

# Geothermal Technologies Program 2010 Peer Review



## ***Air-Cooled Condensers in Next-Generation Conversion Systems***

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**Track: Specialized  
Materials and Fluids and  
Power Plants**

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# ***Project Overview***

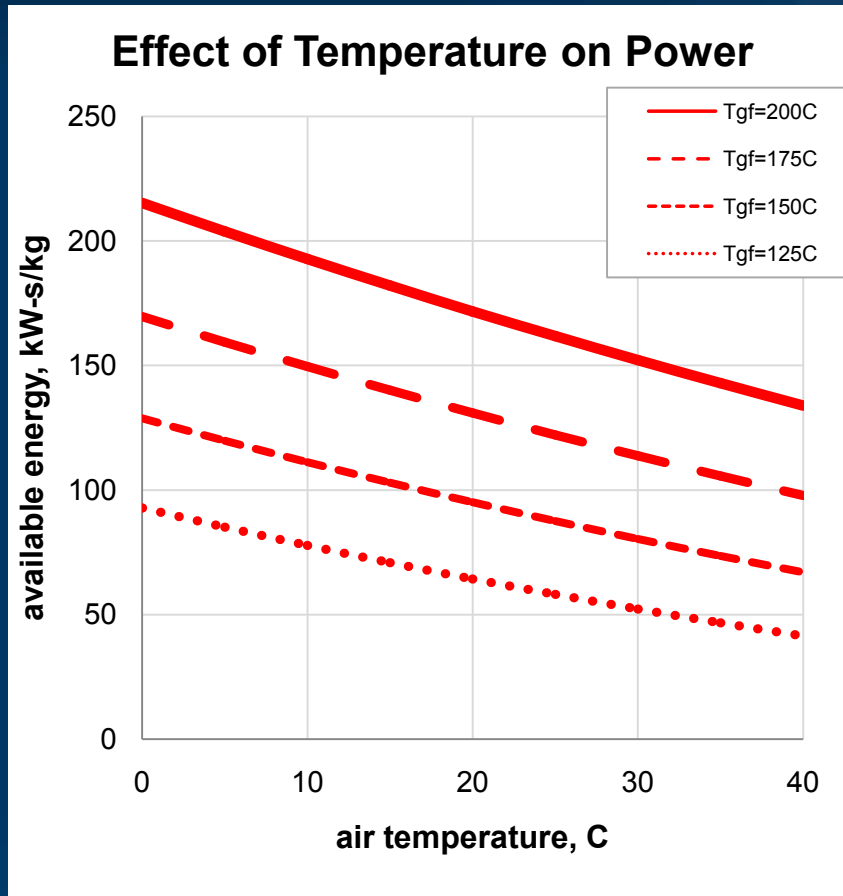
- **Timeline:**
  - Start Date: October 2009
  - End Date: September 2011
  - ~15% Complete
- **Budget:**
  - FY2010: \$375K
  - FY2011: \$435K
- **Barriers:**

The impact of air-cooling on plant performance and the costs of air-cooled condensers are barriers that will impact DOE's goal to develop low-cost conversion systems that are more efficient for both EGS and low-temperature resources.
- **Partners: None**

## *Relevance/Impact of Research:*

- The overlying objective is to reduce the costs associated with the generation of electrical power from air-cooled binary plants
- Premise for this work: No water is available for evaporative cooling
- Issues with Air-Cooling
  - Amount of heat rejected – up to ~90% of heat added is rejected
  - Cost - 30 to 45% of Capital Equipment Cost (EPRI Next Generation Geothermal Power Plant study)
  - Fan power - up to 10% of generator output
  - Sensitivity to temperature change: @150°C ~1.4%  $\Delta$ available energy per °C  $\Delta$ air temperature

## *Relevance/Impact of Research:*



- Plant performance: function of source and sink temperatures, and conversion efficiency
- Conversion efficiency degrades with deviation from design temperatures
- Focus is on
  - Minimizing the effect of temperature changes on conversion efficiency
  - Increasing conversion efficiency by using mixed working fluids

## ***Scientific/Technical Approach***

- Assume no consumptive use of water
- Two resource scenarios (200° and 150°C); two representative locations (Grand Junction CO and Houston TX)

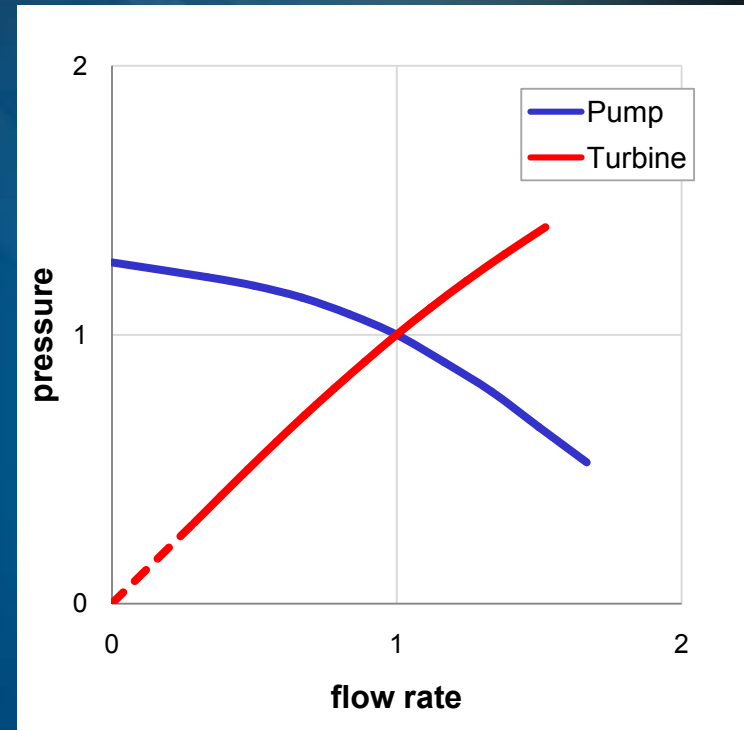
## **Design Conditions**

- Design condition: maximum net power for each scenario – resource temperature, location and outlet temperature constraint
  - Fixed geothermal fluid flow rate
  - Working fluids: iC5, iC4, nC4, C3, R134a, R245fa
  - Incorporate realistic operating parameters (pinch points, efficiencies,  $\Delta P$ 's)
- Evaluate benefit of technologies not used in conventional hydrothermal plants
- Estimate capital cost based on predicted equipment sizes

# Scientific/Technical Approach - continued

## Off-Design:

- Fix equipment sizes for selected design condition
- Include effect of flow and temperature changes on heat transfer coefficients, efficiencies,  $\Delta P$ 's
- Account for effect of turbine on working fluid flow
- Identify conditions giving maximum power for different ambient and resource temperature conditions.
- Project power production over project life
- Evaluate the potential to decrease generation costs
  - Selection of design conditions for ambient and turbine
  - Other concepts (changing working fluids, allowing expansions inside two-phase region)



*Relationship Between Turbine and Pump Flow*



## ***Scientific/Technical Approach - continued***

### **Working Fluid Mixtures:**

- **Evaluate effect of composition and tube orientation on condensing film coefficient**
  - Test data from Heat Cycle Research Facility
  - Tube orientations of 90° (vertical), 60°, and 15°
  - Isobutane and hexane mixtures (0 to 15% hexane)
  - Propane and isopentane mixtures (0 to 40% isopentane)
- **Use data to refine predictive methods for condensing coefficients**
- **Integrate results into a condenser design model capable of evaluating the suitability of at least one commercially available design with these fluids**
- **Identify any potential issues with the design and provide recommendations**

# ***Scientific/Technical Approach - continued***

## **Milestones:**

- Sep 10    Complete Task 1 – Analysis of impact resource decline and ambient temperatures on air-cooled binary plant output, and the potential to mitigate those impacts with existing technologies**
- Feb 11    Complete evaluation of effect of mixture composition and tube orientation on condensing film coefficients**
- Sep 11    Complete Task 2 – Assessment of the suitability of existing condenser designs for mixed working fluids**

## **Decision Points:**

- The methodology used to evaluate existing condenser designs – February 2011**
- Selection of the commercial design to be evaluated (will be largely dictated by the data from the prior testing) – March 2011**

## **Status:**

- Designs have been established for both resource conditions at both locations, and the benefits from a design using recuperation identified**
- Fixed plant design models will be completed in early May**



# Accomplishments, Expected Outcomes and Progress

- Design conditions determined for both resource temperatures at each location (design at mean annual air temperature)
- Benefit of recuperation evaluated for each scenario
  - Positive impact on power only if constraint on outlet temperature
  - No benefit at lower resource temperature
- Model is being modified to fix equipment and reflect impact of varying flow rates and temperature on heat transfer, efficiencies and  $\Delta$ pressure

| <i>Location</i>       | <i>T<sub>gf</sub></i> | <i>Design with no outlet constraint</i> | <i>Design with outlet constraint</i> | <i>Design with Recuperation</i> |
|-----------------------|-----------------------|---|--------------------------------------|---------------------------------|
| <i>Grand Junction</i> | <i>200°C</i>          | <i>87.2 kW-s/kg</i>                     | <i>76.6 kW-s/kg</i>                  | <i>81.8 kW-s/kg</i>             |
|                       | <i>150°C</i>          | <i>41.5 kW-s/kg</i>                     | <i>41.5 kW-s/kg</i>                  | <i>40.5 kW-s/kg</i>             |
| <i>Houston</i>        | <i>200°C</i>          | <i>76.0kW-s/kg</i>                      | <i>70.3 kW-s/kg</i>                  | <i>73.2 kW-s/kg</i>             |
|                       | <i>150°C</i>          | <i>32.8 kW-s/kg</i>                     | <i>32.8 kW-s/kg</i>                  | <i>32.4 kW-s/kg</i>             |

# ***Accomplishments, Expected Outcomes and Progress***

## **Mixed Working Fluids**

- **Non-isothermal boiling and condensing allow heat transfer irreversibility to be reduced**
- **Prior work by Demuth and Whitbeck**
  - +20% increase in plant performance
  - Cost benefit if well field development costs equivalent to or greater than plant cost
- **Vaporization of mixtures**
  - Replicate benefit with pure fluid in supercritical cycles
- **Condensation of mixtures**
  - Can not replicate with pure fluids
  - Prior work successful – in-tube condensation, non-horizontal tube orientation, water cooled condensers

***Can benefits be achieved in air-cooled condensers?***

## ***Project Management/Coordination***

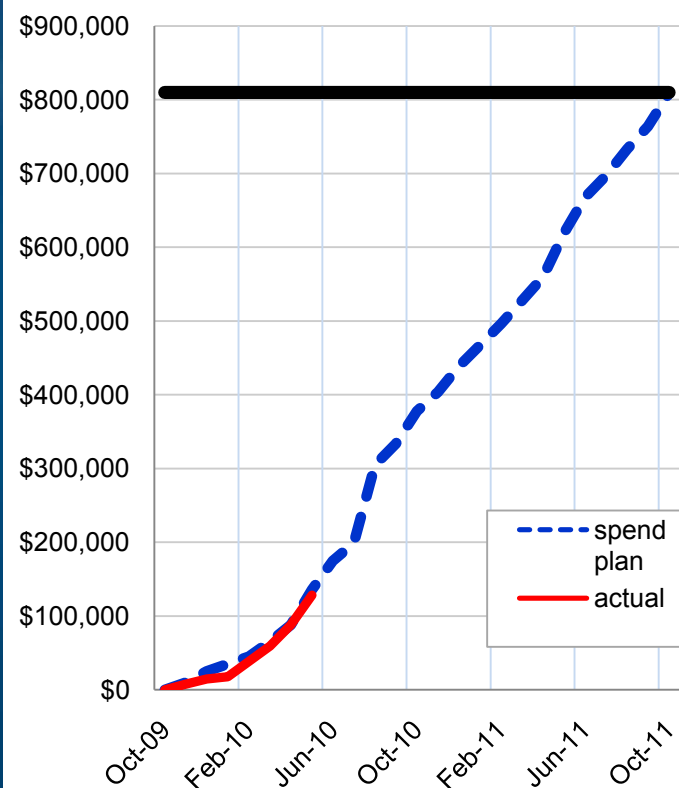
- **With determination that final year of funding would not be provided, project work scope and schedule were revised to focus on binary conversion systems**
- **Activity has been planned to maximize use of existing resources**
  - **Previously developed model of binary plants**
  - **Software platforms (Aspen) available at the INL**
  - **Prior work on the evaluation of binary turbine performance**
  - **Test data from the Heat Cycle Research Facility (mixed working fluids)**
- **Work has been planned to facilitate ‘learning curve’ of staff having no prior geothermal experience**
- **Cost and schedule are monitored and reported internally on a monthly basis**

# Project Management/Coordination

**Air-Cooled Condensers in Next Generation Conversion Systems**

| ID | Task Name  | Start     | Finish    | 2009 |    |    |    | 2010 |    |    |    | 2011 |    |    |    |
|----|--|-----------|-----------|------|----|----|----|------|----|----|----|------|----|----|----|
|    |  |           |           | Q1   | Q2 | Q3 | Q4 | Q1   | Q2 | Q3 | Q4 | Q1   | Q2 | Q3 | Q4 |
| 1  | AIR-COOLED BINARY CYCLE  | 10/1/2009 | 8/31/2010 |      |    |    |    |      |    |    |    |      |    |    |    |
| 2  | 1. Identify concepts, scenarios, configure binary plant model                | 10/1/2009 | 3/1/2010  |      |    |    |    |      |    |    |    |      |    |    |    |
| 3  | 2. Determine performance benefits  | 1/15/2010 | 7/15/2010 |      |    |    |    |      |    |    |    |      |    |    |    |
| 4  | 3. Estimate $\Delta$ capital costs   | 5/3/2010  | 7/30/2010 |      |    |    |    |      |    |    |    |      |    |    |    |
| 5  | 4. Solicit industry comment  | 6/1/2010  | 7/30/2010 |      |    |    |    |      |    |    |    |      |    |    |    |
| 6  | 5. Document results/recommendations  | 7/1/2010  | 8/31/2010 |      |    |    |    |      |    |    |    |      |    |    |    |
| 7  | AIR-COOLING WITH MIXED WF's  | 8/2/2010  | 9/30/2011 |      |    |    |    |      |    |    |    |      |    |    |    |
| 8  | 1. Use prior work to establish impact of mixtures on condensing coefficients | 8/2/2010  | 2/1/2011  |      |    |    |    |      |    |    |    |      |    |    |    |
| 9  | 2. Evaluate suitability of selected Air-Cooled Condenser design for mixtures | 2/2/2011  | 7/1/2011  |      |    |    |    |      |    |    |    |      |    |    |    |
| 10 | 3. Identify design deficiencies and changes needed                           | 6/1/2011  | 8/15/2011 |      |    |    |    |      |    |    |    |      |    |    |    |
| 11 | 4. Solicit industry comment  | 7/1/2011  | 9/1/2011  |      |    |    |    |      |    |    |    |      |    |    |    |
| 12 | 5. Recommendations for further work  | 7/15/2011 | 9/15/2011 |      |    |    |    |      |    |    |    |      |    |    |    |
| 13 | 6. Final Report  | 7/1/2010  | 9/30/2011 |      |    |    |    |      |    |    |    |      |    |    |    |

**Spend Plan for Air Cooled Condenser Task**



## ***Future Direction***

### **Remainder of FY2010**

- **Complete modeling of the effect of varying ambient temperatures and declining resource on binary plant output.**
- **Assess the selection of the design conditions for both the ambient temperature and turbine**
- **Identify concepts/technologies with the potential to lower generation costs**
- **Document findings**
- **Initiate work to examine condenser data from Heat Cycle Research Facility**

# ***Future Direction***

## **FY2011**

- **Determine effect of mixture composition and tube orientation on condensing film coefficients during testing at the Heat Cycle Research Facility**
- **Use these results to evaluate predictive methods**
- **Incorporate best predictive method(s) into model to evaluate existing condenser designs**
- **Select most promising design and assess suitability for use with mixtures**
- **Document findings**



# *Summary*

- The heat source and sink temperatures define the maximum power a cycle can produce
- This work seeks to minimize the impact of variations in the source and sink temperature on the performance of a plant once it has been constructed
- Benefits of technologies that are applied to mitigate effects of off-design operation will be dependent upon the scenario evaluated
- Working fluid mixtures
  - Increase performance and plant cost
  - Reduce contribution of well field and reservoir to generation cost – lower generation cost if non-plant costs are significant
  - Questions whether non-isothermal condensation can proceed in commercial condenser designs