Low Cost, High Capacity Non-Intercalation Chemistry Automotive Cells

Sila Nanotechnologies, Inc. & Georgia Institute of Technology (Project ID# ES244)

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This presentation does not contain any proprietary, confidential or otherwise restricted information

Overview

Timeline

- Project start date: 10/2014
- Project end date: 12/2016
- Percent complete: 70 %

Budget

- Total project funding
 - DOE share: \$1,000,000
 - Contractor share: \$250,000
- Funding received in FY 2015: 446,807
- Funding for FY 2016: 553,193

Barriers

- > Barriers of batteries addressed
 - High cost
 - Low energy density
 - Short battery life
- Targets: low-cost, scalable, drop-inreplacement materials for highenergy batteries

Partners

- Sila Nanotechnologies, Inc. Lead
- Georgia Institute of Technology subcontractor
- Army Research Laboratory collaborator



Relevance & Project Objectives

- The overall goal for the project is to conduct focused R&D aimed to demonstrate automotive cells with energy density, specific energy, discharge power density and specific power <u>nearly two times higher than the U.S. DRIVE</u> <u>End of Life Targets for EV Cells</u>: up to ~580 Wh/kg and ~ 1200 Wh/L
- In order to achieve this objective: develop electrochemically stable ultra-high specific capacity metal fluoride (MF_x)-based cathodes to be matched with ultra-high specific capacity Si-based anodes.
- Design & fabricate novel core-shell MF_x nanocomposite powders that overcomes key material challenges (dissolution, low electrical conductivity of fluorides, volume changes, etc.) that otherwise lead to large voltage hysteresis and rapid capacity fading
- Develop scalable methods of drop-in-replacement material synthesis
- Project targets all listed barriers: high cost, low energy density, short cycle life



Milestones

Budget Period	Milestones & Go/No-Go Decisions	Status
1	Synthesize porous carbon spheres with tunable size	Complete
1	Develop methodology of uniform infiltration of produced porous carbons with metal fluorides (MF _x)	Complete
1	Material Characterization (SEM, TEM, EDS, XPS, N ₂ sorption, etc.)	Complete
1	Electrochemical Characterization: cathode half cells	Complete
	Go /No-Go: Half cell stability of 50 cycles with at least 60% of theoretical capacity utilization	> 800 cycles demonstrated at above 80% of
	Go/No-Go: Achieve 80% of theoretical capacity utilization	theoretical capacity
2	Material Characterization & Post-Mortem Analyses (SEM, TEM, EDS, XPS, N_2 sorption, etc.)	On track
2	Electrochemical Characterization: - MF _x cathode half cells - Si-based anode / MF _x based cathode full cells	On track
2	 Optimize electrode fabrication & full cell construction Demonstrate cycle stability of 200 cycles in full cells Demonstrate unit stack energy density of 1200 Wh/L Demonstrate unit stack power density of 2400 W/L Produce 200 mAh+ full cells 	On track

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Opportunities offered by Conversion Electrodes



- Intercalation materials approach their theoretical limits: increase in specific capacity becomes very challenging and increasing cell voltage raises safety concerns
- Conversion electrodes offer up to 10x higher specific capacity (at the expense of lower cell voltage)
- Replacement of intercalation cell chemistry with conversion-type anodes & cathodes may allow substantial increase in cell specific energy and energy density



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Opportunities offered by Conversion Electrodes



Assumptions:

Calculations of energy density of "building blocks"

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- Electrode density: 60 vol.% active in case of conversion materials and 70 vol.% in case of intercalation materials
- Material properties in the fully expanded (lithiated) state are considered
- Average discharge potential = experimental @ slow rate (intercalation) and 0.25V below theoretical (for conversion materials)
- Improvements possible: up to ~ 2.5x vs. further optimized intercalation chemistries (up to ~ 4x vs. state of the art)
- Since the cost of active materials is only ~ 25% of the full cell cost, increase in the cell energy density (assuming comparable electrode cost) directly leads to reduced cell cost (on Wh basis)
- Cells with Si anodes offer nearly the same energy density as with Li, but are safer, cheaper to use (drop-in replacement) and offer much higher power at high capacity loadings
- Conversion electrodes suffer from multiple challenges that must be overcome



- Drop-in replacement Si-based anode powder: mechanically stable, micron-scale, low surface area powder (compatible with existing equipment & slurry formulations)
- Chemical composition & detailed microstructure is proprietary
- Specific capacity: 800-1800 mAh/g
- Volumetric capacity (<u>at the electrode level</u> <u>after formation</u>): 700-1200 mAh/cc (compared to ~ 400-430 mAh/cc for state of the art graphite anodes)
- Exhibit very small volume changes at a particle level during cycling









- High-precision (≤100 nm) custom-designed tools developed for the *in-situ* thickness measurements were calibrated using multiple standards, including commercial graphite electrodes.
- Thickness changes within individual coatings (excluding Cu foils) are derived from the measurements of the full cell swelling data
- Small (< 12%) cycle-to-cycle volume changes within dense (no extra space between the packed individual particles) anode demonstrated (100% Sila anode powder, no graphite)
- Very low lifetime expansion demonstrated
- Smaller volume changes correlate with longer cycler life in full cells





- Data from early 2015
- Matched full cells with Si anodes: NCM & LFP Cathodes (no pre-lithiation, no excess capacity, 100% DoD)
- Current capacity loadings: 2-5 mAh/cm²; aiming to improve to 8+ mAh/cm²
- Anodes are 100% Sila materials (no graphite mixed)
- Current binder & C additive content: 15-22.5 wt.
 %; aiming to reduce to 5-8 wt. % (capacity is normalized by the mass of active material)
- Degradation rate slows down during cycling
 - **A cell**: 400 cycles to 80% of the initial capacity, 600+ cycles to 75%
- B cell: 500 cycles to 80% of the initial capacity, 750+ cycles to 75% and 1000+ cycles to 70%





- Anode rate tests conducted against LFP cathodes (in matched full cells)
- Anodes are 100% Sila materials (no graphite mixed)
- Discharge rate performance:
 - Capacity @ 1C is 95% of 0.1C
 - Capacity at 5C is 83% of 0.1C
 - Charge rate performance:
 - Capacity @ 6.5C is 95% of 0.1C (without taper)
 - Higher anode potential & thinner electrodes
 help to prevent plating at high charge rates



Challenges with MF_x Cathode Materials



- High M/LF interfacial energy leads to (i) growth of M & LF clusters during cycling and (ii) separation of LF from conductive M, leading to fast impedance growth and rapid cell degradation
- Electrochemical dissolution of M into electrolyte during cycling leads to (i) cathode capacity fading and (ii) damages induced to the SEI on the anode (Li losses and anode degradation)
- Significant volume changes may induce mechanical damages to the electrode and similarly contribute to cell degradation





Proposed MF_x Cathode Materials: Confinement of MFx in Carbon Nanopores combined with the formation of protective outer shell



- Nano-confinement of MF_x minimizes migration of M and LiF clusters
- conductive carbon pore walls supply electrons to/from electrochemical reaction sites (no need to rely on interconnectivity of M clusters)
- Carbon buffers the volume changes in the MF_x cathodes
- Shells prevent undesirable interaction between M and liquid electrolyte



- Methodology: nanoconfinement of MFx in carbon pores may be achieved by a low-cost infiltration of MFx precursors (e.g., FeSiF₆ in case of FeF₂) into the pores of porous carbons, followed by a heat-treatment in a controlled environment.
- Critical parameters: high solubility of the precursor in a solution; good wetting properties; low-cost solvent; low-cost precursor

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G. Yushin et al., Advanced Functional Materials v 26 (10), p. 1507-1516 (2016)

\blacktriangleright FeF₂ – C cathodes





- The average size of the spherical FeF₂-C nanocomposite particles is ~ 1 µm
- The smooth surface of the FeF₂ infiltrated AC particles indicated a good efficiency of our synthesis procedure, where no nanoparticles present outside the carbon pores.
- XRD confirmed the presence of FeF₂ nanoparticles and the lack of any crystalline impurities
- TEM studies confirmed the infiltration of FeF₂ within the AC spheres

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- Concentrated LiFSI/DME undergoes reduction at high potentials and forms a passivating layer
- IDEA: utilize concentrated LiFSI/DME electrolyte to form a protective layer (SEI), which might be efficient for prevention undesirable reactions between liquid electrolyte and M (Fe, in this case)
- Observed dramatic reduction of over-potential & <u>high (>80%) capacity utilization</u>
 G. Yushin et al., *Advanced Functional Materials* v 26 (10), p. 1507–1516 (2016)



- The longest stability of MFx cathodes demonstrated thus far
- Exceeded the 50 cycle millstone (>1,000 cycles in half cells demonstrated)
- The smallest (for this chemistry @ RT) hysteresis @ 140 mA/g (C/3) current density
- Unique MFx-electrolyte combination: concentrated LiFSI electrolyte provides *in*situ surface layer protection





Post-mortem analysis on cathode surface



High resolution XPS spectra of FeF_2/C nanocomposite cathode cycled in 0.9M, 3.3M and 4.6M LiFSI/DME electrolytes: (a) C_{1s} ; (b) O_{1s} ; (c) F_{1s} ; (d) S_{2p} .

C_{1s} peak at 285eV is due to C-C bonds from AC spheres, and -CH₂-CH₂- bonds from polymerized DME; the C-F peak due to PVdF (at 290.5eV) is diminished at higher salt concentration due to thicker layer of the reduced electrolyte; peak at 286.4eV corresponding to C-O-C bonds from polymerized DME; C=O peak from the breakdown of the backbone of DME.

- O1s: C=O peak is confirmed; peak at 532.4eV is due to O-C bonds in DME and O=S in LiFSI and its reduction products such as LiNSO₂ and LiFSO₂
- F1s: dampening of the LiF peak at 685eV and rise of the F-S peak at 687.8eV

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Collaboration on QC modeling with Dr. Oleg Borodin, ARL



Selected results of G4MP2 quantum chemistry calculations showing the LiFSI(DME) redox, decomposition and polymerization reactions and the expected SEI components:

- (a) formation of FSI_(-F) -• radicals and their potential polymerization;
- (b) reduction of FSI_(-F) -• and decomposition of some of the reduction products;
- (c) co-polymerization and other reactions of oxidized FSI_(-F) • with DME, such as H abstraction;
- (d) NSO₂⁻ oxidation coupled with its reaction with DME, leading to H abstraction and the resulting formation of DME• radicals or co-polymerization.

Georgia



Post-mortem analysis on Li anode surface:



- <u>4.6 M LiFSI in DME Electrolyte</u>: Fe dissolution is eliminated
- Bonus: NO DENDRITE GROWTH / very smooth Li surface after 1,000 cycles in our electrolytes (regular Li surface, no coatings, no alloying with other elements)





Responses to Previous Year Reviewers' Comments

Not applicable





Collaborations

> Dr. Oleg Borodin, Army Research Laboratory: QM Modeling





Remaining Challenges & Barriers

- \blacktriangleright Electrochemical stabilization of CuF₂ remains a grand challenge
- In-situ formation of protective shells may be insufficient for CuF₂ (particularly at elevated temperatures)
- Further reduction in voltage hysteresis (and energy efficiency of cells) is also challenging
- Enhancement of rate capabilities (particular at high loadings of MF_x into C and small fraction of the remaining pores) is another challenge



Proposed Future Work

- Form Li-ion permeable (solvent impermeable) shells on CuF₂-C composite powders prior to forming them into electrodes & cycling in order to enhance their cycle stability
- Develop hierarchical composites (with channels for faster Li ion access from the surface into the bulk of the particles) to enhance rate performance
- \blacktriangleright Explore doping MF_x in order to enhance rate performance & stability
- Develop high capacity loading cathodes for matching with Si anodes & optimize electrode construction and electrolyte composition to achieve high rate performance in full cells
- Advantages & limitations of different approaches of introduction Li into the system (e.g., cathode lithiation) needs to be explored

