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Anaerobic MBR: Challenges & Opportunities

Symposium:
**Hydrogen, Hydrocarbons, and
Bioproduct Precursors from Wastewaters**
National Renewable Energy Laboratory
Washington, DC

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MWH[®]

BUILDING A BETTER WORLD

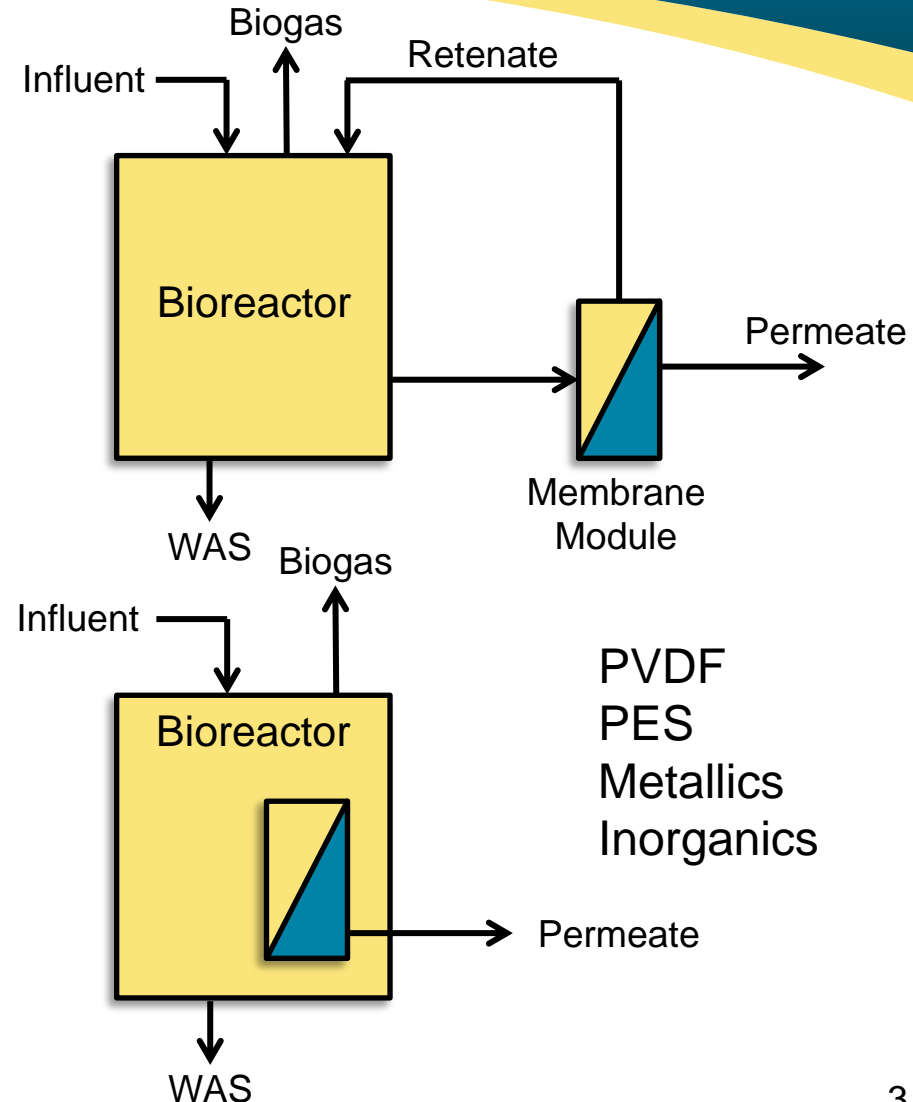
Outline

- Challenge for Municipal Wastewater
- Membrane Fouling
- Energy Potential
- System Economics
- Research Needs



Challenges: Municipal Wastewater Treatment Using AnMBR

- Low temperatures in municipal wastewaters
- Low strength municipal wastewaters
- Bioreactors must be heated
- Long SRTs are required
- Post-treatment is required for direct discharge
- High SO₄ reduces methane production
- Methane solubility at low temperatures limits recovery
- GHG emissions

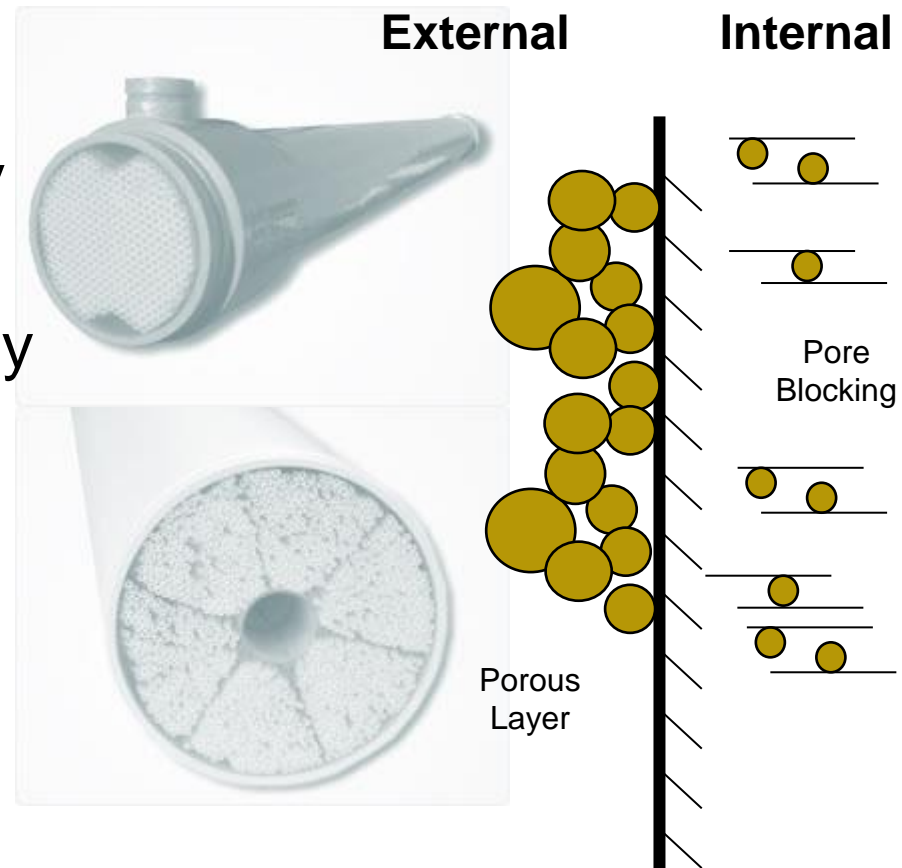


Challenges: Municipal Wastewater Treatment Using AnMBR

- Limited Development Realized Since Early 2000s
 - Anaerobic processes are complex
 - Methanogens highly sensitive to wastewater toxicity
 - Difficulty in managing variable conditions
 - Membrane fouling
 - Relatively low flux
- Necessity of Operating at Ambient Temperatures
 - Low organic strength → low methane production
 - Low methane production → limited heating potential
 - Long SRTs → increases membrane fouling

Challenges with Membrane Fouling

- Internal fouling generally irreversible
- External fouling generally reversible
- Internal deposits generally more inorganic
- Long SRT operation promotes internal pore blocking
- Fouling → higher costs & membrane replacement



Suspended biomass, colloidal solids, SMP, EPS, Attached cells, inorganics (e.g., struvite)

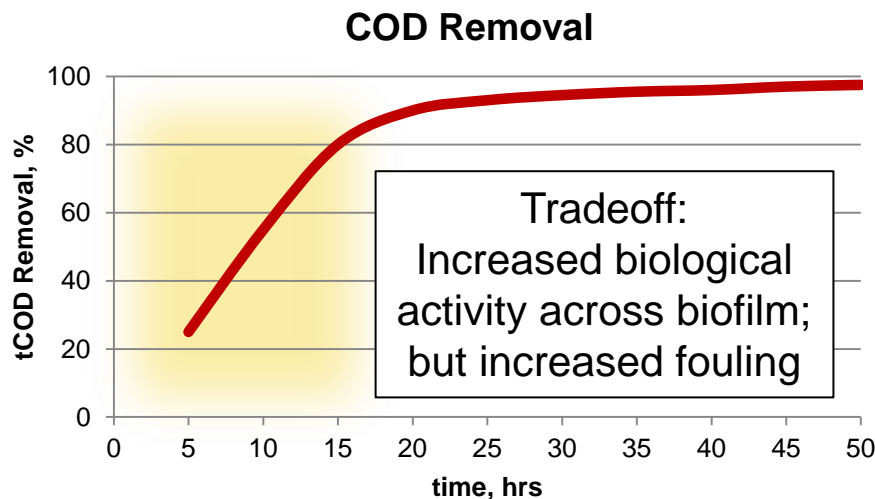
Membrane
Surface

Fouling Control Methods

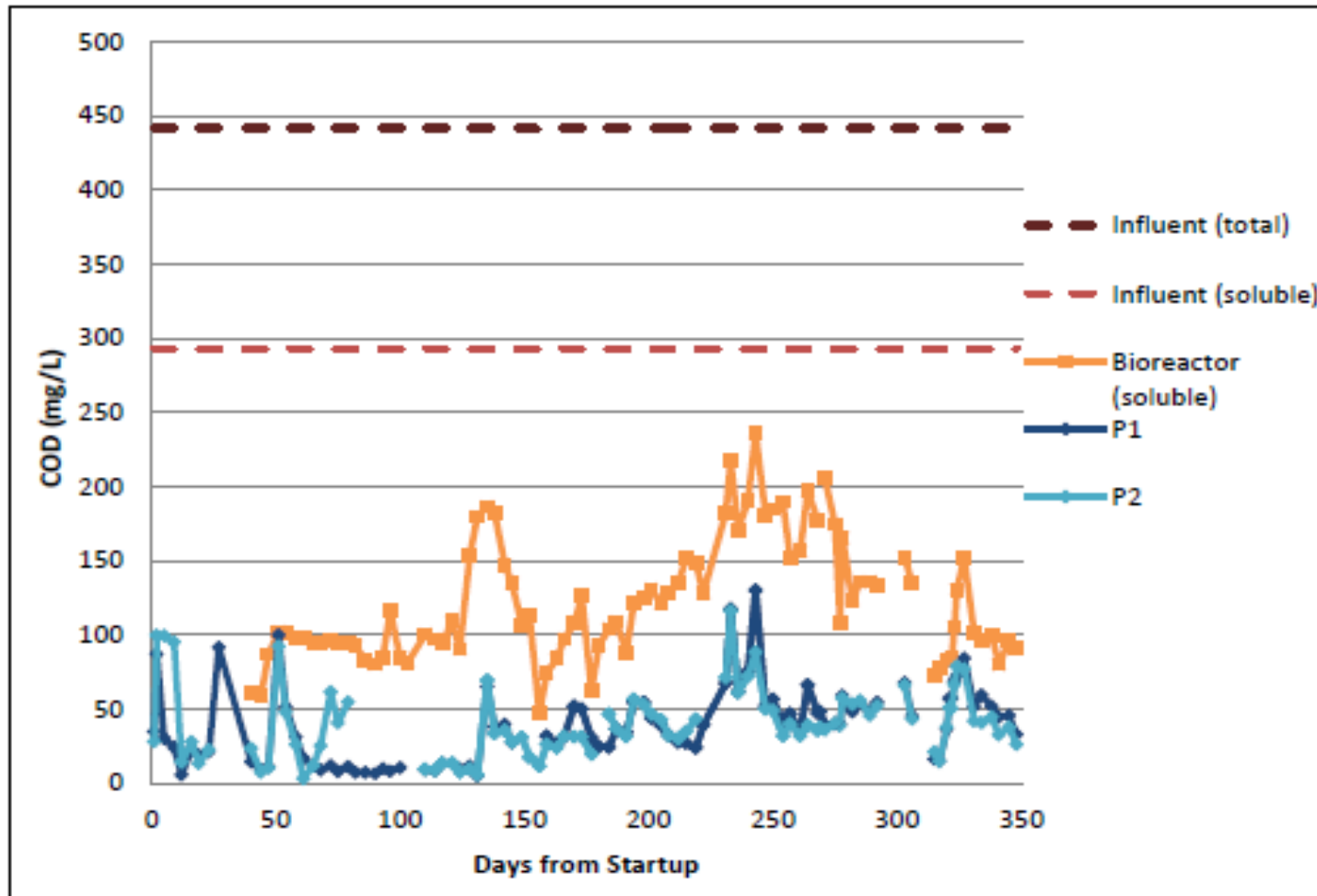
- Biogas sparging
- Backflushing
- Periodic membrane relaxation
- PAC/GAC addition
- Combinations

Operational/Performance Considerations

- OLR: >10 kg COD/m³/d
- HRT: ~ 8-12 hours
- Sustainable flux rate:
< 15 LMH
- Temperature
- Methane solubility
- $>85\%$ COD removal
- $>99\%$ TSS removal
- TN and TP removals negligible
- Effluent COD/N & COD/P unfavorable for downstream BNR



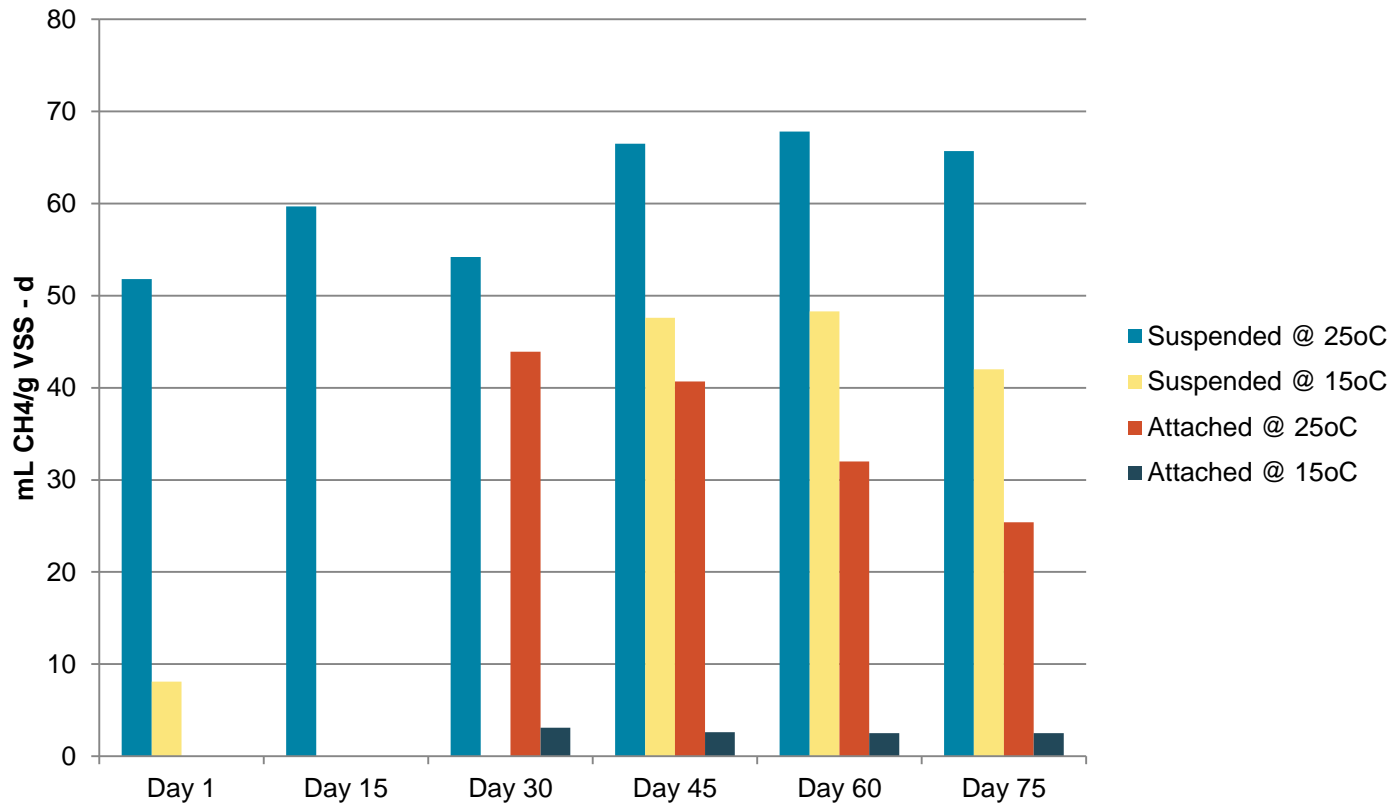
AnMBR Performance – COD Removal



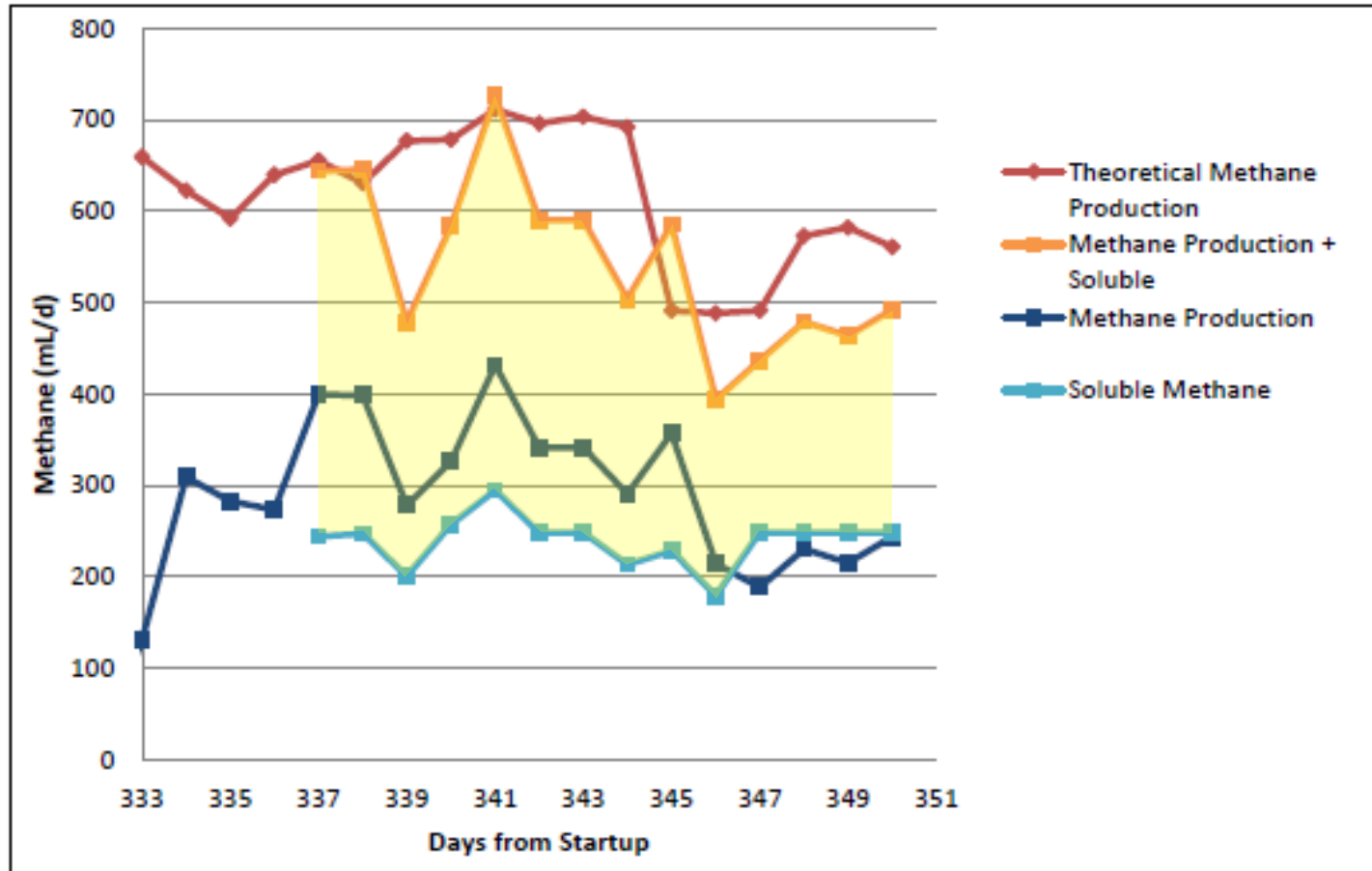
Methane Production Potential

- Colder reactor temperatures result in lower methane production

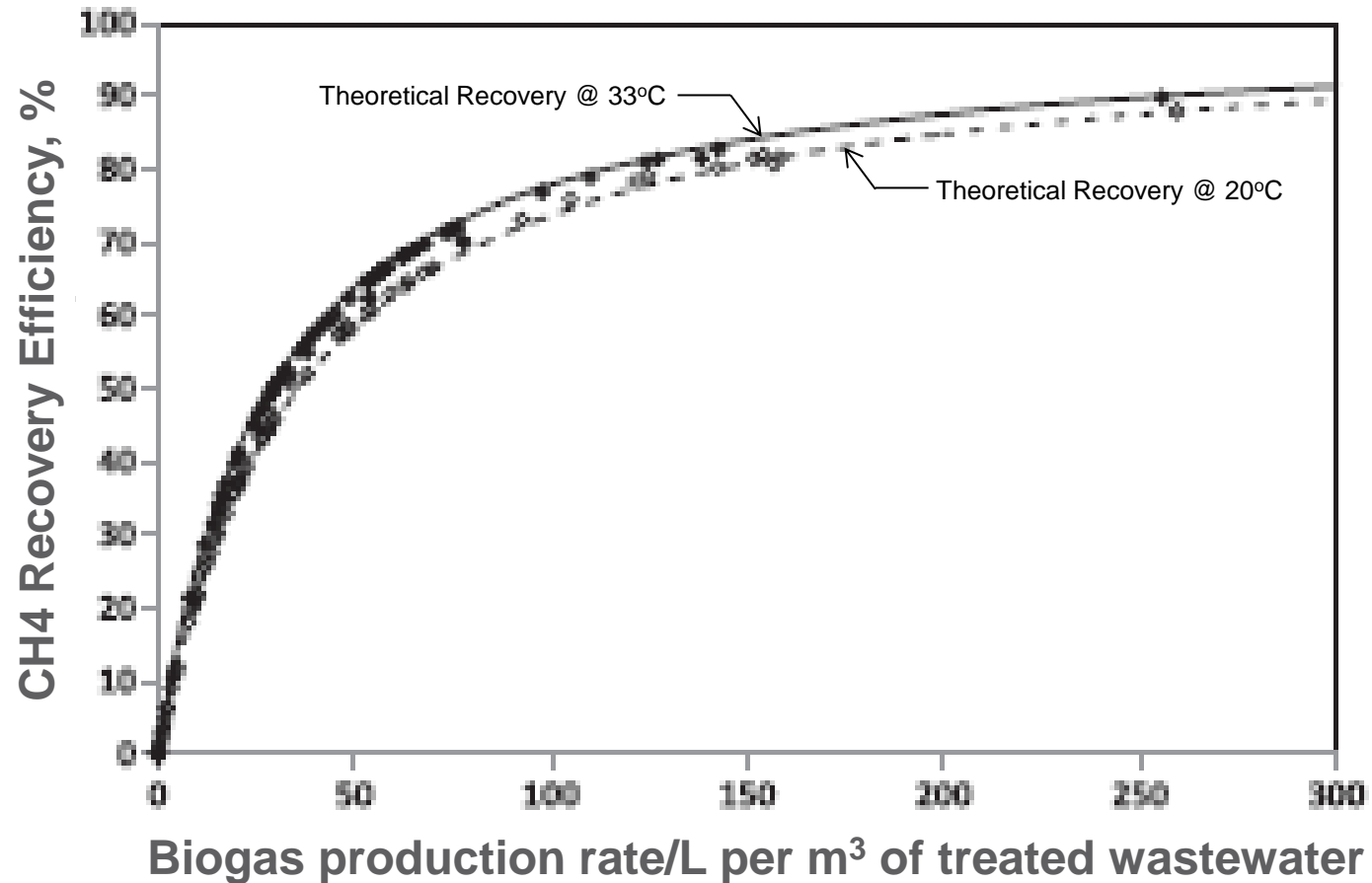
Specific Methanogenic Activity



Methane Production Potential

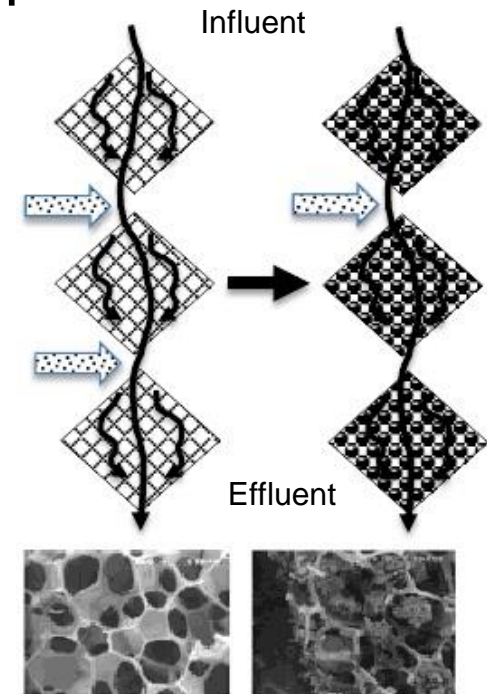


Methane Production Potential



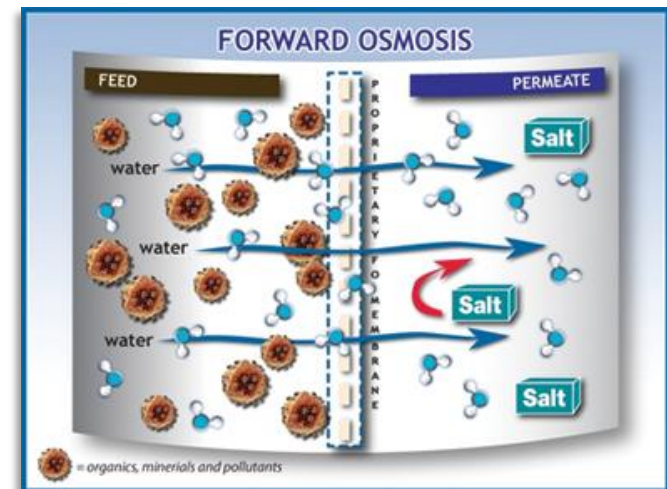
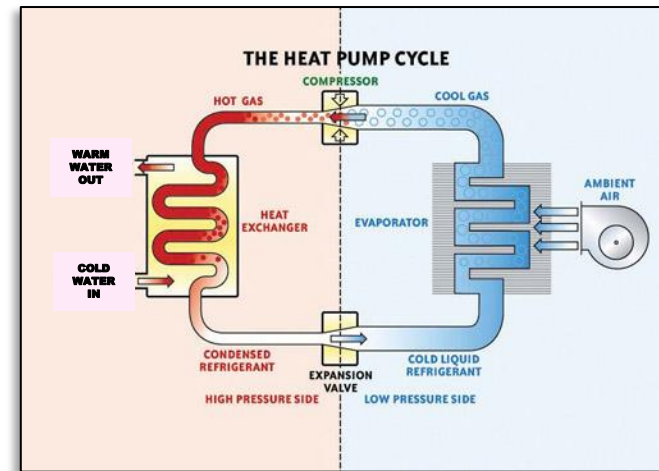
Methane Solubility Creates a Challenge

- CH_4 ~ 1.5x more soluble at 15°C than at 35°C
- Dissolved CH_4 leaving process in permeate is significant fraction to total CH_4 generated
- Permeate concentration tends to be oversaturated
- Impact on GHGs
- Post-treatment stripping
- Degassing membrane
- Downflow Hanging Sponge reactor

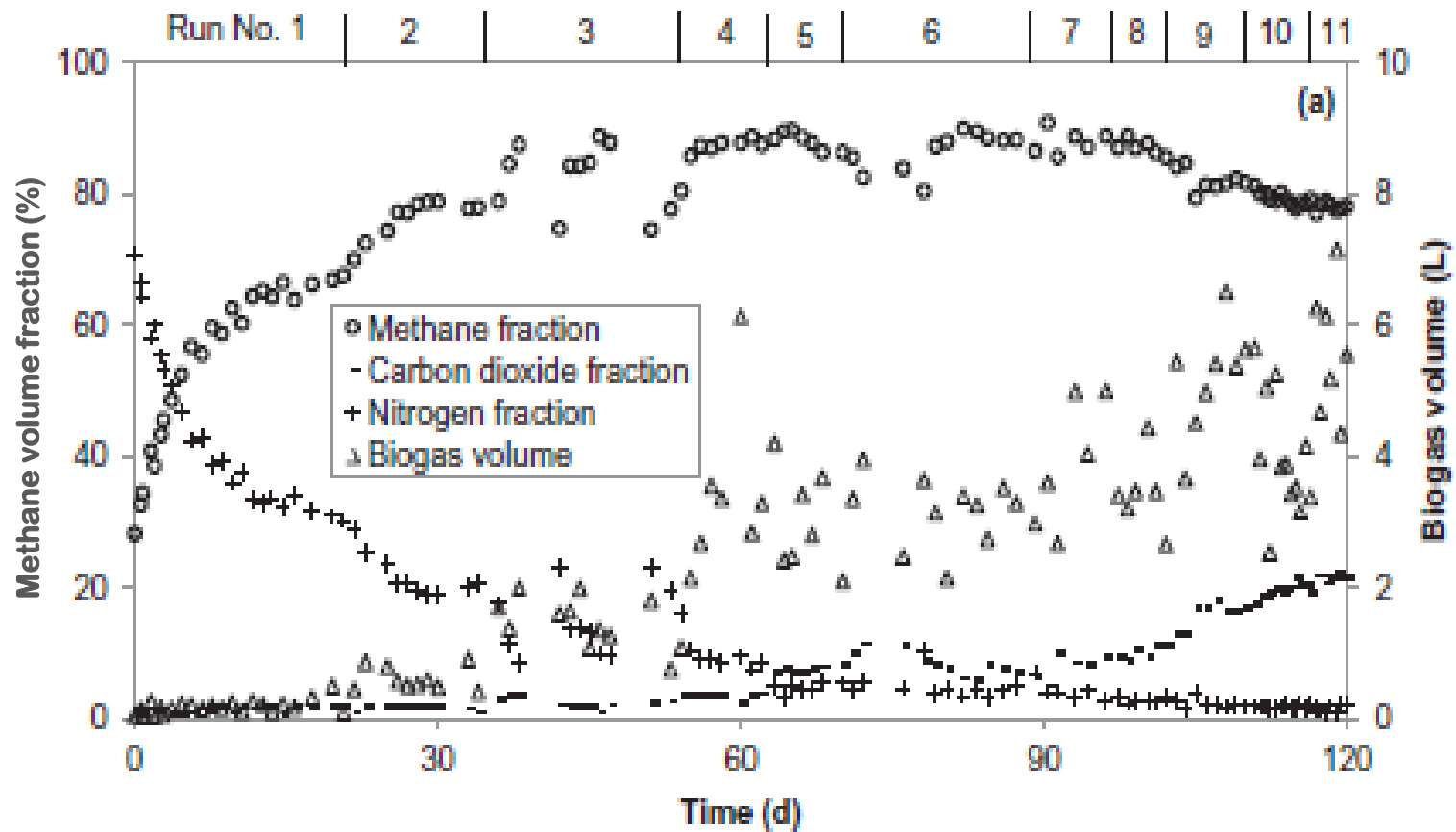


Implications for Energy Recovery

- Production is function of:
 - Temperature
 - Loading rate
 - Operating condition
 - Influent pre-treatment
 - Influent pre-heating
- 110-320 mL CH₄/g COD removed
- Net energy recovery achievable at 9.5 g COD/L or higher

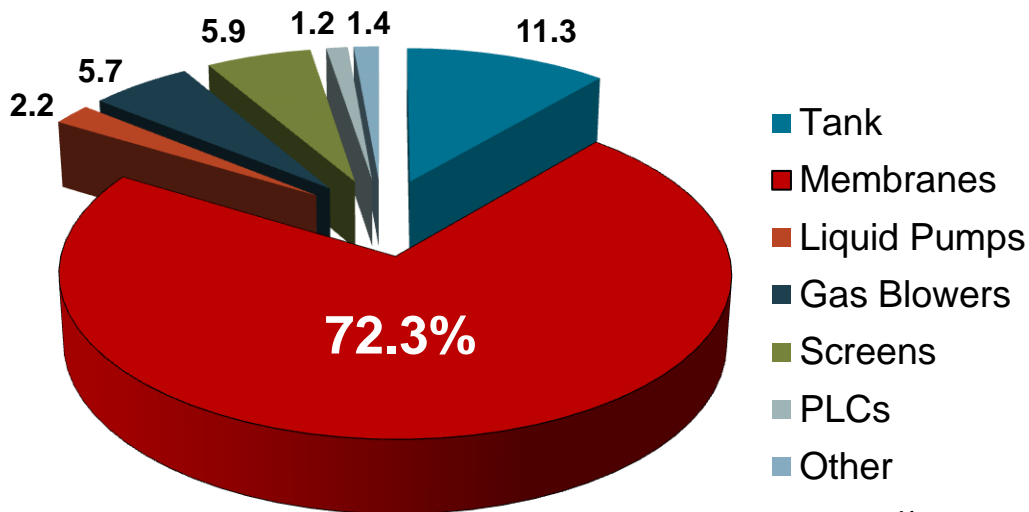


Methane Production

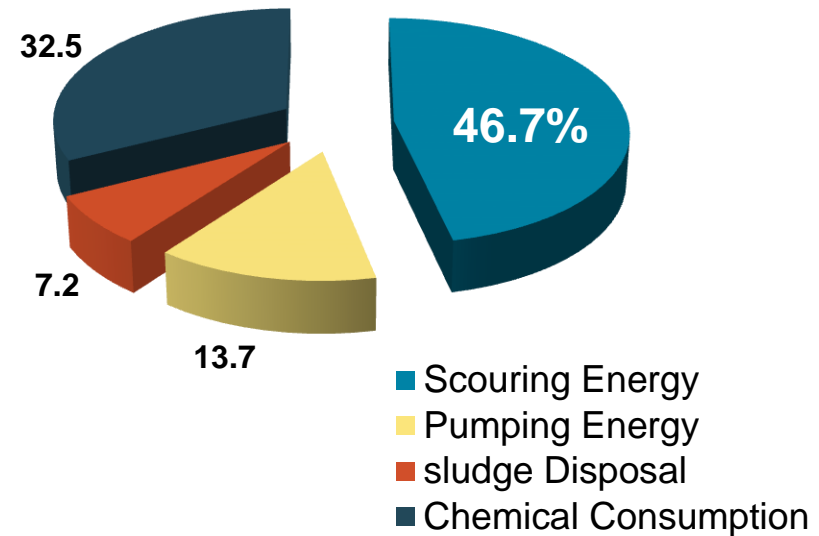


Economic Overview

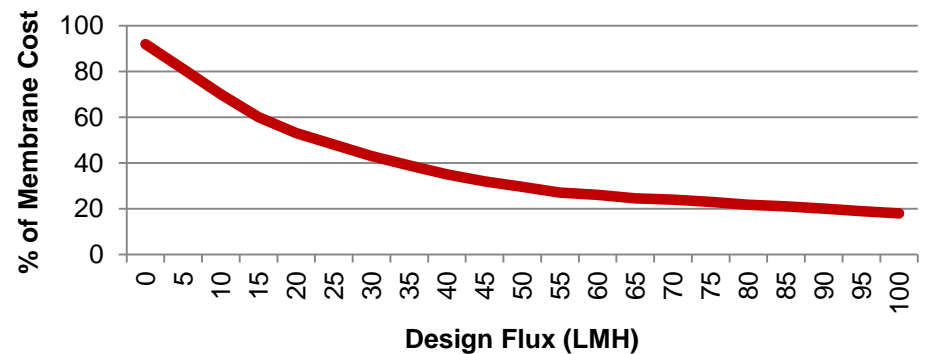
Capital Cost Elements



Operational Cost Elements



Flux Influence on Cost



Research Needs for AnMBRs

- Membrane fouling, particularly with low-strength wastewaters
- Consumption and optimization of energy
- Relationship between HRT, SRT, performance and fouling
- Methane solubility at low temperatures.
- Operation at low and high temperatures
- Effects of microbial seeding
- Nutrient removal systems
- Comprehensive effects of OLR on methane production
- Pre-treatment effects

Summary

- AnMBR Remains Challenging for Municipal
- Membrane Fouling Solutions are Elusive
- Significant Impediment is Nutrient Removal
- Methane Solubility a Challenge for Recovery
- Membranes Remain Primary Capital Cost
- Scouring Energy Primary Operational Cost
- Research Opportunities Remain High