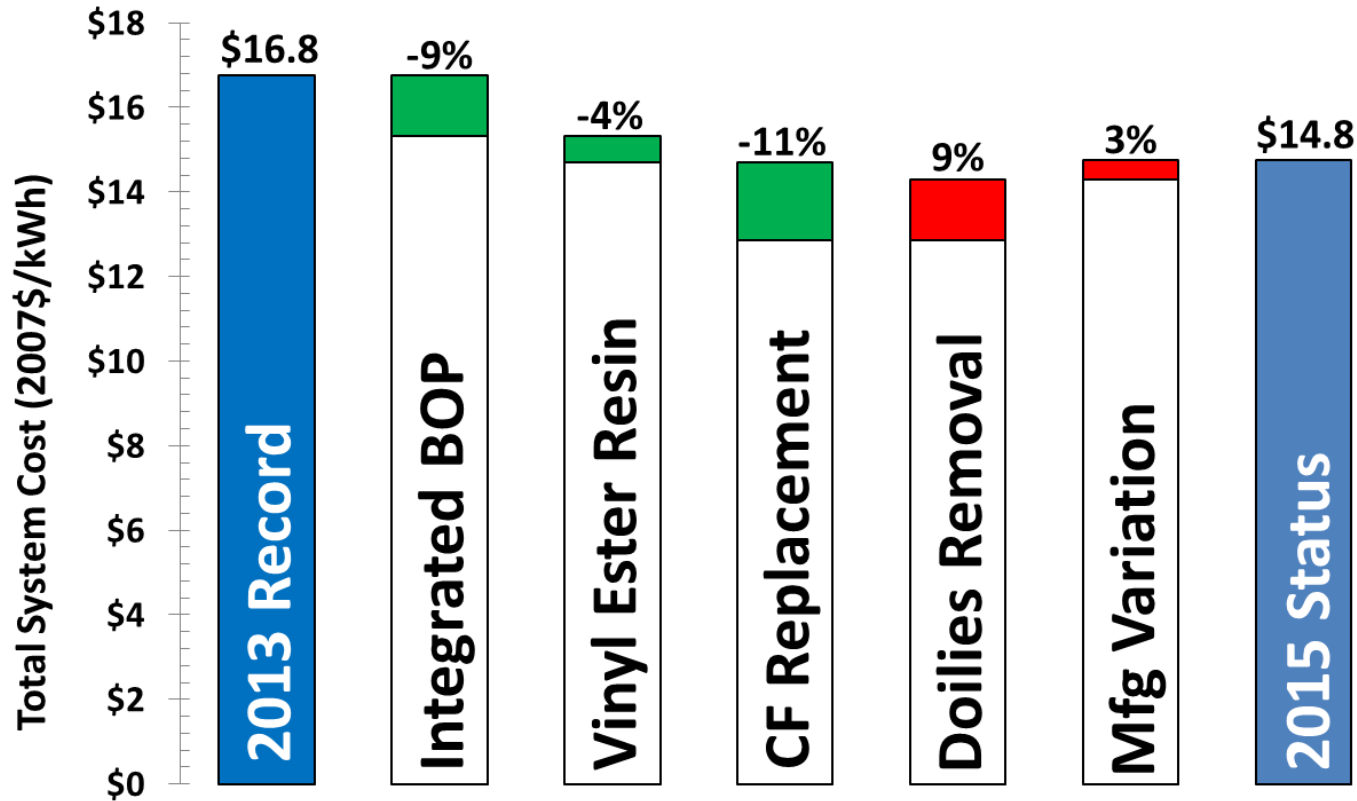


BOP Bill of Materials

Annual Manufacturing Rate	Sys/Year	Single-Tank Configuration					Two-Tank Configuration				
		10,000	30,000	80,000	100,000	500,000	10,000	30,000	80,000	100,000	500,000
Integrated In-Tank Valve	Per Tank	\$447	\$325	\$261	\$247	\$178	\$759	\$563	\$458	\$437	\$327
TPRD (1)	Per Tank	\$31	\$27	\$23	\$22	\$16	\$62	\$53	\$46	\$44	\$33
Excess Flow Valve (1)	Per Tank	\$40	\$32	\$28	\$27	\$21	\$80	\$64	\$55	\$53	\$41
Filter (1)	Per Tank	\$27	\$22	\$20	\$19	\$16	\$54	\$45	\$40	\$39	\$32
Manual Override (1)	Per Tank	\$6	\$5	\$5	\$5	\$5	\$12	\$11	\$10	\$10	\$10
Temperature Sensor (1)	Per Tank	\$43	\$29	\$21	\$20	\$12	\$87	\$58	\$42	\$39	\$25
Auto Solenoid Valve (1)	Per Tank	\$105	\$77	\$64	\$62	\$48	\$211	\$154	\$128	\$123	\$97
Valve Body (1)	Per Tank	\$19	\$16	\$15	\$15	\$14	\$38	\$32	\$30	\$30	\$27
Insulated Leadwire Sealing Fitting (1)	Per Tank	\$29	\$20	\$15	\$13	\$8	\$59	\$40	\$29	\$27	\$16
Valve Integration and Test (1)	Per Tank	\$9	\$8	\$8	\$8	\$7	\$18	\$17	\$16	\$16	\$15
Check Valve (1)	Per System	\$44	\$29	\$21	\$19	\$11	\$44	\$29	\$21	\$19	\$11
High Pressure Transducer (1)	Per System	\$94	\$60	\$41	\$37	\$20	\$94	\$60	\$41	\$37	\$20
Integrated Pressure Regulator	Per System	\$586	\$396	\$327	\$302	\$209	\$586	\$396	\$327	\$302	\$209
Integrated Pressure Regulator Block	Per System	\$33	\$10	\$12	\$11	\$8	\$33	\$10	\$12	\$11	\$8
Pressure Regulator (1)	Per System	\$204	\$164	\$164	\$153	\$127	\$204	\$164	\$164	\$153	\$127
PRV (1)	Per System	\$92	\$58	\$39	\$35	\$18	\$92	\$58	\$39	\$35	\$18
Low Pressure Transducer (1)	Per System	\$55	\$35	\$24	\$22	\$13	\$55	\$35	\$24	\$22	\$13
Manual Defuel Valve incl. "Defuel Recep." (1)	Per System	\$87	\$55	\$37	\$34	\$17	\$87	\$55	\$37	\$34	\$17
Low Pressure Automated Shutoff Valve (1)	Per System	\$115	\$74	\$51	\$47	\$26	\$115	\$74	\$51	\$47	\$26
Other (tubing, mount, etc.)	Per System	\$770	\$541	\$413	\$387	\$262	\$991	\$688	\$518	\$485	\$321
Fuel Tank Controller (1)	Per System	\$138	\$117	\$101	\$97	\$76	\$138	\$117	\$101	\$97	\$76
Pipings/Fittings for first tank	Per System	\$91	\$68	\$61	\$59	\$51	\$91	\$68	\$61	\$59	\$51
Pipings/Fittings per additional tank	per addtl tank	\$0	\$0	\$0	\$0	\$0	\$35	\$30	\$27	\$26	\$23
Plug and TPRD (1)	Per tank	\$140	\$89	\$59	\$54	\$28	\$280	\$177	\$118	\$108	\$55
Fill Receptacle (incl. IR Transmitter) (1)	Per System	\$195	\$124	\$83	\$76	\$40	\$195	\$124	\$83	\$76	\$40
Mounting Frame (1)	Per Tank	\$45	\$29	\$19	\$17	\$9	\$91	\$58	\$38	\$35	\$18
Miscellaneous	Per System	\$161	\$114	\$90	\$84	\$58	\$161	\$114	\$90	\$84	\$58
BOP Subtotal	\$/System	\$1,804	\$1,264	\$997	\$936	\$651	\$2,335	\$1,648	\$1,300	\$1,224	\$857
BOP Subtotal	\$/kWh	\$9.65	\$6.76	\$5.33	\$5.01	\$3.48	\$12.49	\$8.82	\$6.95	\$6.54	\$4.59

Accomplishments & Progress:

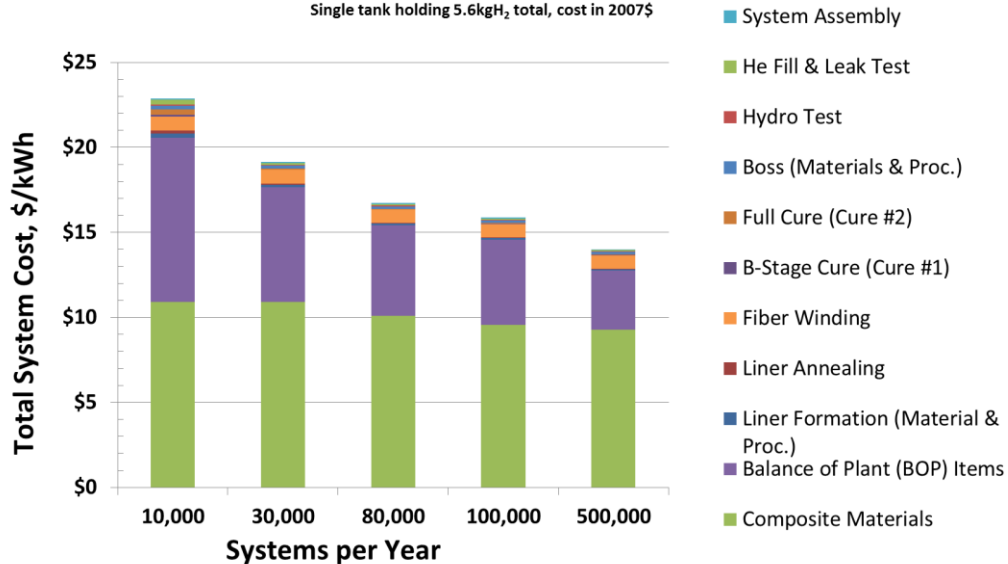
700 bar type IV H₂ storage system cost reduction identified



*Cost at 500,000 systems per year

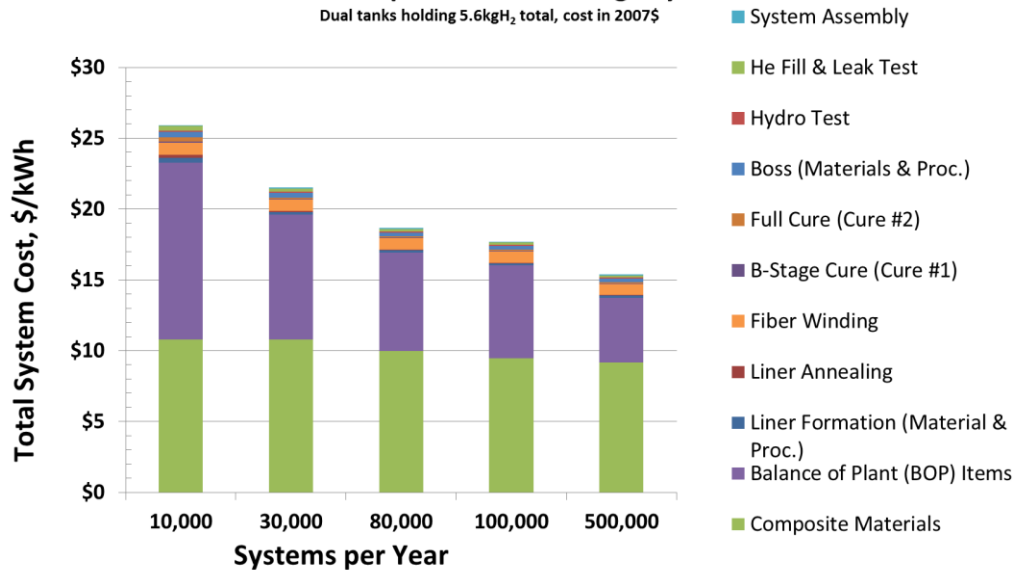
70MPa Compressed Gas Storage System

Single tank holding 5.6kgH₂ total, cost in 2007\$



70MPa Compressed Gas Storage System

Dual tanks holding 5.6kgH₂ total, cost in 2007\$



Total System Cost By Manufacturing Rate

