

# Hydrogen Fuel Quality

*Focus: Analytical Methods Development &  
Hydrogen Fuel Quality Results*

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# Overview

## Timeline

- Project start date: 10/1/06
- Project end date: 9/30/11
- Percent complete: 45%

## Barriers

- Barriers addressed
  - I. Conflicts between Domestic and International Standards
  - N. Insufficient Technical Data to Revise Standards

## Budget

- Total project funding: \$1,950K
  - DOE share: 100%
  - Contractor share: 0%
- Funding received in FY08: \$850K
- Funding for FY09: \$850K

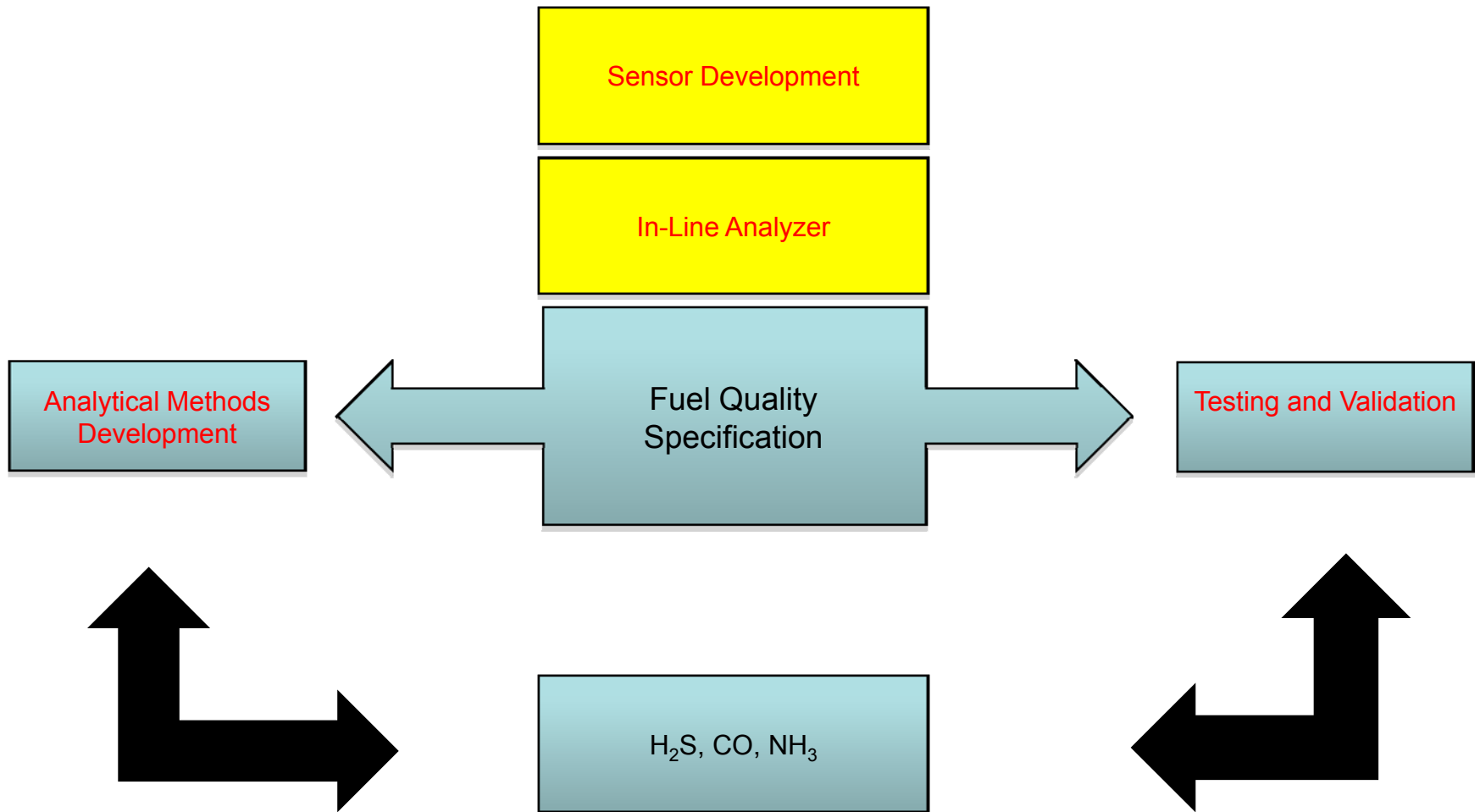
## Partners/Collaborators

- University of Hawaii/HNEI
- University of Connecticut
- University of South Carolina
- Clemson University
- SRNL
- NIST
- NREL
- ANL

# Milestones & Deliverables

Month/Year	Milestone or Deliverable
Dec 08	Milestone: Evaluate cross interference and sensitivity of sulfur-specific ion analysis methods to the presence of other impurities. <b>Completed</b>
June 09	Deliverable: Report on ammonia analytical methods development. <b>In progress, ahead of schedule</b>
Sept 09	Milestone: Evaluate cross interference of ammonia ion-specific analysis methods to the presence of other impurities. <b>In progress, ahead of schedule</b>

# Overall LANL Program



# Technical Approach

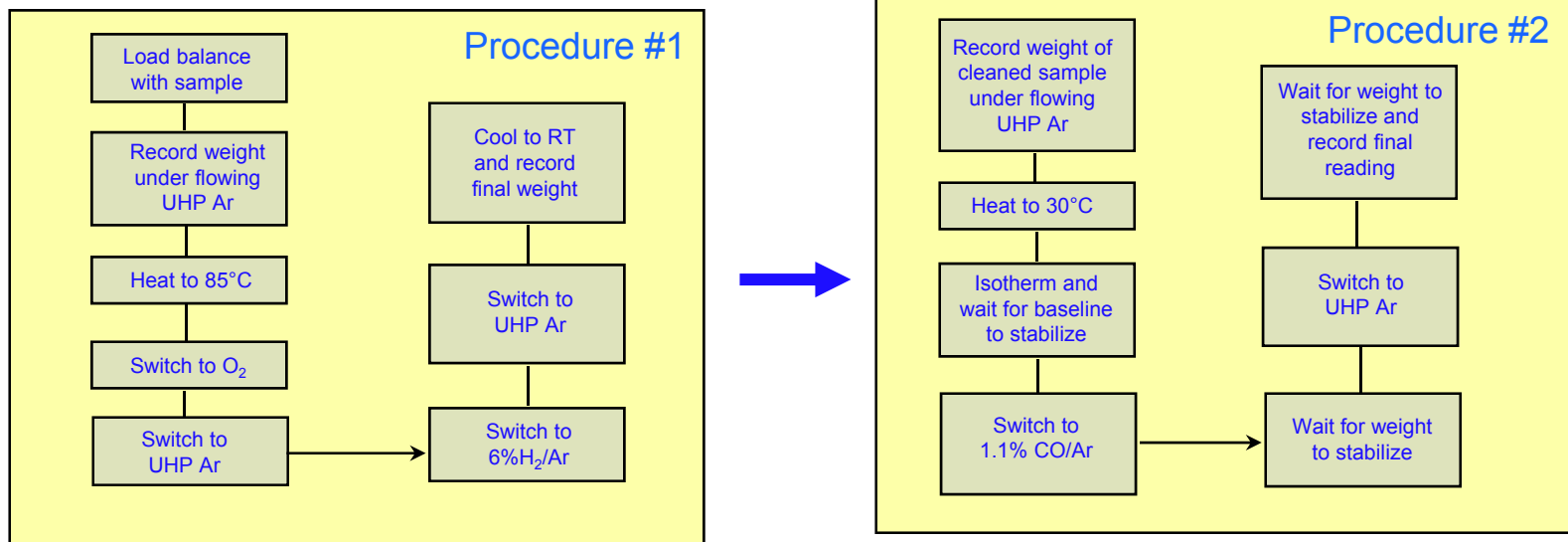
- Analytical Development: Employ, modify and/or create novel techniques that allow reproducible trace levels of contaminants to be measured.
  - Specifically: CO, Sulfur and Ammonia
- Test the critical constituents (CO, H<sub>2</sub>S, and NH<sub>3</sub>) and provide data sets to FC modelers to establish predictive mechanistic models.
  - Tested at various conditions (Temperature, Rel. humidity, Concentrations)

# Technical Approach: Gravimetry for CO Surface Adsorption PEMFC Catalysts Study

- Netzsch STA-449 high precision, simultaneous TGA/DSC was relocated for surface coverage measurements
  - CO work required enhanced safety precautions - alarms, etc.
  - H<sub>2</sub>S use requires greater safeguards
- Unique Instrument Specifications
  - Rated vacuum tight at 10<sup>-4</sup> torr operation (required for work with toxic gases)
  - Unique thermostatic controlled balance unit
    - Lab room is subject to large temperature swings through 24hr period
    - Exceptional stability despite variations in ambient T
- Exceptional performance
  - 5 g maximum sample wt. held by special, large capacity “buckets” with use of TGA sample carrier
  - 0.1 µg resolution
  - Instrument rated at <1 µg/hr drift (best possible)
- Energetics of desorption may be studied with DSC

# Technical Approach: Gravimetry Procedure

- Two TG runs required for Analysis
  - 1<sup>st</sup> : used to clean surface of sample to prep it for CO absorption
  - 2<sup>nd</sup> : CO (1.1%)/Ar mixture is applied to sample and mass change is recorded
    - [CO] verified by GC analysis



\* No buoyancy corrections since experiments are isothermal.

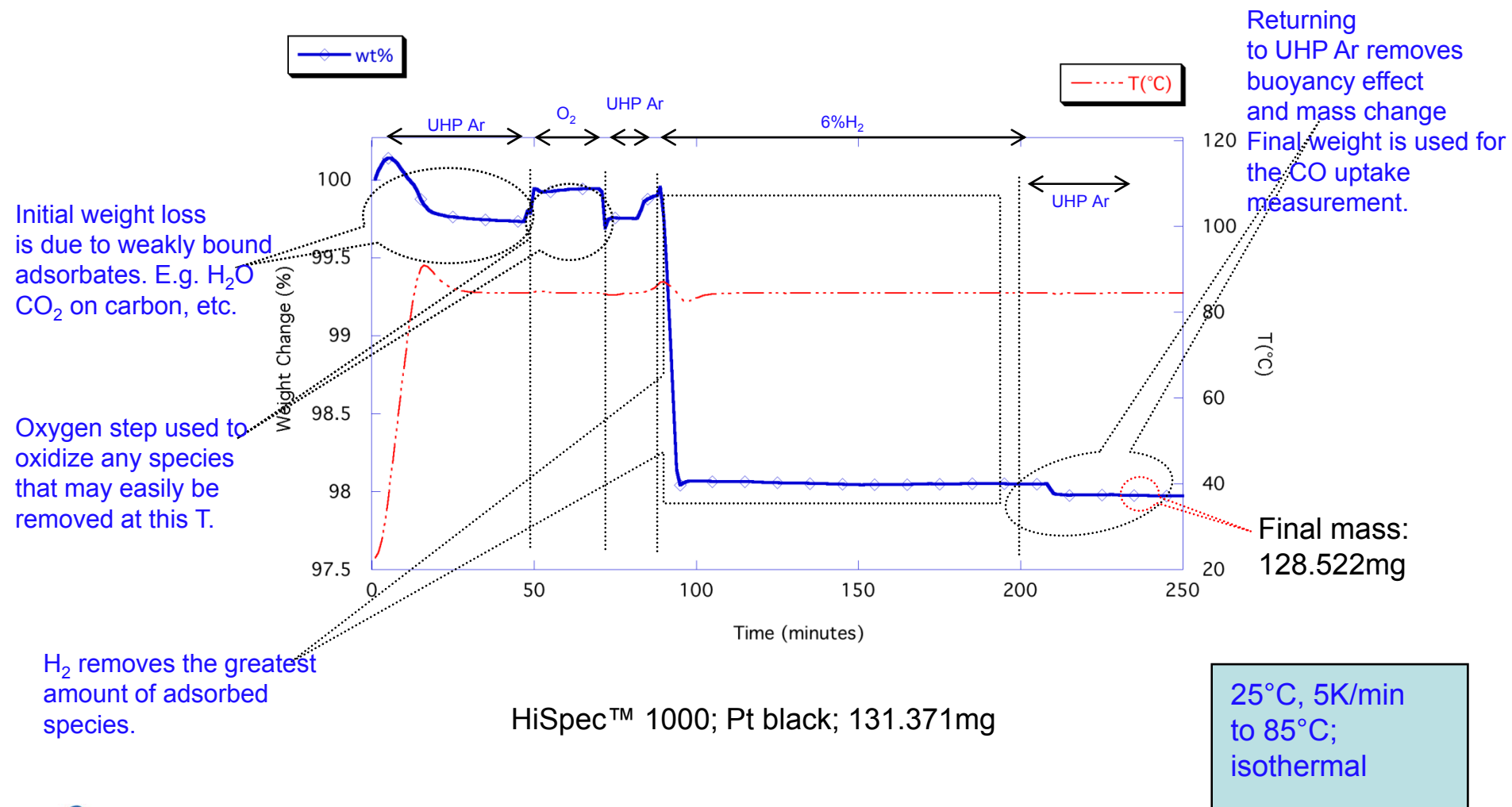
# Technical Approach: Experimental Details

- Catalyst samples examined in first series of experiments
  - Pt Black - Alfa HiSpec™ 1000
  - Pt/Al<sub>2</sub>O<sub>3</sub> - Alfa 5 wt% Pt on gamma alumina
  - Pt/XC-72 - ETEK 20 wt% Pt on carbon XC-72
- Samples were taken from manufacturers bottle and placed into a 3.4ml, high- volume, alumina TG crucible
  - Sample weight kept to around 100mg for each sample
- TG crucible placed onto TGA sample carrier and furnace closed and purged with UHP Ar
  - TGA previously tared and gas flowrates fixed for duration of experiment
  - VERY important that rotameter settings are not changed during the exp.

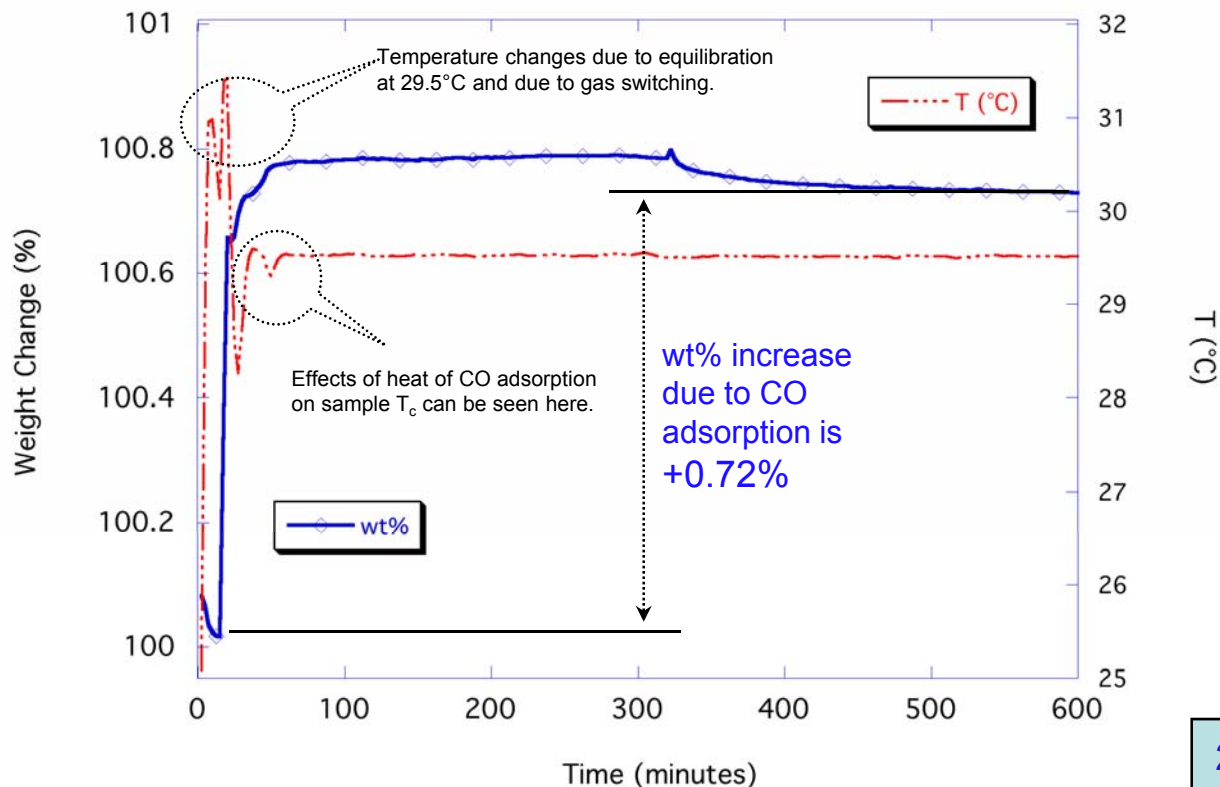


# Technical Accomplishments

## Procedure 1: Typical Cleaning Curve



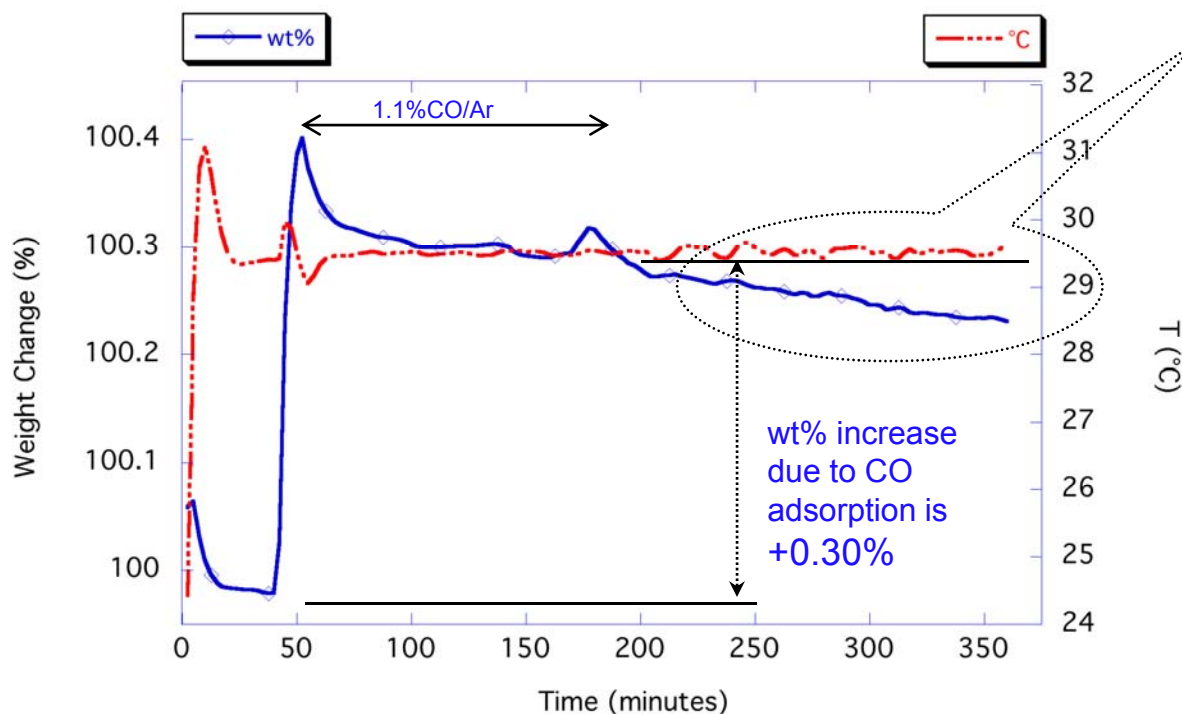
# Technical Accomplishments— CO adsorption/Pt Black



HiSpec™ 1000; Pt black cleaned; 128.522mg

25°C, 5K/min  
to 30°C;  
isothermal

# Technical Accomplishments— Pt (5wt%)/Al<sub>2</sub>O<sub>3</sub>



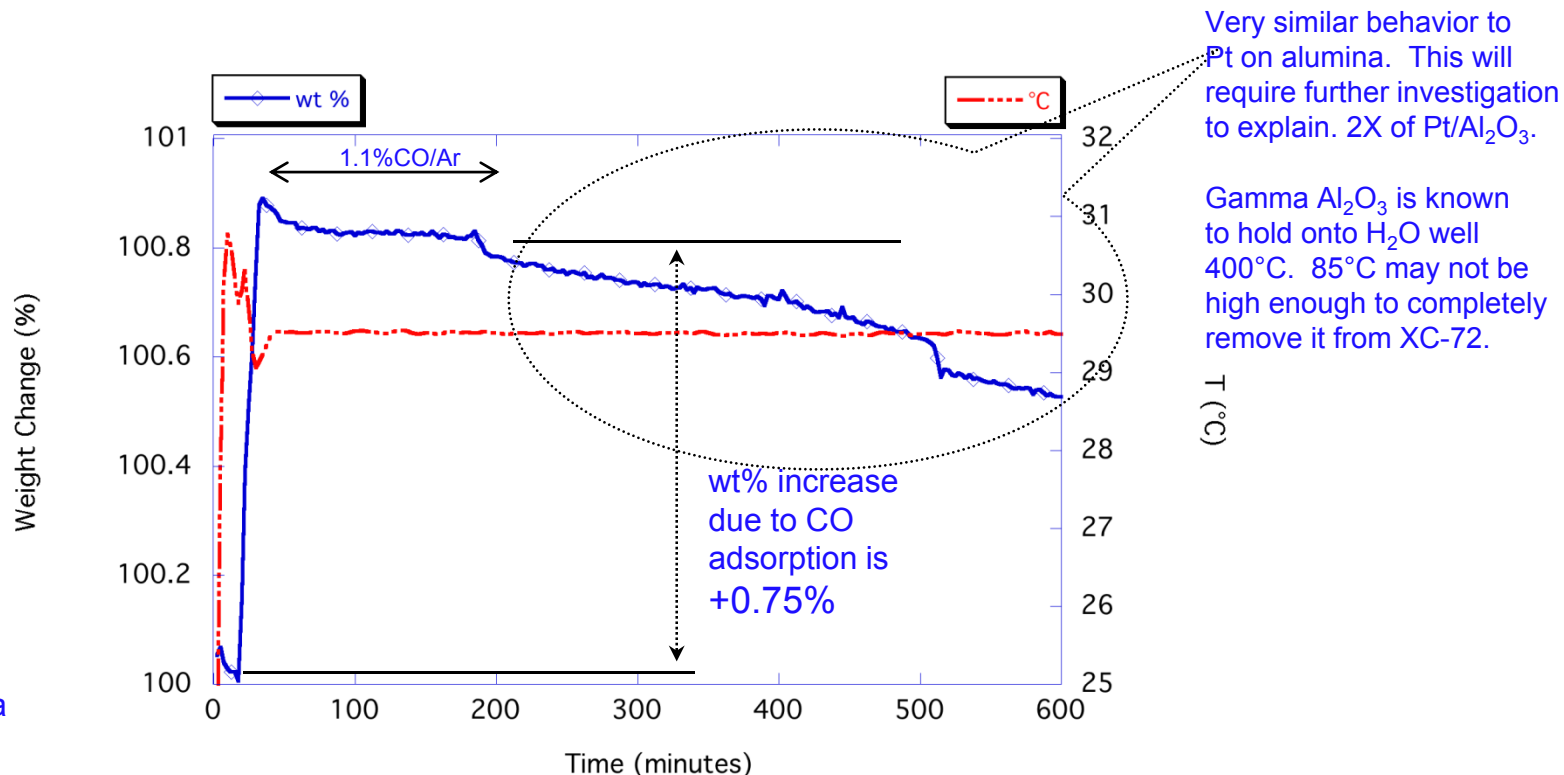
% increase due to CO adsorption on a Pt basis is + 5.97 wt% (immediately after CO absorption.)

Pt (5wt%)/Al<sub>2</sub>O<sub>3</sub>; cleaned; 120.613mg

Repeat experiments show loss is real, constant and well outside any mass Changes that may be attributed to instrument errors or gas flow Variations (by almost a factor of 3).  
• Tightly bound H<sub>2</sub>O?

25°C, 5K/min to 30°C; isothermal

# Technical Accomplishments— 20% Pt/C ETEK



% increase due to CO adsorption on a Pt basis is + 3.77 wt% (immediately after CO absorption.)

ETEK Pt (20wt%)/XC-72; cleaned; 123.286mg

25°C, 5K/min  
to 30°C;  
isothermal

# Summary and a note on experimental error

- On Pt Basis, CO coverage and calculated SA\*
  - HiSpec™ 1000 = +0.72wt%, 25.1m<sup>2</sup>/g
  - Pt (5wt%)/Al<sub>2</sub>O<sub>3</sub> = +5.97wt%, 210 m<sup>2</sup>/g
  - ETEK Pt(20)/XC-72 = +3.77wt%, 132 m<sup>2</sup>/g
- Both Pt/Al<sub>2</sub>O<sub>3</sub> and ETEK catalysts showed a high rate of weight loss after CO flow was terminated (approx. 20 and 40µg/hr respectively). This requires further investigation.
- Worst case drift rates due to temperature-induced gas flow variations have been measured on the order of 7-8µg/hr with the average observed to be around 2-3µg/hr.
  - Potential error of 0.04% for the sample sizes and durations used in this work.
- Drift is cyclic (T & P) and averaged over several days is less than 1µg/hr.

\* using a value of  $1.63 \times 10^{-19} \text{m}^2/\text{CO molecule}$  calculated from the work of K. Shinozaki, T. Hatanaka, and Y. Morimoto, "Pt Utilization Analysis Using CO Adsorption," ECS Transactions, 11 (1) (2007) 497-507.

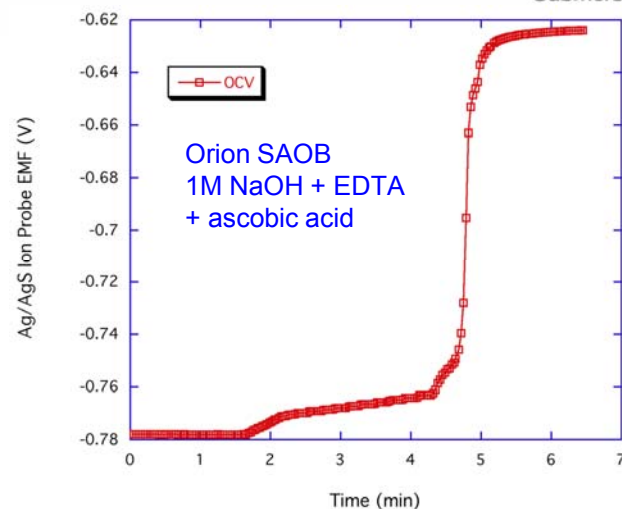
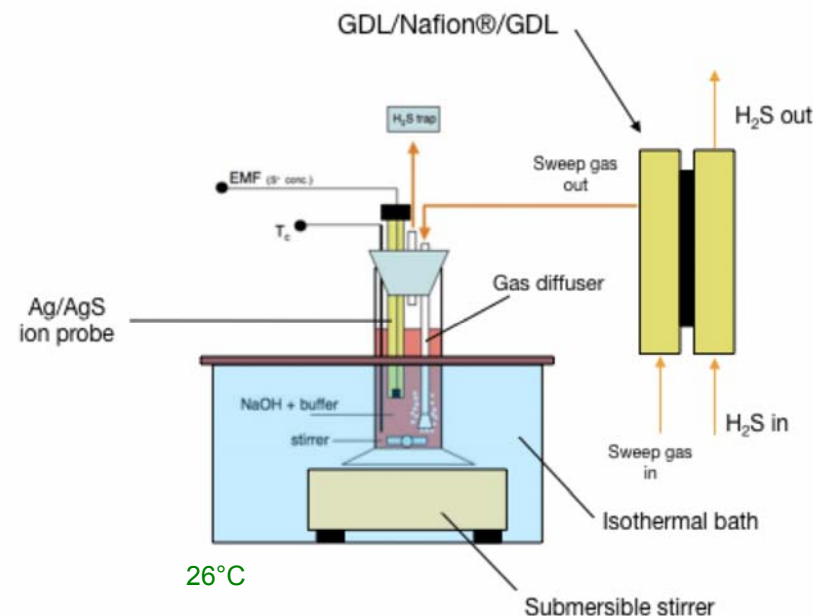
# Future Improvements to Gravimetric Capability

- **Mass flow controllers** to remove temperature- (and barometric pressure-) induced drift.
- Gas supply bottles must be **isothermal**.
- **Netzsch Aëolos quadrupole mass spectroscopy system** has been added to the STA-449 to correlate mass loss to gas species during cleaning, adsorption, and to probe any surface reactions occurring on the catalysts.
- **Other QMS applications** are being developed and applied at present time.

# Technical Accomplishments

## H<sub>2</sub>S Methods Update

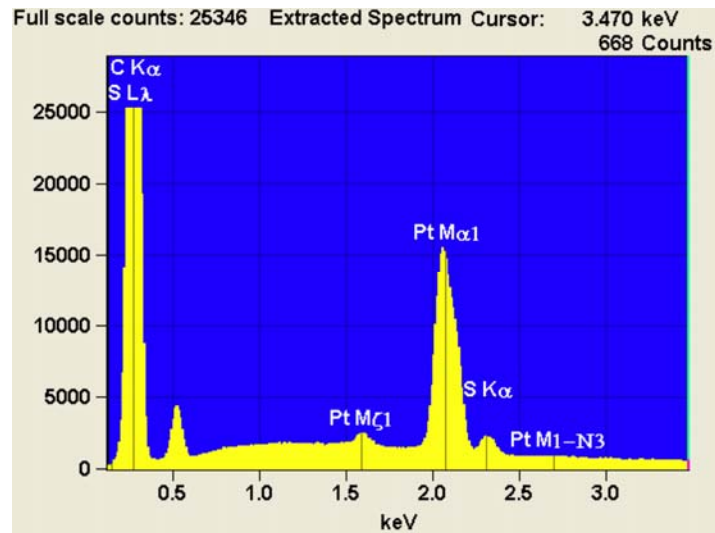
- Analytical technique using commercial Ag/AgS ion probes to trap and concentrate trace amounts of H<sub>2</sub>S present in gas streams and measure accumulated [S<sup>-</sup>] with low error.
- Low concentrations of H<sub>2</sub>S may be measured by concentrating in a high pH chemical trap with anti-oxidant additives over a known period of time (Orion® SAOB diluted 50 vol%).
  - Integration followed by lead nitrate titration using ion probe to determine endpoint.
  - Cumulative errors determined for titration process (including errors assoc. with volume meas., preparation of [Pb<sup>2+</sup>] titrant, etc.) is 2%.
- Method successfully used to measure trace quantities of H<sub>2</sub>S permeating through Nafion® polymers .
  - Methods used for N117, N112, and N212 membranes at 25°C
  - 50 cm<sup>2</sup> with GDL (no catalyst), 1000ppm and 96 ppm sources of H<sub>2</sub>S used, mixed from pure H<sub>2</sub>S



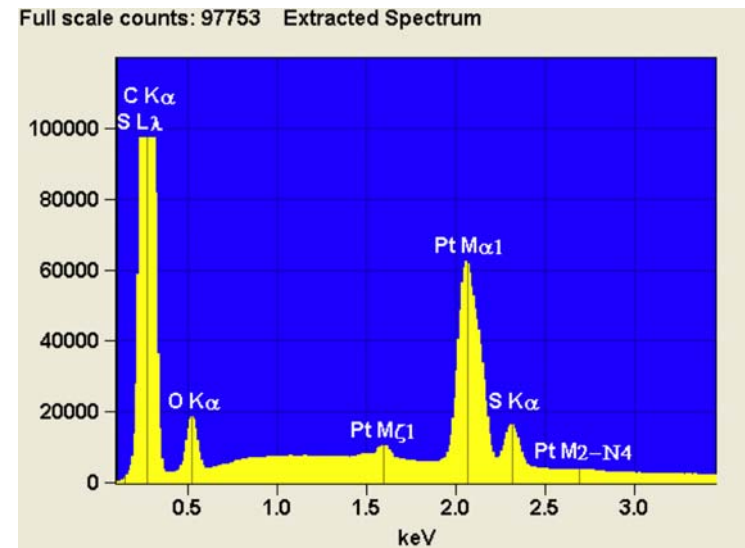
Sample titration of a 60ml trap used to capture H<sub>2</sub>S permeating through N112 at a rate of 40 ng/s.

# Technical Accomplishments

## Complementary Sulfur Analytical Technique



As received S from carbon support



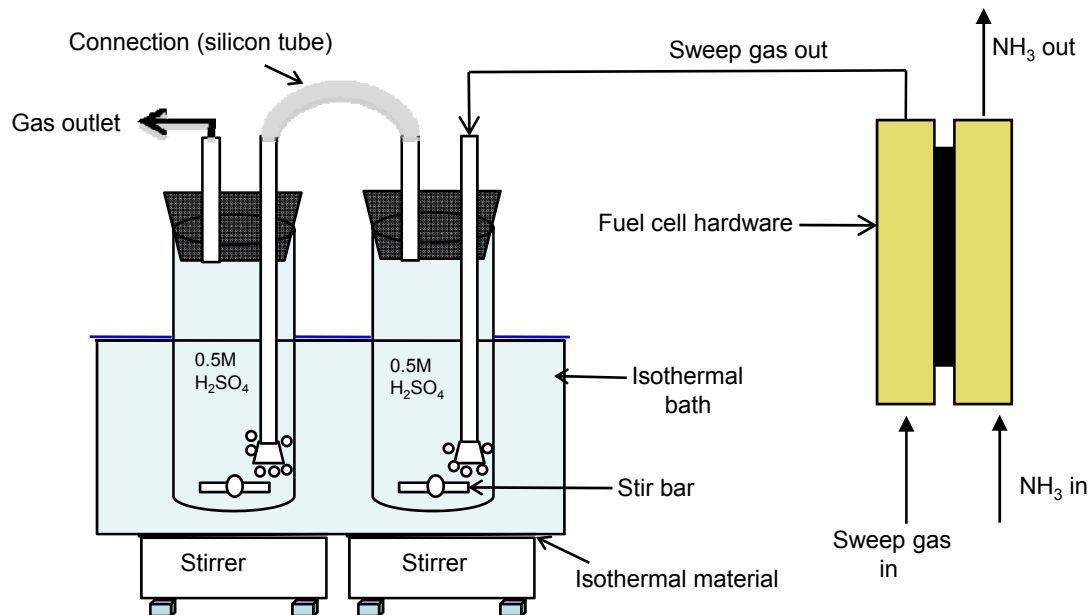
After H<sub>2</sub>S Exposure carbon

ESEM shows 2% S<sub>wt</sub> gain after Pt/C which agrees with LANL-developed ultra-low H<sub>2</sub>S analytical technique similar conditions



# Technical Accomplishment

## Ammonia Method Development

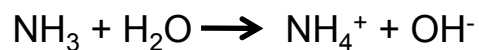


Erlenmeyer in series configuration, immersed in a water bath at 10-15°C while collecting the outlet gas

The ammonia quantified by modified ASTM method for ammonia/nitrogen in water

# Ammonia Method

The ammonia in solution permeates through the membrane and dissolves in the internal filling solution (0.1M  $\text{NH}_4\text{Cl}$  solution), reacting reversibly with water and altering the pH of the internal solution.



- The working electrode potential, sensitive to  $\text{OH}^-$ , is governed by Nernst equation,

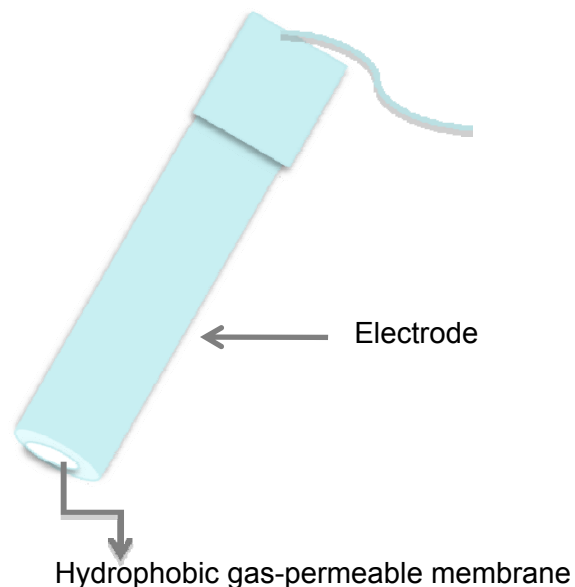
$$E = E_0 - S \log [\text{OH}^-]$$

Since the filling solution has a sufficiently high concentration of  $\text{NH}_4\text{Cl}$ :

$$[\text{OH}^-] = [\text{NH}_3] \times K_{\text{eq}}$$

the electrode response to ammonia is also

$$E = E_0' - S \log [\text{NH}_3]$$

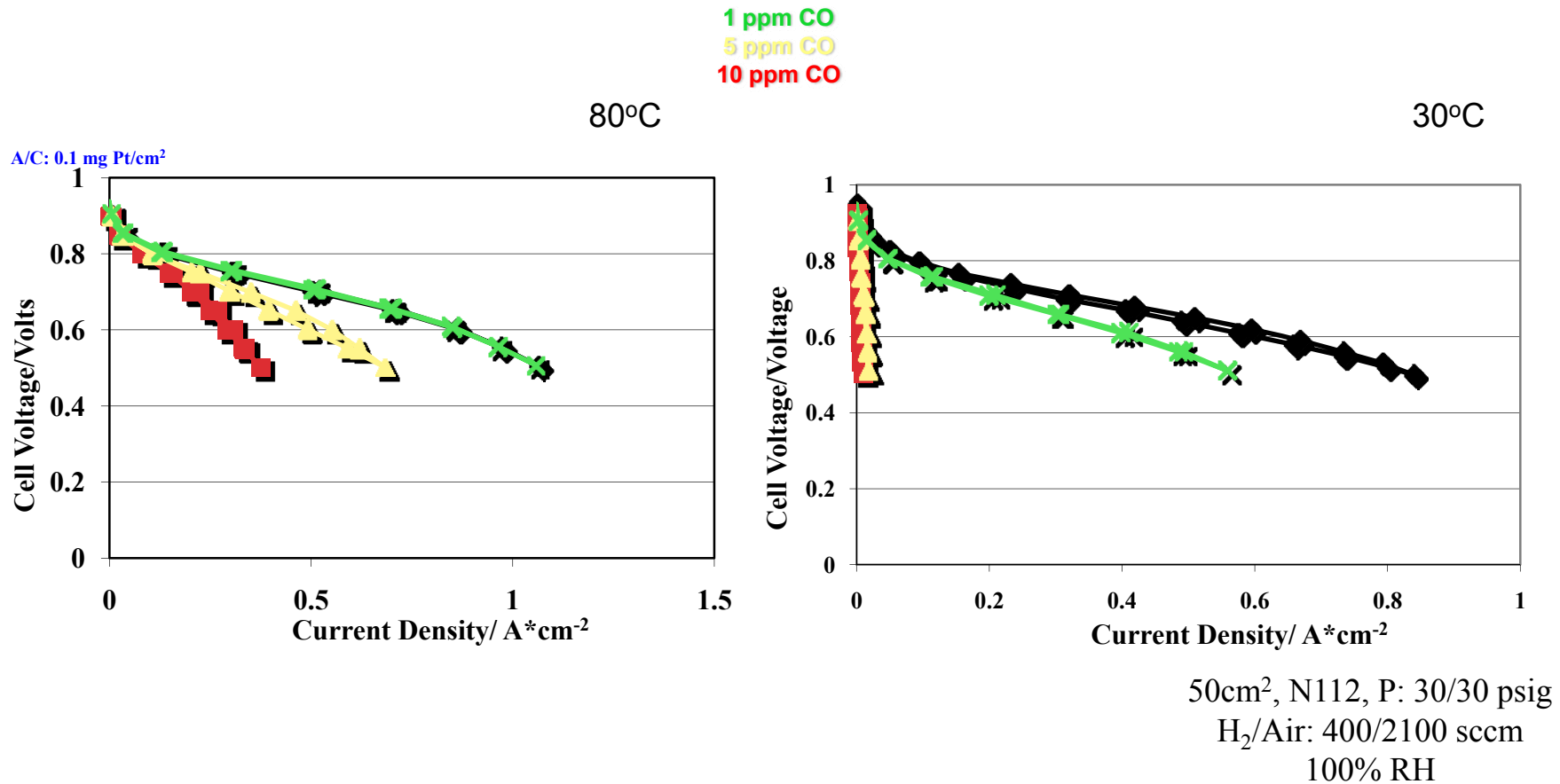


Equilibrium equation:

$$K_{\text{eq}} = \frac{[\text{NH}_4^+][\text{OH}^-]}{[\text{NH}_3]}$$

# Carbon Monoxide Results

Concentration, Temp, Pt loading



- The increase in CO concentration translates to an increase in performance loss
- At low Pt loadings\* and 80°C; tolerance to 1 ppm CO is achievable
- Clearly as the temperature decrease so does the CO tolerance this maybe problematic during start-up.

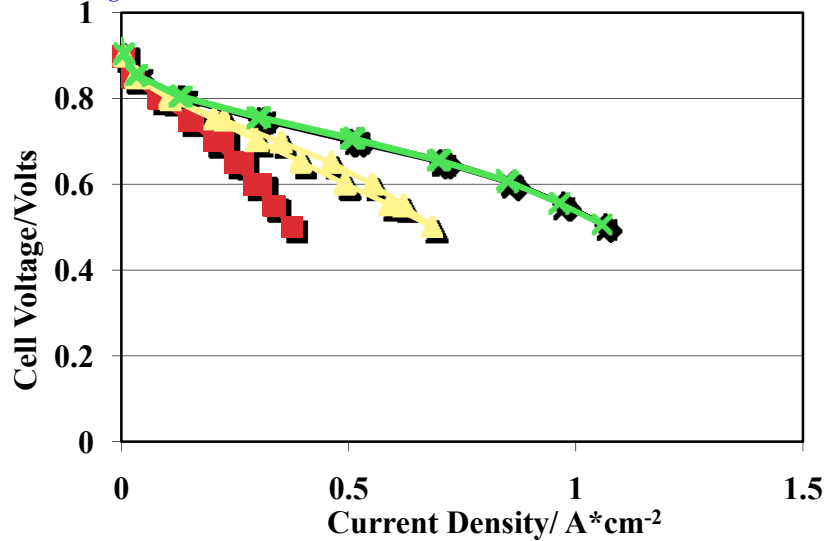
# Carbon Monoxide Results

Concentration, Temp, Pt loading

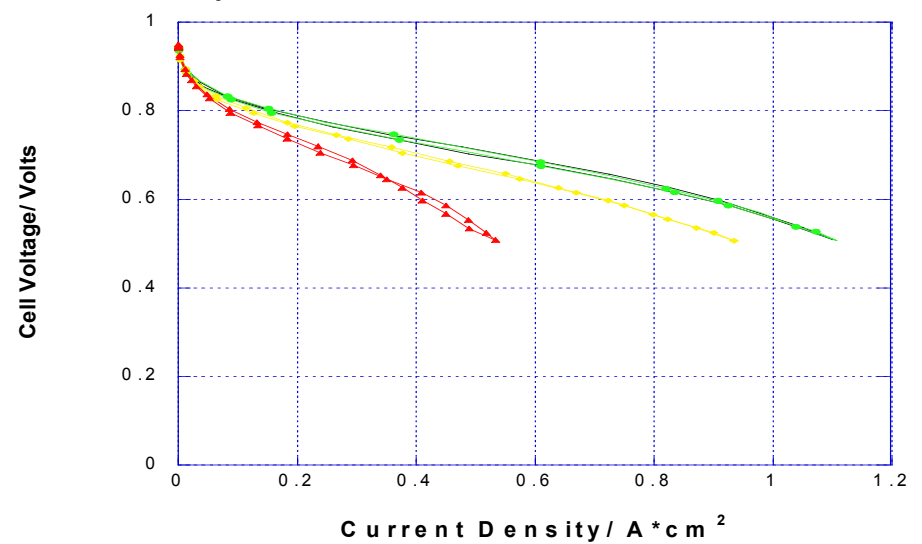
1 ppm CO  
5 ppm CO  
10 ppm CO

80°C

A/C: 0.1 mg Pt/cm<sup>2</sup>



A/C: 0.1/0.2 mg Pt/cm<sup>2</sup>

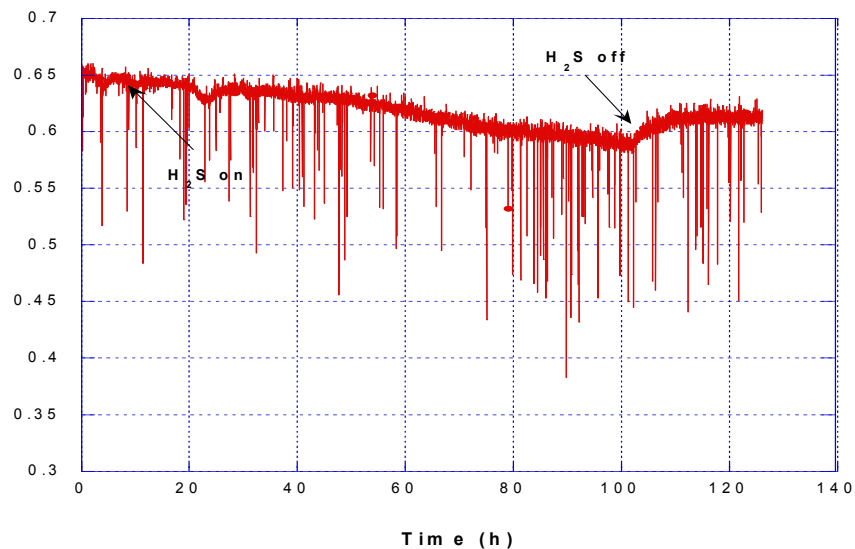


50cm<sup>2</sup>, N112, P: 30/30 psig  
H<sub>2</sub>/Air: 400/2100 sccm  
100% RH

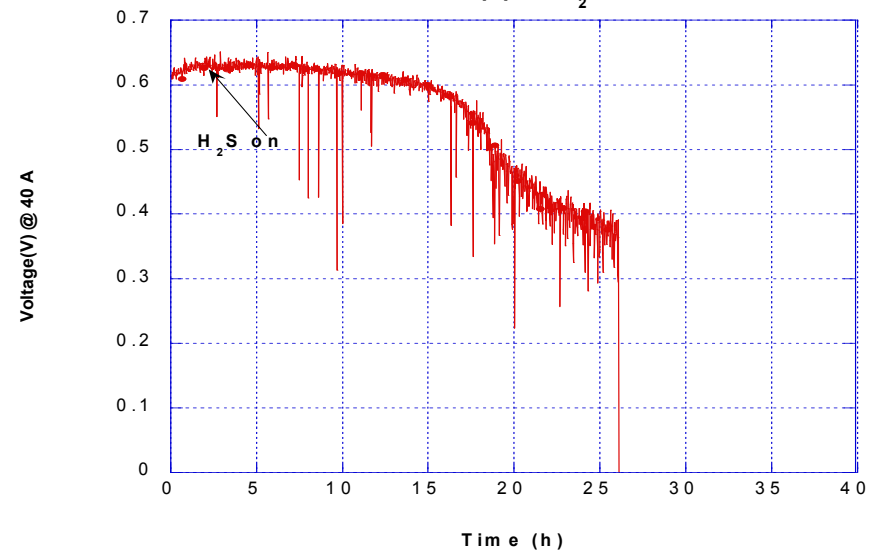
- Clearly changing the cathode loading does not impact the CO tolerance.
- Results nearly identical for two different FC with 0.1 mg Pt/cm<sup>2</sup> on the anode

# H<sub>2</sub>S Results

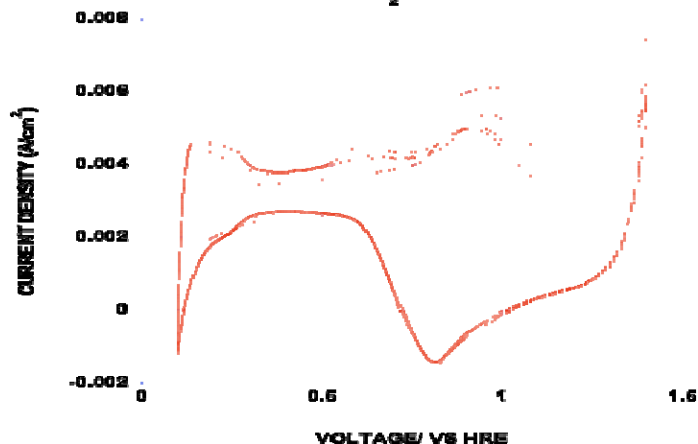
100 ppb H<sub>2</sub>S



250 ppb H<sub>2</sub>S



100 ppb H<sub>2</sub>S for 100hrs



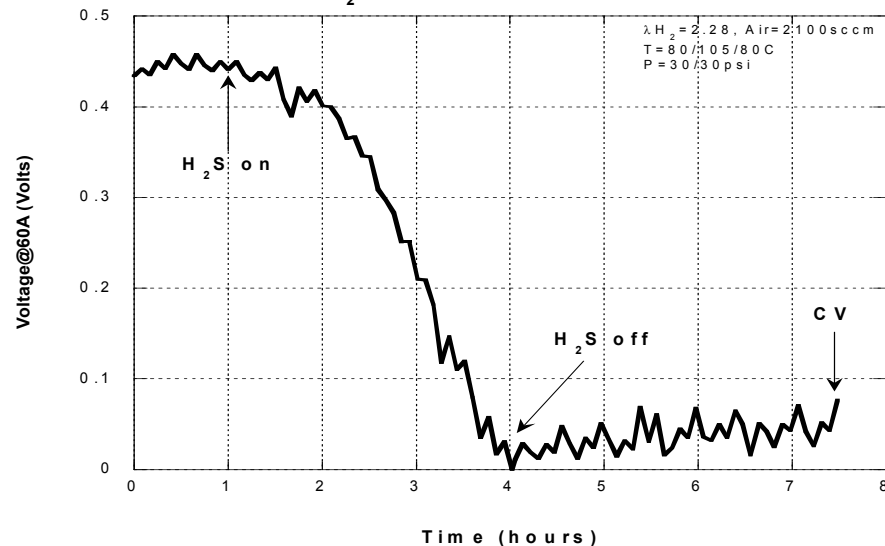
2 mil, /0.1/0.2 mg Pt/cm<sup>2</sup>  
80°C, 100% RH, 30 psig

H<sub>2</sub>/N<sub>2</sub>: 500 sccm; 80°C, 100% RH(sat)  
Scan rate: 20 mV/S, Sweep 0.1-1.4 V

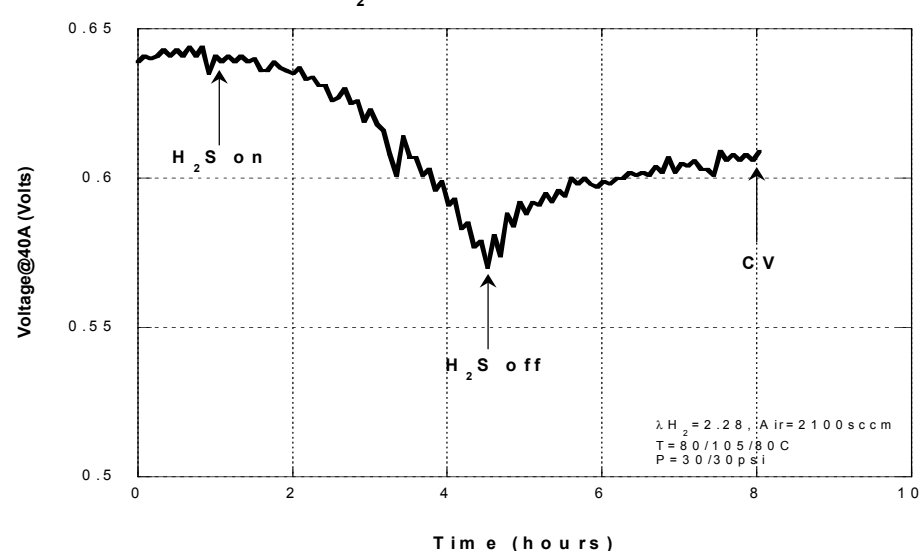
# H<sub>2</sub>S Results

2 mil, 0.2 mg Pt/cm<sup>2</sup>  
80oC, 100% RH, 30 psig

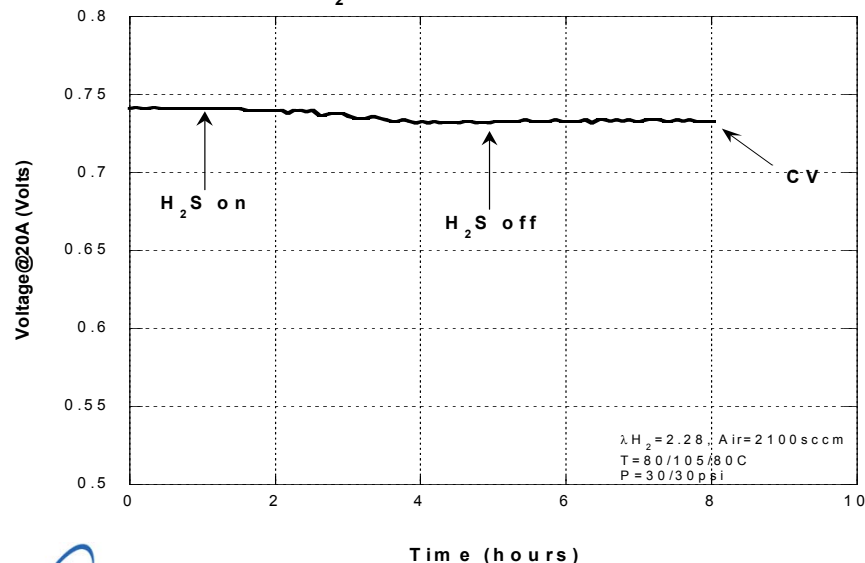
0.5 ppm H<sub>2</sub>S poisoning for 3.5 h at 60 A



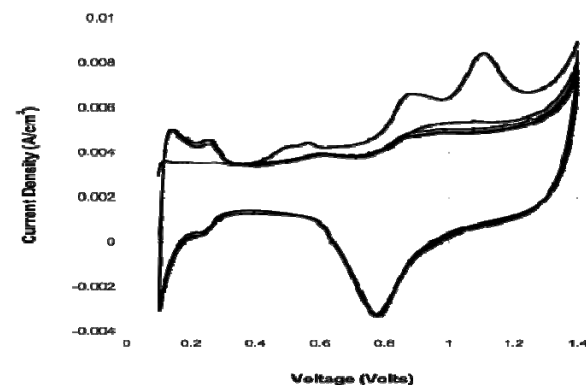
0.5 ppm H<sub>2</sub>S poisoning for 3.5 h at 40 A



0.5 ppm H<sub>2</sub>S poisoning for 3.5 h at 20 A



CR50608\_anodeCV\_0.5 ppm H<sub>2</sub>S @40A for 3.5h +3.5h recovery

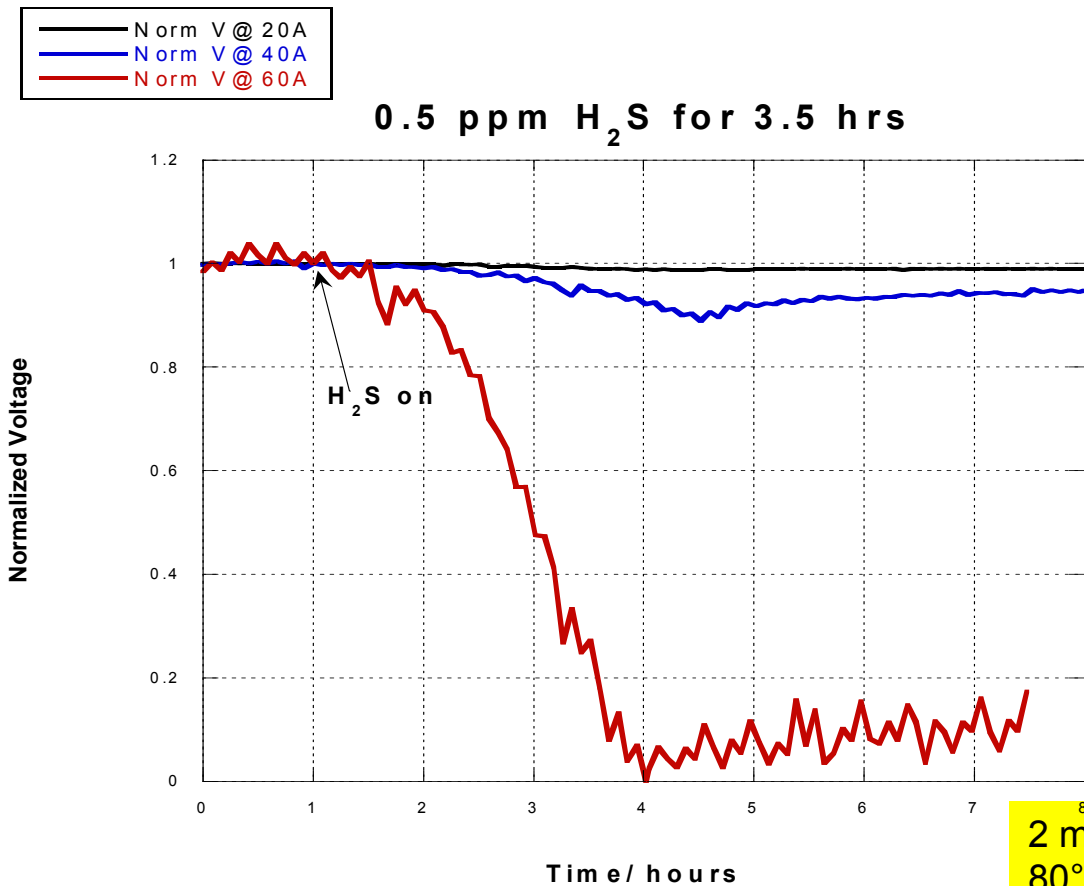


H<sub>2</sub>/N<sub>2</sub>: 500 sccm; 80oC, 100% RH(sat)  
Scan rate: 20 mV/S, Sweep 0.1-1.4 V

- Voltage response for 0.5 ppm H<sub>2</sub>S short term exposure at different currents
- Cyclic Voltammetry used to oxidize S-species from Pt surface (cleaning?)

# H<sub>2</sub>S Results

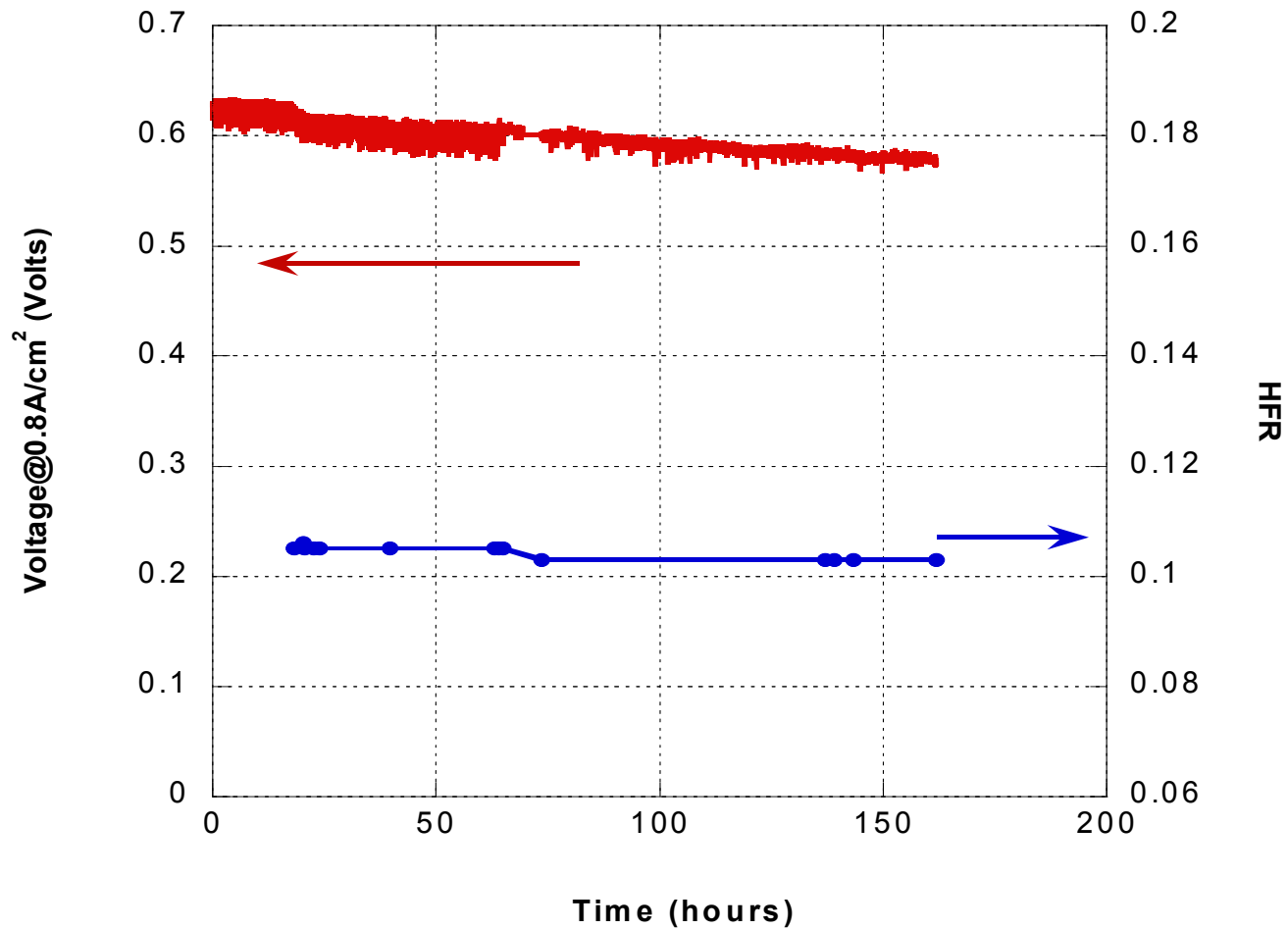
Current dependence/Normalized voltage



- Performance degradation more pronounced at higher currents (i.e. low voltages.)  
(Voltage-dependence and/or S-crossover)

# Ammonia Studies

1 ppm  $\text{NH}_3$ , 40 A, 80°C, 100% RH



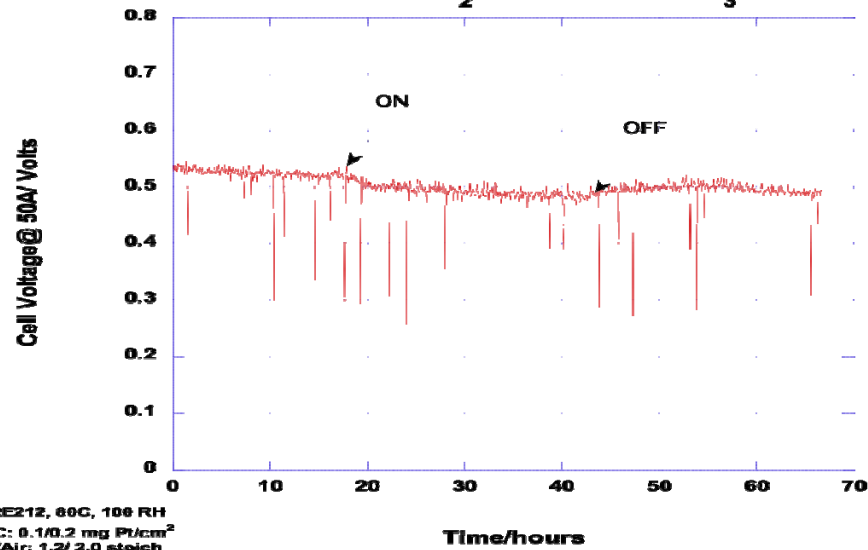
Voltage response over time for 1 ppm  $\text{NH}_3$ , HFR remain constant



# Combined Ammonia Studies

B

Effects of 10ppb  $H_2S$  and 1ppm  $NH_3$  Mixture

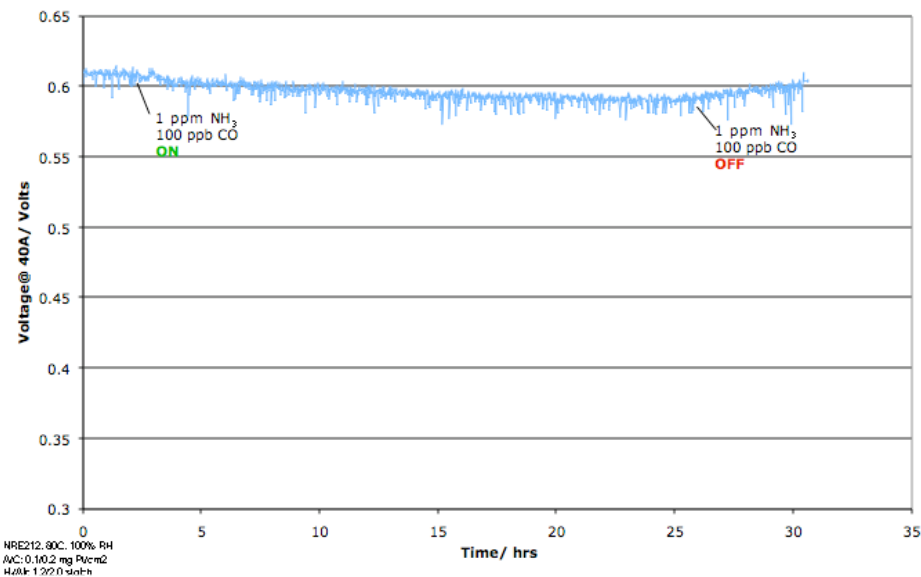


- $NH_3$  showed 20 mV loss in 24 hrs
- $H_2S/NH_3$  mixture showed 38 mV losses in 24 hrs
- $CO/NH_3$  mixture showed 20 mV losses in 24 hrs
- CVs show minimal adsorbates, HFR constant

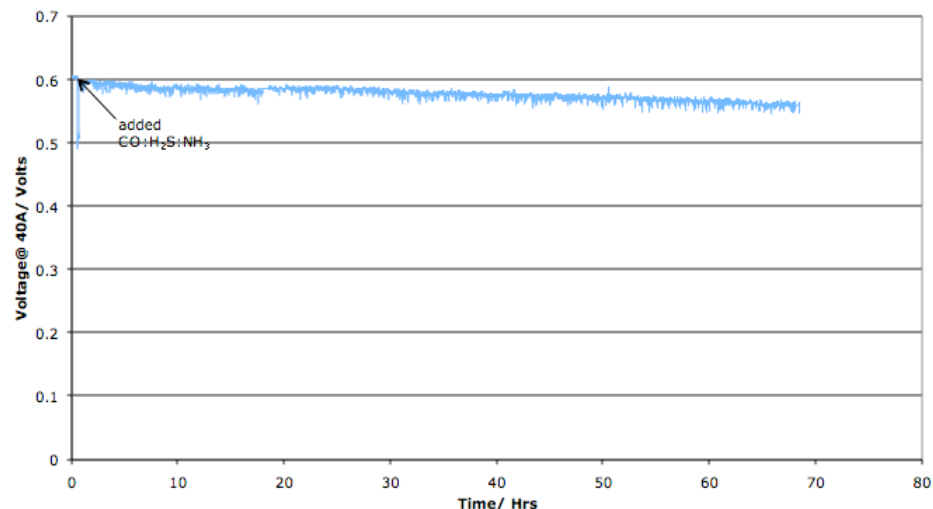
- $CO/H_2S/NH_3$  shows 52 mV losses over 70 hrs (HFR increased  $0.003 \Omega \cdot cm^2$ ) ~ 2.4 mV loss

## •Sources of Losses?

Effects of 100 ppb  $CO$  and 1 ppm  $NH_3$  Mixture



Mixture of 100 ppb  $CO$ : 4 ppb  $H_2S$ : 1 ppm  $NH_3$   
A/C: 0.1/0.2 mg Pt/cm<sup>2</sup>  
80°C, 100% RH, 83% Utilization



# Technical Accomplishments Summary

- *Completed DOE round robin study by including data sets from NIST and the final from LANL*
- Analytical method for measuring trace levels of Sulfur developed. Now being used to quantify S permeation rates.
- Tested critical constituents (CO, H<sub>2</sub>S, and NH<sub>3</sub>) individually and in combination

## Future Work

- Optimization of our analytical method for H<sub>2</sub>S and modifying it for in-line analysis.
- Complete initial development of ammonia analytical method
- Continue testing the critical constituents (CO, H<sub>2</sub>S, and NH<sub>3</sub>) and populating the test matrix.
- Continue providing data sets and interacting with FC modelers.